

The committee rejected this recommendation in PI 23 stating, "The maintenance of appliances is

covered within the code. Fuel gas appliances in LNG plants are under NFPA 54 where they fall into the scope of NFPA 54 and is the proposed text is unnecessary".

This ignores the fact that NPFA excludes in 1.1.1.2 (9) LNG installations, which is reasonably interpreted by many code users to mean the entire LNG installation, including all natural gas in the vapor state, including low pressure uses, such as heating buildings and cooking. This clarification is needed to provide requirements for gas appliances and related piping in LNG plants. NFPA 59A provides no such requirements.

Related Item

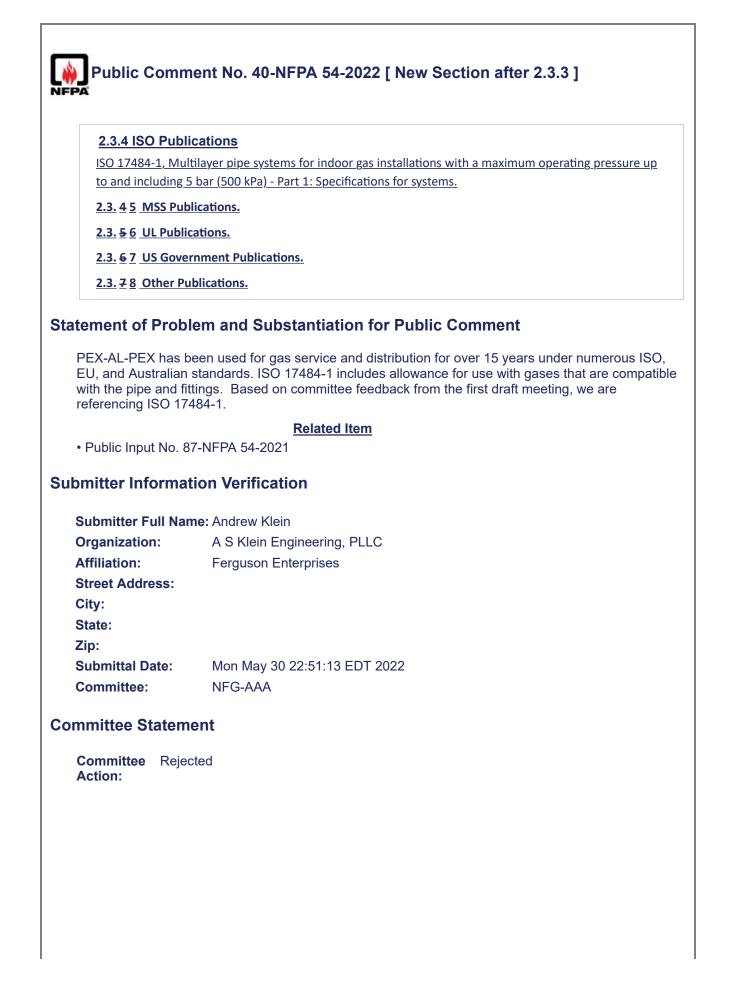
• PI 23

Submitter Information Verification

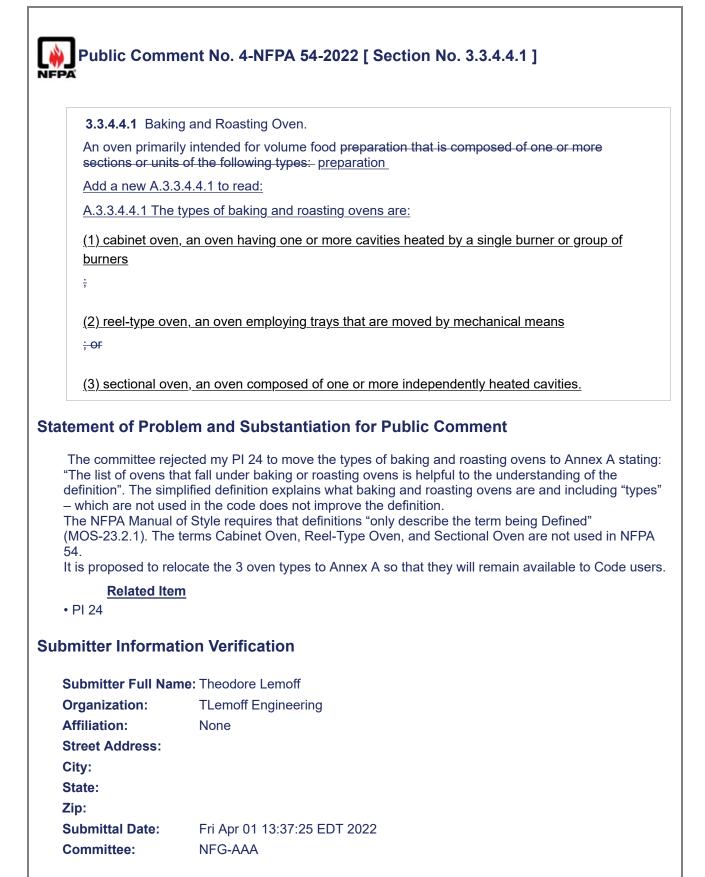
Submitter Full Name	: Theodore Lemoff
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Street Address:	
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Submittal Date:	Fri Apr 01 13:27:13 EDT 2022
Committee:	NFG-AAA

Committee Statement

Committee Action:	Rejected but see related SR
Resolution:	<u>SR-20-NFPA 54-2022</u>
Statement:	LNG Installation refers to everything inside the fence line of an LNG facility while systems covers the LNG process systems (liquefaction, regasification, etc.) and permits the use of NFPA 54 for design of systems typically designed under NFPA 54.



Resolution: Public Comments 41, 44, 45 The proposed composite tubing product (PEX-AL-PEX) as presented does not have a fire resistance that matches other similar metallic piping products that are currently recognized in Section 5.5 of the NFPA 54. The proposed PEX-AL-PEX fitting do not meet ANSI LC 4 for press-to-connect fittings (which requires 1000F). Brazing also requires a high temperature fitting (1000F). The ISO 17484-1 Standard proposed for the material does not include fire resistance requirements, and the proposed requirements do not require additional fire protection methods such as excess flow valves or external fire protection (installation behind gypsum walls). The requirement language did not require the listing to the ISO 17484-1 rather compliance to the standard. Public Comments 40, 42, 43 The definition and sizing tables were not added as the proposed piping material was not added to the code.

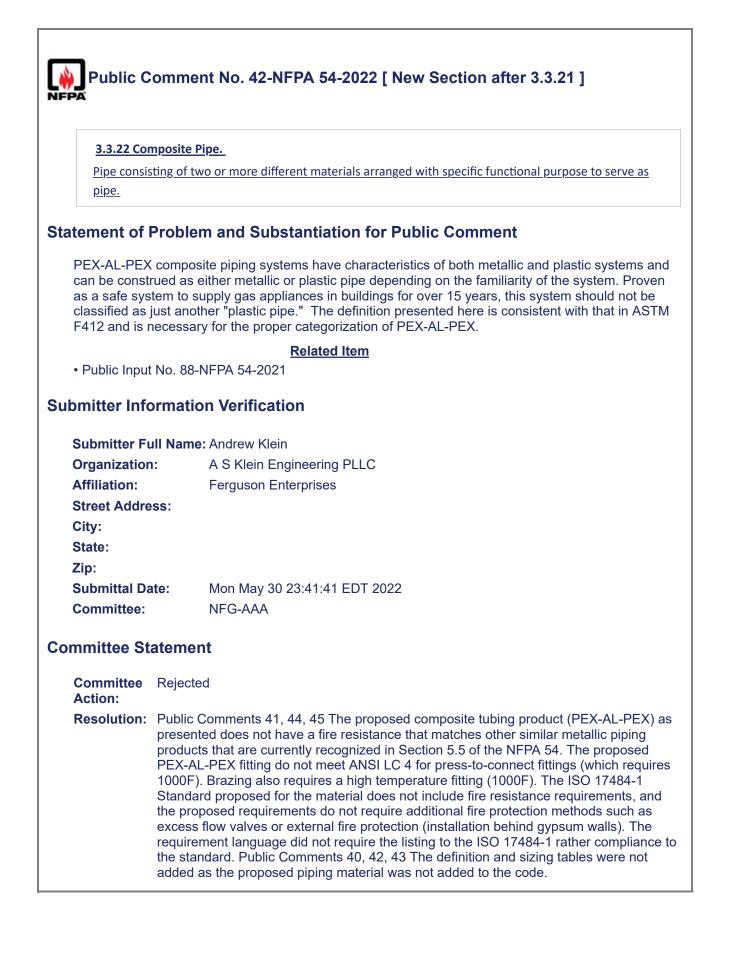


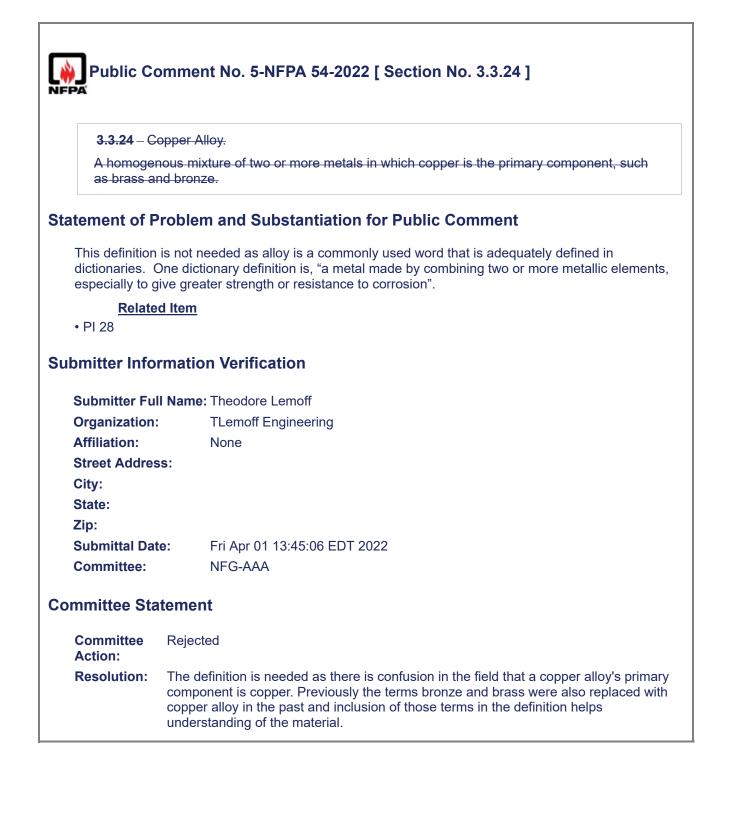
Committee Statement

Committee Action: Rejected but see related SR

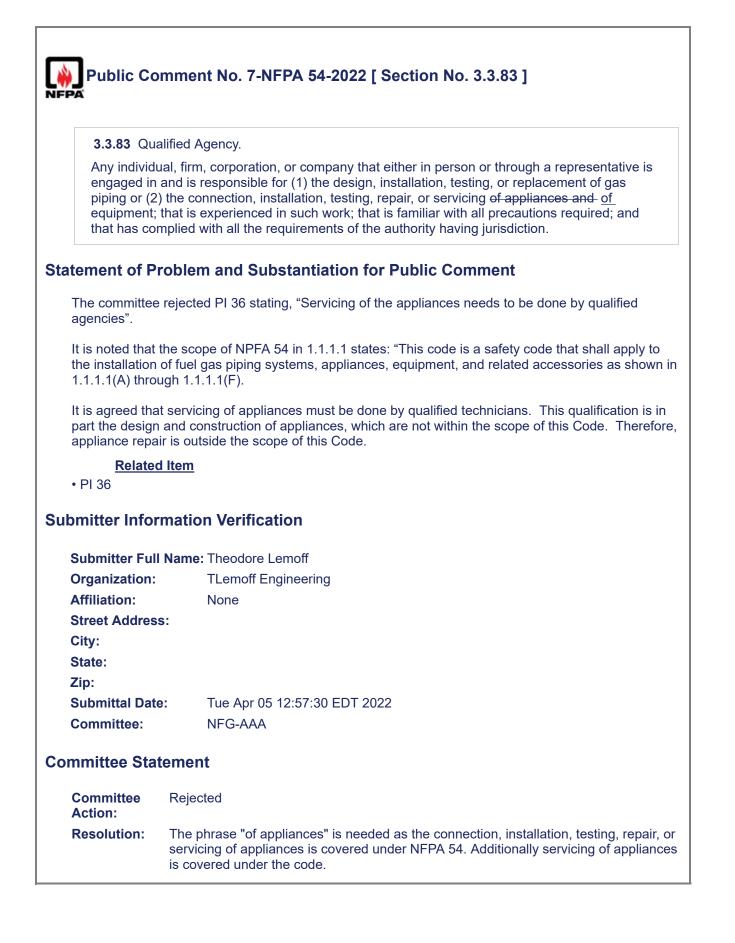
Resolution:SR-21-NFPA 54-2022Statement:Examples are being moved to the annex to clean up the definition.

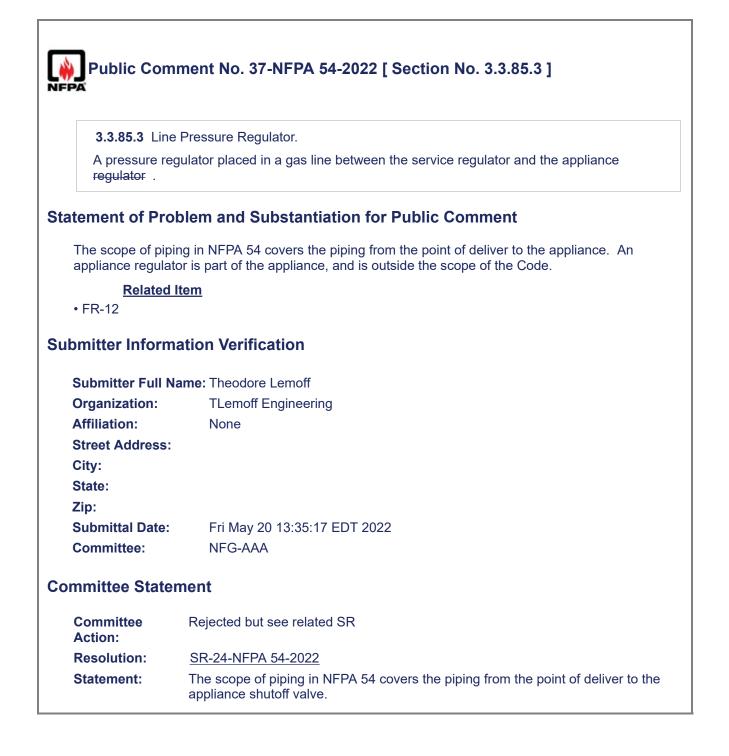
Public Comr NFPA Sub-Sections]]	ment No. 15-NFPA 54-2022 [Section No. 3.3.4.5 [Excluding any
	or domestic food preparation, providing at least one function of (1) top or surface en cooking, or (3) broiling.
Statement of Prob	plem and Substantiation for Public Comment
appliance the revis	evised by deleting "domestic". As the term being defined is inherently a residential sed definition remains clear. The subsidiary definitions of various household include the term "domestic".
Related It • PC 11	tem
Submitter Informa	ation Verification
Submitter Full Na	me: Theodore Lemoff
Organization:	TLemoff Engineering
Affiliation:	None
Street Address:	
City:	
State:	
Zip:	
Submittal Date:	Thu Apr 07 11:00:59 EDT 2022
Committee:	NFG-AAA
Committee Staten	nent
Committee Action:	Rejected but see related SR
Resolution:	<u>SR-22-NFPA 54-2022</u>
Statement:	As the term being defined is inherently a residential appliance the revised definition remains clear.

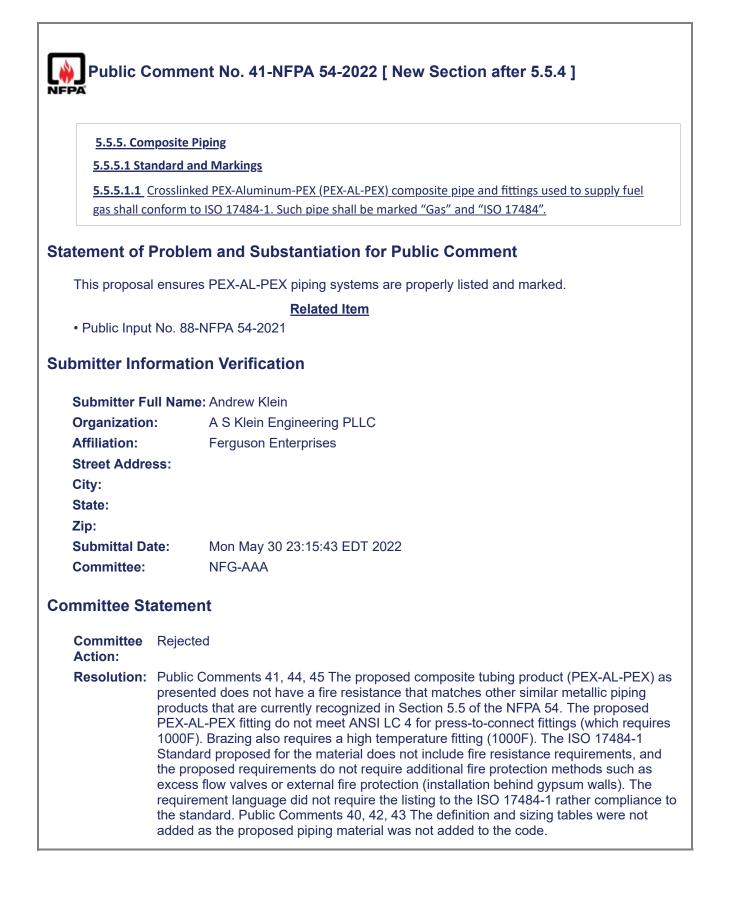




	nent No. 6-NFPA 54-2022 [Section No. 3.3.56.7]
3.3.56.7 Wate	r Heater.
An appliance for	or supplying hot water for domestic or commercial purposes. water
atement of Prob	lem and Substantiation for Public Comment
PI 33 proposing th	e substituting of "residential" for "commercial" in this definition was rejected by the
Committee with the	
	ancies are broader than what the committee intends for these appliances. The andard also refers to these appliances as domestic of household appliances and n
residential.	
	imilar, but simplifies the definition to apply to all appliance that supply hot water for ater heater is a water heater no matter what the use of the heated water is.
Related Ite	
• PI 33	<u></u>
ıbmitter Informa	tion Verification
Submitter Full Na	me: Theodore Lemoff
Organization:	TLemoff Engineering
Affiliation:	None
Street Address:	
City:	
State:	
Zip:	
Zip: Submittal Date:	Fri Apr 01 13:47:39 EDT 2022
•	Fri Apr 01 13:47:39 EDT 2022 NFG-AAA
Submittal Date:	NFG-AAA
Submittal Date: Committee:	NFG-AAA
Submittal Date: Committee:	NFG-AAA nent

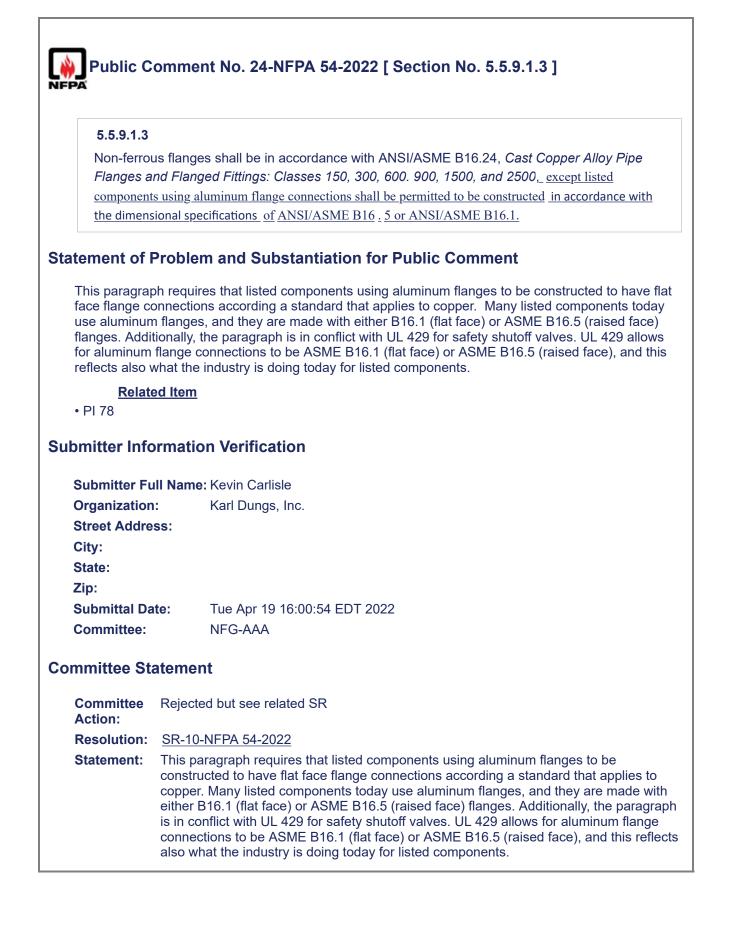


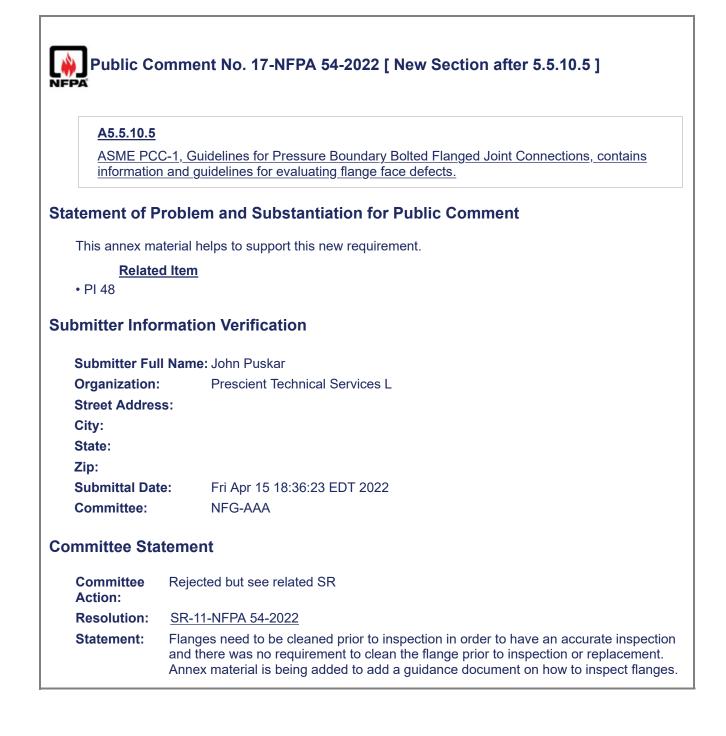


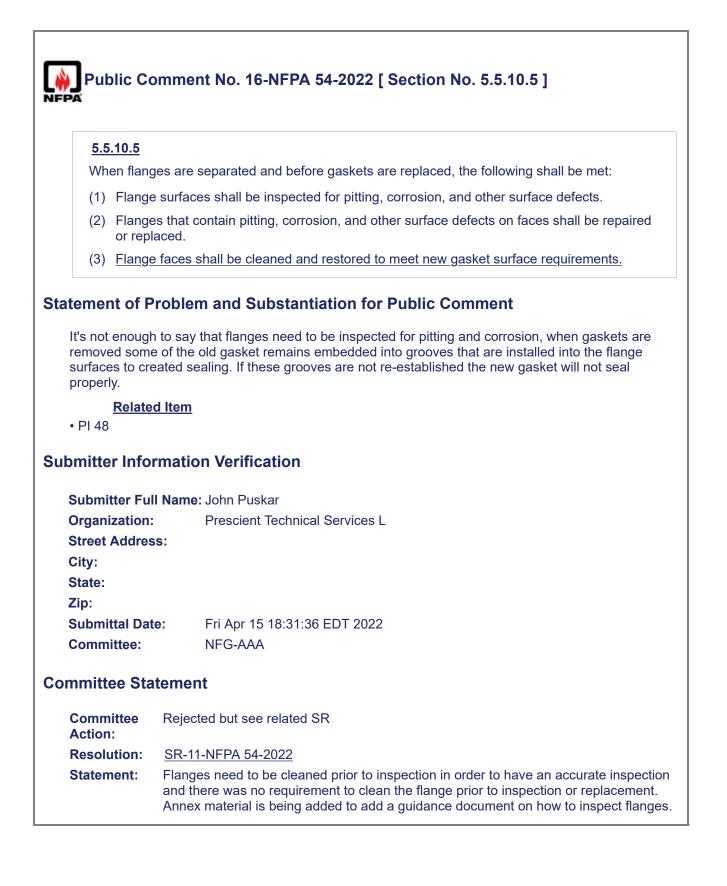


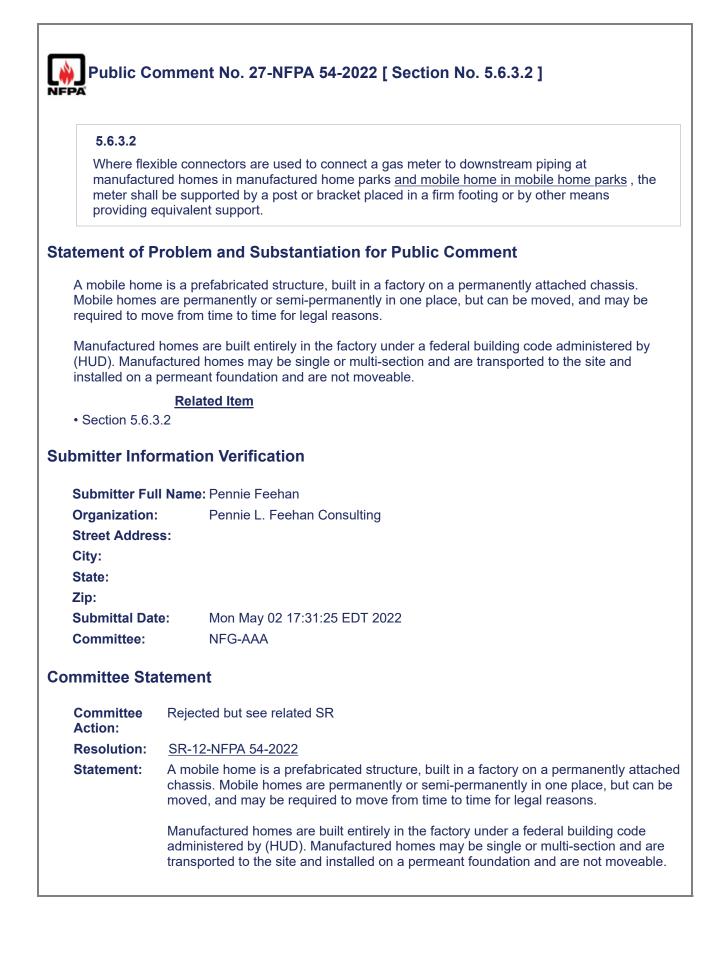
Public Comm	nent No. 46-NFPA 54-2022 [Section No. 5.5.4.2]
FFA	
5.5.4.2* Regula	ator Vent Piping.
PVC conforming	fittings used to connect regulator vents to remote vent terminations shall be g to UL 651, <i>Schedule 40 and 80 Rigid PVC Conduit and Fittings</i> PVC vent be installed indoors.
atement of Prob	lem and Substantiation for Public Comment
651 to be exposed indoors. This practi reconsider this prof • Using black in stresses on the reg used to extend ven 3/4-, and 1-inch ver • UL 651 PVC of line pressure regula resistant. Regulator and adjusting screw regulator diaphragr enhancement of sa tested for fire resist • A related cond to fire while the reg regulator vent pipin mode. If the regular will vent and therefore safety risk.	on or galvanized pipe or larger diameter copper tubing could impose excessive ulator housing. When regulators had 1/4-inch vent openings, small diameter tubing ts imposed minimal stress on the regulator. However, regulators now install 1/2-, nt openings which lead to much greater stresses on the housing. conduit is tested for limited resistance to fire. However, LP-gas second stage and ators, which are both approved for use inside buildings, are not required to be fire rs contain components which have low melting points. Plastic regulator vent caps vs will melt at temperatures as low as 225°F, and the elastomer materials of ns and seat discs will fail at approximately 400°F. Therefore, there is no fety in mandating fire-resistant vent piping, when the regulator assembly itself is not
• PI No. 121	
ubmitter Informa	tion Verification
Submitter Full Na	ne: Bruce Swiecicki
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Affiliation:	NPGA Technology, Standards and Safety Committee
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Submittal Date:	Tue May 31 13:04:21 EDT 2022
Committee:	NFG-AAA
ommittee Statem	ent
Committee Reje Action:	ected

Resolution: PVC piping material is still not acceptable to be installed indoors as there are questions on the integrity of the PVC vent piping indoors when exposed to fire. There are also questions on if UL 651 is the appropriate reference standard for indoor vent piping as there are concerns on fittings for the vent piping. Larger industrial and commercial installations could have longer vent pipe runs which are subject to physical damage. Static electricity is also a concern with plastic vent piping.









Public Comment No. 25-NFPA 54-2022 [Section No. 5.7.2]

5.7.2-_Listing.

Line pressure regulators shall either

<u>1)</u> be listed in accordance with ANSI Z21.80/CSA 6.22, *Line Pressure Regulators*, where the outlet pressure is set to 2 psi or less, <u>or</u>

2)* incorporate a high and low gas pressure device downstream that shutdown the appliance served when high and low pressure is detected.

<u>A.5.7.1(2) Each appliance downstream require a high and low gas pressure device if there are no high and low gas pressure devices located on the gas piping system serving those appliances.</u>

Statement of Problem and Substantiation for Public Comment

Listed line pressure regulators are limited in their scope for industrial applications and large commercial applications for two reasons.

 The maximum allowed outlet pressure for a listed line pressure regulator is 2 PSI. There are some industrial applications and large commercial applications that require 10 PSI at the burner.
 There are some industrial applications and large commercial applications where the delivery pressure is less than 2 PSI, but the regulators used in these applications will not comply with ANSI Z21.80, Standard for line pressure regulators, for the following reasons.

• the standard for line pressure regulators ANSI Z21.80 requires that regulator be capable with flowing a minimum of 0.15CFH of natural gas. Many regulators used on industrial applications and large commercial applications today can be in the 5" – 8" pipe size, and these regulators cannot flow this small rate.

• the standard for line pressure regulators ANSI Z.21.80 requires that regulator be capable with passing a 100,000 life cycle test. Many regulators used on large industrial applications and large commercial applications today are big. To move the mechanical parts within a big regulator means bigger forces, and this leads to mechanical failure long before reaching 100,000 cycles.

• the standard for line pressure regulators ANSI Z.21.80 requires that regulator be capable of a lockup pressure of 150% of the setpoint or +5"WC, whichever is greater. Many regulators used on industrial applications and large commercial applications are pilot loaded, and thus cannot pass this ANSI Z.21.80 requirement. The pilot loaded regulator are much slower reacting than the typical, "direct acting" spring loaded regulators that are currently certified to ANSI Z21.80.

The proposed solution is good for all code users. Not only is it easy to enforce and reflects what these industries are currently doing, the requirement for high and low gas offers as-good-as or greater safety for these two reasons:

1. The devices are "safety" devices, subjected to the stringent safety requirements of UL 353 or UL 60739-2-5.

2. Regulator can fail because: a diaphragm fails, debris gets into the regulator mechanisms and causes the regulator to stick, a regulating disc breaks, there is a condition where there is too high or too low of an inlet pressure which causes significant droop, or there is an improper field adjustment or incorrect installation of a spring. These risks are all greatly mitigated when a line pressure regulator certified to ANSI Z21.80. However, those same risks are mitigated even more when using a high and low gas pressure device. These devices continuous monitor the outlet pressure of the upstream regulator during operation of the appliance, and any condition (for whatever reason) that causes the regulated pressure to exceed the settings of the devices, the appliance shuts down.

Related Item

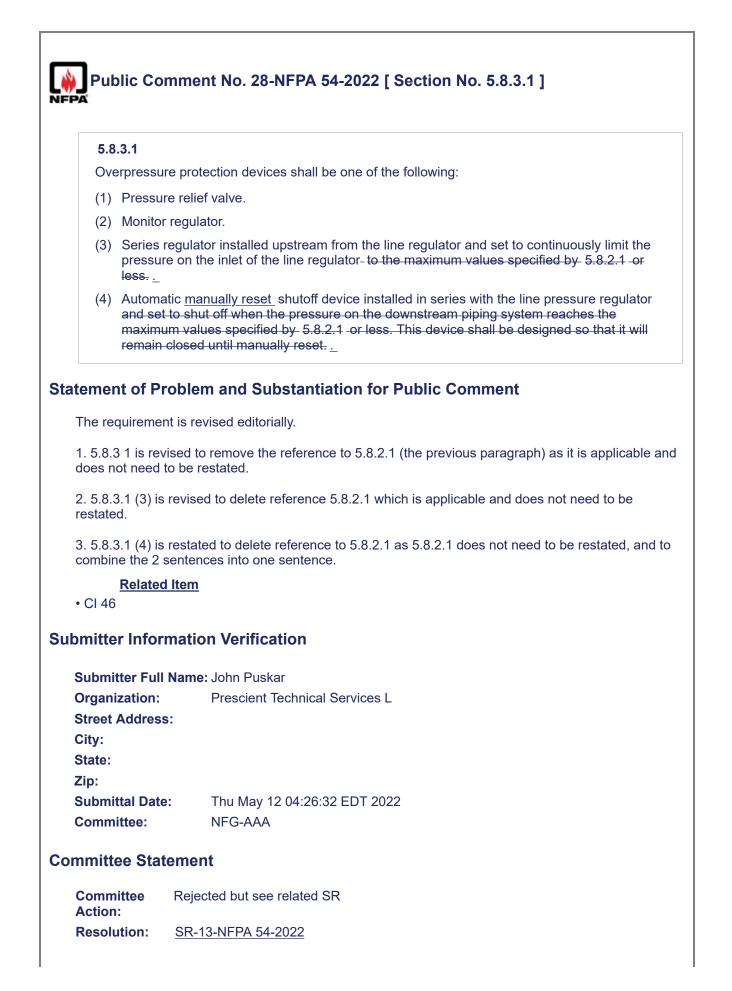
• PI 18

Submitter Information Verification

Submitter Full Name	: Kevin Carlisle
Organization:	Karl Dungs, Inc.
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Submittal Date:	Thu Apr 21 14:35:15 EDT 2022
Committee:	NFG-AAA

Committee Statement

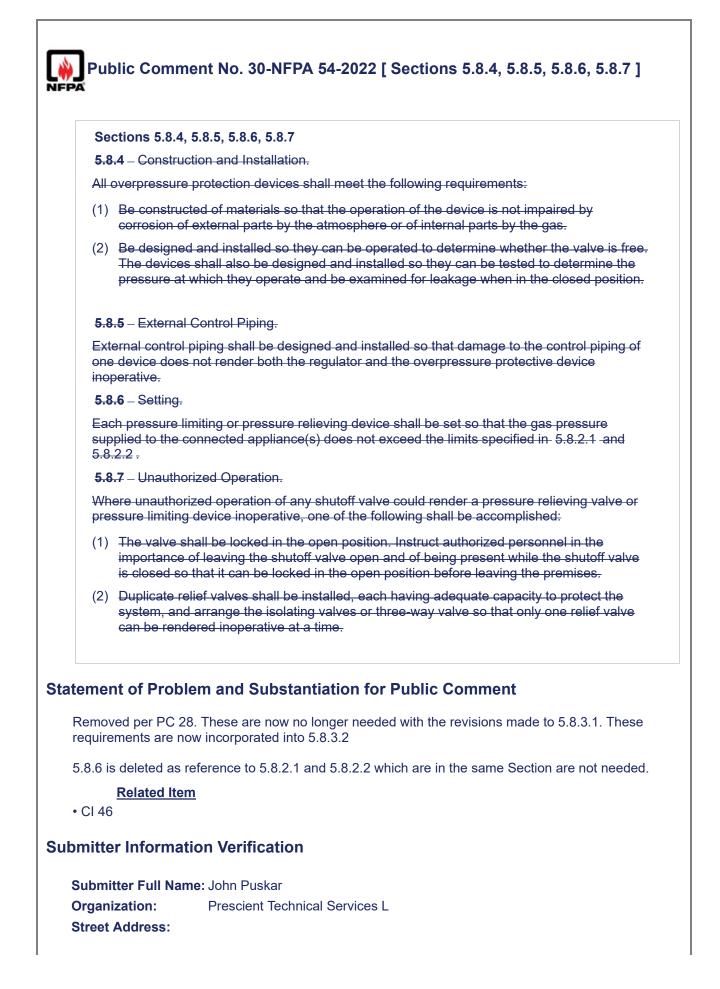
Committee Action:	Rejected
Resolution:	The proposed changes fall under a product listing standard rather than an installation standard. This proposal also potentially negates the need to have a listed line pressure regulator. The language also limits the alternative methods that are also acceptable protection methods.



Statement: 5.8.3.1 (3) is revised to delete reference 5.8.2.1 which is applicable and does not need to be restated. 5.8.3.1 (4) is revised to delete reference to 5.8.2.1 as 5.8.2.1 does not need to be restated.

See Global SR 32 for related revisions on multi-requirement renumbering.

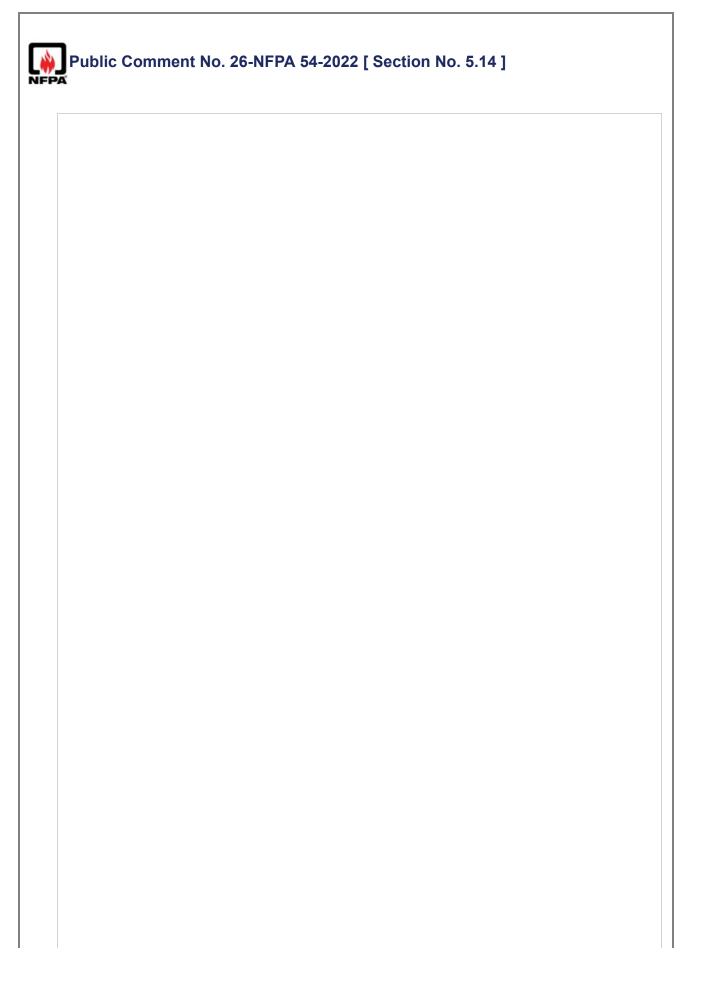
5.8.3.2	
pressure re installed, th <u>1. Be const</u>	s in 5.8.3.1 shall be installed either as an integral part of the service or line gulator or as separate units. Where separate overpressure protection devices are ey shall comply with 5.8.4 through 5.8.9. ructed so that the operation of the device is not impaired by corrosion of external or ts by the gas
	ned and installed so that they can be operated to determine that the valve s are free to operate as designed.
<u>3. Prevent u</u>	unauthorized operation.
• CI 46	mation Verification
	Name: John Puskar
Organization: Street Address City:	Prescient Technical Services L
State: Zip:	
Submittal Date Committee:	e: Thu May 12 04:30:35 EDT 2022 NFG-AAA
committee.	
	tement
committee Stat	Rejected



City: State: Zip: Submittal Date Committee:	: Thu May 12 04:34:57 EDT 2022 NFG-AAA
Committee Stat	ement
Committee Action:	Rejected
Resolution:	The requirements in 5.8.4 through 5.8.7 are necessary for overpressure protection devices where they are not integrally part of the service or line pressure regulator.

TA	
E 0 0 0	
5.8.8.2	stack or yest line shell be:
	stack or vent line shall be:
	same size as the outlet of the pressure relieving device.
<u>b) designed ar</u> could cause bl	nd installed to prevent the entry of insects, water, or other foreign materials that ockage.
atement of Pro	blem and Substantiation for Public Comment
The additional rec piping to enhance	uirements addresses an important factor in the design and installation of discharg safety.
Related Ite	-
• fr 25	
bmitter Inform	ation Verification
Submitter Full N	ame: John Puskar
Submitter Full Na Organization:	
Submitter Full Na Organization: Street Address:	ame: John Puskar
Submitter Full Na Organization: Street Address: City:	ame: John Puskar
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Submitter Full Na Organization: Street Address: City: State:	ame: John Puskar
Submitter Full Na Organization: Street Address: City: State: Zip: Submittal Date: Committee:	ame: John Puskar Prescient Technical Services L Thu May 12 04:39:47 EDT 2022 NFG-AAA
Submitter Full Na Organization: Street Address: City: State: Zip: Submittal Date:	ame: John Puskar Prescient Technical Services L Thu May 12 04:39:47 EDT 2022 NFG-AAA

Dublic C	mment No. 22 NEDA 54 2022 (Section No. 5.9.0.)
	omment No. 32-NFPA 54-2022 [Section No. 5.8.9]
5.8.9 Size	e of Fittings, Pipe, and Openings.
relieving d	s, pipe, and openings located between the system to be protected and the pressure evice shall be sized to prevent hammering of the valve and to prevent impairment of <u>of</u> relief capacity.
atement of F	Problem and Substantiation for Public Comment
	an mean many things, reduction speaks more directly to the actual condition we are lress with this item.
Related	d Item
• fr 25	
ubmitter Info	rmation Verification
Submitter Fu	II Name: John Puskar
Organization	
Street Addres	SS:
City: State:	
Zip:	
Submittal Da	te: Thu May 12 04:44:13 EDT 2022
Committee:	NFG-AAA
ommittee Sta	atement
Committee Action:	Rejected but see related SR
Resolution:	<u>SR-15-NFPA 54-2022</u>
Statement:	Reduction of relief capacity is the concern when sizing fittings, pipe, and openings between the system and pressure relieving devices. The term hammering is being removed as it is unclear what the term is referring to and if sized correctly hammering is not a concern.



5.14– _ Pressure Regulator and Pressure Control Venting.

	of the atmospheric side of diaphragms in line pressure regulators, gas appliance nd gas pressure limit controls shall be
	e with all of the following:An independent vent pipe to the outdoors, sized in with the device manufacturer's instructions, shall be provided
	here the location of a device is such that a discharge of fuel gas will cause a
hazard.	<u> </u>
For devices of where the	other than appliance regulators, vents shall not be required to be independent
5.14.2 Instal	lation of Pressure Control Venting.
pressure reg	led, pressure control venting of the atmospheric side of diaphragms in line ulators, gas appliance regulators, and gas pressure limit controls shall be in with this section.
other than ap	e vent shall be independent, excluding approved vent designs for devices that are opliance regulators whose vents are connected to a common manifold designed in with engineering methods to minimize backpressure in the event of diaphragm
	sign is approved.A regulator
anu suon uc <u>.</u>	oign to approvour trogulator
5.14.2.2 The	e vent pipe shall vent to the outdoors, excluding regulators and vent limiting means
combination combinations	listed in accordance with ANSI Z21.80/CSA 6.22, Line Pressure Regulators,
shall not be listed gas a	required to be vented to the outdoors.A <u>ppliance</u>
r egulator regulators_fa	ctory equipped with
a	
vent limiting	
	required to be vented to the outdoors.A listed listed gas pressure limit
control	
<u>controls_that</u>	
i s factory are factory_e	equipped with
a <u>vent limiting</u>	
device	
devices and	in accordance with UL 353, <i>Limit Controls</i> , or UL 60730-2-6, <i>Automatic Electrical</i> Household and Similar Use, Part 2
, shall not be	required to be vented to the outdoors.Materials
- <u>5.14.2.3</u> The instructions.	e vent pipe shall be sized in accordance with the device manufacturer's
5.14.2.4 Ven	t piping shall be installed to minimize static loads and bending moments placed on s and gas pressure control devices.
5.14.2.5 Ven	<u>it piping from pressure regulators and gas pressure controls shall not be</u> a common manifold that serves a bleed line from a diaphragm-type gas valve.
	Materials <u>.</u>
<u>0.14.0 v</u> ont i	
	vent piping shall be in accordance with Section 5.5.

	vent terminus shall be designed to prevent the entry of water, insects, and other that could cause blockage.
Vent piping sh regulators and	all be installed to minimize static loads and bending moments placed on the logal pressure control devices. s shall terminate not less than 3 ft (0.9 m) from a possible source of ignition.
accumulations	cations where a vent termination could be submerged during floods or snow , an antiflood-type breather vent fitting shall be installed, or the vent terminal d above the height of the expected flood waters or snow.
	om pressure regulators and gas pressure controls shall not be connected to a fold that serves a bleed line from a diaphragm-type gas valve.
Additional Propos	sed Changes
File N PC on FR No.	
	olem and Substantiation for Public Comment
the PC and shows to include only on	uirements and avoid conflicts. The attached document provides a clean version of s where each provision from the original language was moved. The text was worded e "shall" in each clause and to incorporate exceptions into the main requirement. coordinate this section with work the Editorial Task Group had already done.
Public Input No.	Related Item 19 • FR No. 12
Submitter Informa	ation Verification
Submitter Full Na	ame: Daniel Buuck
Organization:	National Association of Home Builders
Street Address:	
City:	
State:	
Zip:	
Submittal Date:	Fri Apr 29 13:08:27 EDT 2022
Committee:	NFG-AAA
Committee Stater	nent
Committee Action:	Rejected
Resolution:	The proposed revisions confused the concept of gas controls as opposed to gas pressure regulators

Clean Text Version of PCp. 1	
Public Commentp. 2	
Legislative text with comments	

Public Comment - Clean Text Version

5.14 Pressure Regulator and Pressure Control Venting.

5.14.1 Protection Against Discharge.

The venting of the atmospheric side of diaphragms in line pressure regulators, gas appliance regulators, and gas pressure limit controls shall be provided where the location of a device is such that a discharge of fuel gas will cause a hazard.

5.14.2 Installation of Pressure Control Venting.

Where installed, pressure control venting of the atmospheric side of diaphragms in line pressure regulators, gas appliance regulators, and gas pressure limit controls shall be in accordance with this section.

5.14.2.1 The vent shall be independent, excluding approved vent designs for devices that are other than appliance regulators whose vents are connected to a common manifold designed in accordance with engineering methods to minimize backpressure in the event of diaphragm failure.

5.14.2.2 The vent pipe shall vent to the outdoors, excluding regulators and vent limiting means combinations listed in accordance with ANSI Z21.80/CSA 6.22, *Line Pressure Regulators*, listed gas appliance regulators factory equipped with vent limiting devices and listed gas pressure limit controls that are factory equipped with vent limiting devices and in accordance with UL 353, *Limit Controls*, or UL 60730-2-6, *Automatic Electrical Controls for Household and Similar Use, Part 2*.

5.14.2.3 The vent pipe shall be sized in accordance with the device manufacturer's instructions.

5.14.2.4 Vent piping shall be installed to minimize static loads and bending moments placed on the regulators and gas pressure control devices.

5.14.2.5 Vent piping from pressure regulators and gas pressure controls shall not be a connected to a common manifold that serves a bleed line from a diaphragm-type gas valve.

5.14.3 Vent Materials.

Materials for vent piping shall be in accordance with Section 5.5.

5.14.4 Vent Terminations.

5.14.4.1 The vent terminus shall be designed to prevent the entry of water, insects, and other foreign matter that could cause blockage.

5.14.4.2 Vents shall terminate not less than 3 ft (0.9 m) from a possible source of ignition.

5.14.4.3 At locations where a vent termination could be submerged during floods or snow accumulations, an antiflood-type breather vent fitting shall be installed, or the vent terminal shall be located above the height of the expected flood waters or snow.

Public Comment – Legislative Text Version

5.14 Pressure Regulator and Pressure Control Venting.

5.14.1 Protection Against Discharge.

The venting of the atmospheric side of diaphragms in line pressure regulators, gas appliance regulators, and gas pressure limit controls shall be in accordance with all of the following:

(1) An independent vent pipe to the outdoors, sized in accordance with the device manufacturer's instructions, shall be provided where the location of a device is such that a discharge of fuel gas will cause a hazard.

5.14.2 Installation of Pressure Control Venting.

Where installed, pressure control venting [of the atmospheric side of diaphragms in line pressure regulators, gas appliance regulators, and gas pressure limit controls] shall be in accordance with this section.

5.14.2.1 (2) The vent shall be independent, excluding approved vent designs for For devices that are other than appliance regulators, vents shall not be required to be independent where the whose vents are connected to a common manifold designed in accordance with engineering methods to minimize backpressure in the event of diaphragm failure and such design is approved.

5.14.2.2 (3) —<u>The</u>-vent pipe shall vent to the outdoors, excluding <u>A</u>-regulator<u>s</u> and vent limiting means combination<u>s</u> listed in accordance with ANSI Z21.80/CSA 6.22, Line Pressure Regulators, shall not be required to be vented to the outdoors.

(4) A listed gas appliance regulators factory equipped with a-vent limiting devices and is not required to be vented to the outdoors.

(5) A listed gas pressure limit controls that is are factory equipped with a vent limiting devices and in accordance with UL 353, Limit Controls, or UL 60730-2-6, Automatic Electrical Controls for Household and Similar Use, Part 2, shall not be required to be vented to the outdoors.

5.14.2.3 The vent pipe shall be sized in accordance with the device manufacturer's instructions.

5.14.2.4 Vent piping shall be installed to minimize static loads and bending moments placed on the regulators and gas pressure control devices.

5.14.2.5 Vent piping from pressure regulators and gas pressure controls shall not be a connected to a common manifold that serves a bleed line from a diaphragm-type gas valve.

5.14.3 Vent Materials.

(6) Materials for vent piping shall be in accordance with Section 5.5.

5.14.4 Vent Terminations.

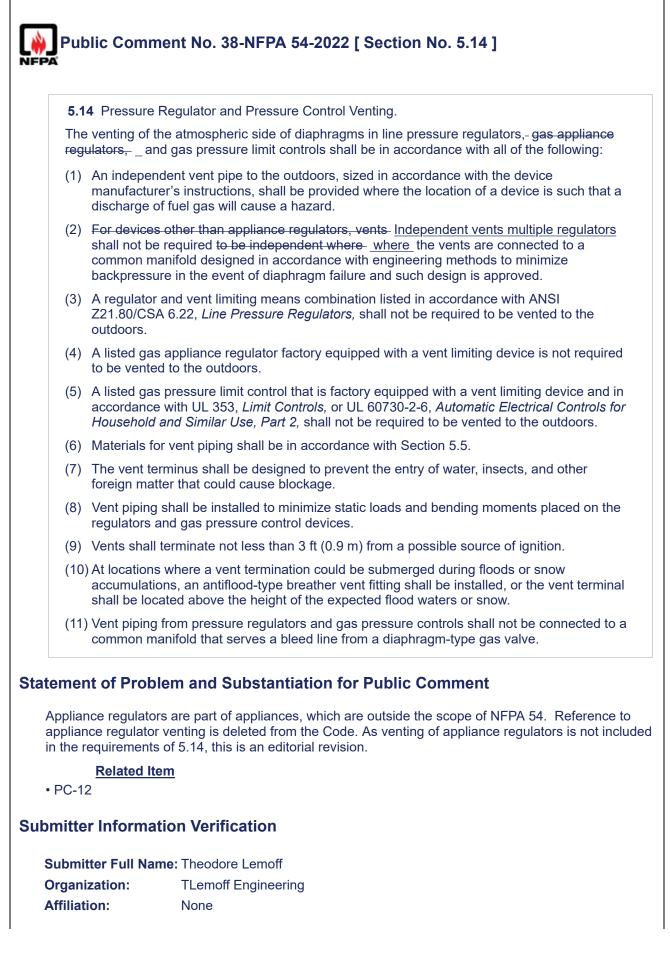
5.14.4.1 (7) — The vent terminus shall be designed to prevent the entry of water, insects, and other foreign matter that could cause blockage.

(8) Vent piping shall be installed to minimize static loads and bending moments placed on the regulators and gas pressure control devices.

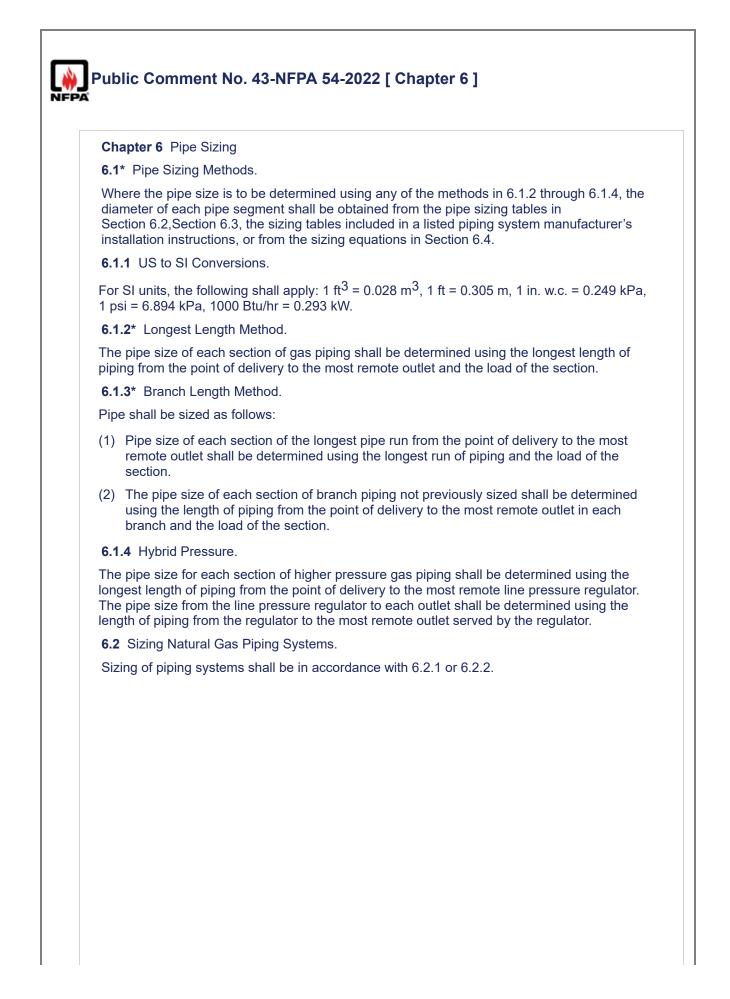
5.14.4.2 (9) Vents shall terminate not less than 3 ft (0.9 m) from a possible source of ignition.

5.14.4.3 (10) At locations where a vent termination could be submerged during floods or snow accumulations, an antiflood-type breather vent fitting shall be installed, or the vent terminal shall be located above the height of the expected flood waters or snow.

(11) Vent piping from pressure regulators and gas pressure controls shall not be a connected to a common manifold that serves a bleed line from a diaphragm type gas valve.



Street Address: City: State: Zip:	
Submittal Date:	Fri May 20 13:39:57 EDT 2022
Committee:	NFG-AAA
Committee State Committee Action:	ment Rejected but see related SR
Resolution:	<u>SR-29-NFPA 54-2022</u>
Statement:	Appliance regulators are part of appliances, which are outside the scope of NFPA 54. Reference to appliance regulator venting is deleted from the Code.
	See Global SR 31 for changes to 5.14(10)



6.2.1

Table 6.2.1(a) through Table 6.2.1(x) shall be used in conjunction with one of the methods described in 6.1.2 through 6.1.4 for piping materials other than non-corrugated stainless steel tubing.

Table 6.2.1(a) Schedule 40 Metallic Pipe

		leuule										
-	-	-	_	-	-	-	-	-	-	-		<u>Gas</u>
											Pr	<u>Inle</u> essure
-	-	-	-	-	-	-	-	-	-	-		ressur
-	_	_	_	_	_	_	_	_	_	-		Drop
												Specifi
-	-	-	-	-	-	-	-	-	-	-		<u>Gravity</u>
-					1	1	<u>Pipe</u>	<u>e Size (</u>	<u>in.)</u>			
Nominal:	¹ /2	³ /4	<u>1</u>	<u>1¼</u>	<u>1½</u>	<u>2</u>	<u>2¹/2</u>	<u>3</u>	<u>4</u>	<u>5</u>	<u>6</u>	<u>8</u>
<u>Actual</u>		0.004	4 0 4 0	4 000	4 0 4 0	0.007	0.400	0.000	4 000	E 0.47	0.005	7 004
<u>ID:</u>	<u>0.622</u>	<u>0.824</u>	<u>1.049</u>	<u>1.380</u>	<u>1.610</u>	<u>2.067</u>	2.469	3.068	<u>4.026</u>	<u>5.047</u>	<u>6.065</u>	<u>7.981</u>
Length (ft)					Car	oacitv i	n Cubi	c Feet	of Gas	per Ho	ur	
10	131	273	514	1,060	1,580	3,050				-	51,300	105 00
20	90	188	353	726	1,090	2,090	· ·	· ·	12,000	· ·	· ·	72,400
30	72	151	284	583	873	1,680		4,740		17,500		58,200
40	62	129	243	499	747	1,440	2,290	4,050		15,000		49,800
50	55	114	215	442	662	1,280	· ·	3,590		13,300		44,100
60	50	104	195	400	600	1,160	1,840	3,260	6,640	12,000	19,500	40,000
70	46	95	179	368	552	1,060	1,690	3,000	6,110	11,100	17,900	36,800
80	42	89	167	343	514	989	1,580	2,790	5,680	10,300	16,700	34,200
90	40	83	157	322	482	928	1,480	2,610	5,330	9,650	15,600	32,100
100	38	79	148	304	455	877	1,400	2,470	5,040	9,110	14,800	30,300
125	33	70	131	269	403	777	1,240	2,190	4,460	8,080	13,100	26,900
150	30	63	119	244	366	704	1,120	1,980	4,050	7,320	11,900	24,300
175	28	58	109	224	336	648	1,030	1,820	3,720	6,730	10,900	22,400
200	26	54	102	209	313	602	960	1,700	3,460	6,260	10,100	20,800
250	23	48	90	185	277	534	851	1,500	3,070	5,550	8,990	18,500
300	21	43	82	168	251	484	771	1,360		5,030	8,150	16,700
350	19	40	75	154	231	445	709	1,250	2,560	4,630	7,490	15,400
400	18	37	70	143	215	414	660	1,170	2,380	4,310	6,970	14,300
450 500	17 16	35	66 62	135	202	389	619	1,090	2,230	4,040	6,540	13,400
500	16	33	62 50	127	191	367	585	1,030	2,110	3,820	6,180 5,870	12,700
550 600	15 14	31 30	59 56	121 115	181 173	349 333	556 530	982 937	2,000	3,620 3,460	5,600	12,100 11,500
650	14	29	50 54	110	165	318	508	897	1,830	3,310	5,360	11,000
700	14	23	52	106	159	306	488	862	1,760	3,180	5,150	10,600
750	13	26	50	102	153	295	470	830	1,690	3,060	4,960	10,200
800	12	26	48	99	148	285	454	802	1,640	2,960	4,790	9,840
850	12	25	46	95	143	275	439	776	1,580	2,860	4,640	9,530
	11	24	45	93	139	267	426	752	1,530	2,780	4,500	9,240

950	11	23	44	90	135	259	413	731	1,490	2,700	4,370	8,970
1,000	11	23	43	87	131	252	402	711	1,450	2,620	4,250	8,720
1,100	10	21	40	83	124	240	382	675	1,380	2,490	4,030	8,290
1,200	NA	20	39	79	119	229	364	644	1,310	2,380	3,850	7,910
1,300	NA	20	37	76	114	219	349	617	1,260	2,280	3,680	7,570
1,400	NA	19	35	73	109	210	335	592	1,210	2,190	3,540	7,270
1,500	NA	18	34	70	105	203	323	571	1,160	2,110	3,410	7,010
1,600	NA	18	33	68	102	196	312	551	1,120	2,030	3,290	6,770
1,700	NA	17	32	66	98	189	302	533	1,090	1,970	3,190	6,550
1,800	NA	16	31	64	95	184	293	517	1,050	1,910	3,090	6,350
1,900	NA	16	30	62	93	178	284	502	1,020	1,850	3,000	6,170
2,000	NA	16	29	60	90	173	276	488	1,000	1,800	2,920	6,000

Note: All table entries are rounded to 3 significant digits.

Table 6.2.1(b) Schedule 40 Metallic Pipe

		licuuic										
-	_	-	-	-	-	-	-	-	-	-		<u>Gas:</u>
											D	<u>Inlet</u>
-	-	-	-	-	-	-	-	-	-	-		essure:
											<u> </u>	ressure Drop:
-	-	-	-	-	-	-	-	-	-	-		<u>Specific</u>
_	_	_	_	_	_	_	_	_	_	_		Gravity:
							Pipe	e Size (<u>in.)</u>		1	
Nominal:	1/2	3/4	<u>1</u>	<u>1</u> ¹ /4	<u>1</u> ½	2	<u>2</u> ¹ / ₂	3	<u>4</u>	<u>5</u>	6	8
Actual												
ID:	<u>0.622</u>	<u>0.824</u>	<u>1.049</u>	<u>1.380</u>	<u>1.610</u>	<u>2.067</u>	<u>2.469</u>	<u>3.068</u>	<u>4.026</u>	<u>5.047</u>	<u>6.065</u>	<u>7.981</u>
<u>Length</u>												
(<u>ft</u>)					<u>Ca</u>	<u>pacity i</u>	n Cubi	c Feet	of Gas	<u>per Ho</u>	<u>ur</u>	
10	172	360	678	1,390	2,090	4,020	6,400	11,300	23,100	41,800	67,600	139,000
20	118	247	466	957	1,430	2,760	4,400	7,780	15,900	28,700	46,500	95,500
30	95	199	374	768	1,150	2,220	3,530	6,250	12,700	23,000	37,300	76,700
40	81	170	320	657	985	1,900	3,020	5,350	10,900	19,700	31,900	65,600
50	72	151	284	583	873	1,680	2,680	4,740	9,660	17,500	28,300	58,200
60	65	137	257	528	791	1,520	2,430	4,290	8,760	15,800	25,600	52,700
70	60	126	237	486	728	1,400	2,230	3,950	8,050	14,600	23,600	48,500
80	56	117	220	452	677	1,300	2,080	3,670	7,490	13,600	22,000	45,100
90	52	110	207	424	635	1,220	1,950	3,450	7,030	12,700	20,600	42,300
100	50	104	195	400	600	1,160	1,840	3,260	6,640	12,000	19,500	40,000
125	44	92	173	355	532	1,020	1,630	2,890	5,890	10,600	17,200	35,400
150	40	83	157	322	482	928	1,480	2,610	5,330	9,650	15,600	32,100
175	37	77	144	296	443	854	1,360	2,410	4,910	8,880	14,400	29,500
200	34	71	134	275	412	794	1,270	2,240	4,560	8,260	13,400	27,500
250	30	63	119	244	366	704	1,120	1,980	4,050	7,320	11,900	24,300
300	27	57	108	221	331	638	1,020	1,800	3,670	6,630	10,700	22,100

350	25	53	99	203	305	587	935	1,650	3,370	6,100	9,880	20,300
400	23	49	92	189	283	546	870	1,540	3,140	5,680	9,190	18,900
450	22	46	86	177	266	512	816	1,440	2,940	5,330	8,620	17,700
500	21	43	82	168	251	484	771	1,360	2,780	5,030	8,150	16,700
550	20	41	78	159	239	459	732	1,290	2,640	4,780	7,740	15,900
600	19	39	74	152	228	438	699	1,240	2,520	4,560	7,380	15,200
650	18	38	71	145	218	420	669	1,180	2,410	4,360	7,070	14,500
700	17	36	68	140	209	403	643	1,140	2,320	4,190	6,790	14,000
750	17	35	66	135	202	389	619	1,090	2,230	4,040	6,540	13,400
800	16	34	63	130	195	375	598	1,060	2,160	3,900	6,320	13,000
850	16	33	61	126	189	363	579	1,020	2,090	3,780	6,110	12,600
900	15	32	59	122	183	352	561	992	2,020	3,660	5,930	12,200
950	15	31	58	118	178	342	545	963	1,960	3,550	5,760	11,800
1,000	14	30	56	115	173	333	530	937	1,910	3,460	5,600	11,500
1,100	14	28	53	109	164	316	503	890	1,810	3,280	5,320	10,900
1,200	13	27	51	104	156	301	480	849	1,730	3,130	5,070	10,400
1,300	12	26	49	100	150	289	460	813	1,660	3,000	4,860	9,980
1,400	12	25	47	96	144	277	442	781	1,590	2,880	4,670	9,590
1,500	11	24	45	93	139	267	426	752	1,530	2,780	4,500	9,240
1,600	11	23	44	89	134	258	411	727	1,480	2,680	4,340	8,920
1,700	11	22	42	86	130	250	398	703	1,430	2,590	4,200	8,630
1,800	10	22	41	84	126	242	386	682	1,390	2,520	4,070	8,370
1,900	10	21	40	81	122	235	375	662	1,350	2,440	3,960	8,130
2,000	NA	20	39	79	119	229	364	644	1,310	2,380	3,850	7,910
	400 450 500 550 600 650 700 750 800 850 900 950 1,000 1,100 1,200 1,300 1,300 1,400 1,500 1,600 1,700 1,800 1,900	4002345022500215502060019650187001775017800168501690015950151,000141,200131,300121,400121,500111,600111,700111,800101,90010	4002349450224650021435502041600193965018387001736750173580016348501633900153295015311,00014281,20013271,30012261,40012251,50011231,70011221,80010221,9001021	4002349924502246865002143825502041786001939746501838717001736687501735668001634638501633619001532599501531581,0001428531,2001327511,3001226491,4001225471,5001123441,7001122421,8001022411,900102140	4002349921894502246861775002143821685502041781596001939741526501838711457001736681407501735661358001634631308501633611269001532591229501531581181,0001428531091,2001327511041,3001226491001,400122547961,500112344891,700112242861,800102241841,90010214081	4002349921892834502246861772665002143821682515502041781592396001939741522286501838711452187001736681402097501735661352028001634631301958501633611261899001532591221839501531581181781,0001428531091641,2001327511041561,3001226491001501,400122547961441,500112344891341,700112242861301,800102241841261,90010214081122	4002349921892835464502246861772665125002143821682514845502041781592394596001939741522284386501838711452184207001736681402094037501735661352023898001634631301953758501633611261893639001532591221833529501531581181783421,0001428531091643161,2001327511041563011,3001226491001502891,400122547961442771,500112344891342581,700112242861302501,800102241841262421,90010214081122235	4002349921892835468704502246861772665128165002143821682514847715502041781592394597326001939741522284386996501838711452184206697001736681402094036437501735661352023896198001634631301953755988501633611261893635799001532591221833525619501531581181733335301,0001430561151733335301,2001327511041563014801,300122547961442774421,500112445931392674261,600112242861302503981,800102241841262423861,90010214081122235375	4002349921892835468701,5404502246861772665128161,4405002143821682514847711,3605502041781592394597321,2906001939741522284386991,2406501838711452184206691,1807001736681402094036431,1407501735661352023896191,0908001634631301953755981,0608501632591221833525619929001532591221833525619929501531581181783425459631,0001430561151733335309371,1001428531091643165038901,20013275111041563014808491,300122547961442774427811,500112445931392674267521,60011234489134 <td>4002349921892835468701,5403,1404502246861772665128161,4402,9405002143821682514847711,3602,7805502041781592394597321,2902,6406001939741522284386991,2402,5206501838711452184206691,1802,4107001736681402094036431,1402,3207501735661352023896191,0902,2308001634631301953755981,0602,16085016336111261893635791,0202,0909001532591221833525619922,0209501531581181783425459631,9601,0001430561151733335309371,9101,1001428531091643165038901,8101,2001327511041563014808491,7301,300122547961442774</td> <td>4002349921892835468701,5403,1405,6804502246861772665128161,4402,9405,3305002143821682514847711,3602,7805,0305502041781592394597321,2902,6404,7806001939741522284386991,2402,5204,5606501838711452184206691,1802,4104,3607001736681402094036431,1402,3204,0408001634631301953755981,0602,1603,9008501633611261893635791,0202,0903,7809001532591221833525619922,0203,6609501531581181783425459631,9603,2801,0001430561151733335309371,9103,4601,1001428531091643165038901,8103,2801,2001327511041563014808491,7303,1301,40012<!--</td--><td>4002349921892835468701,5403,1405,6809,1904502246861772665128161,4402,9405,3308,6205002143821682514847711,3602,7805,0308,1505502041781592394597321,2902,6404,7807,7406001939741522284386991,2402,5204,5607,3806501838711452184206691,1802,4104,3607,0707001736681402094036431,1402,3204,0406,5407501735661352023896191,0902,2304,0406,5408001634631301953755981,0602,1603,9006,3208501633611261893635791,0202,0903,7806,1109001532591221833525619922,0203,6605,9309501531581181783425459631,9603,5505,7601,0001430561151733335309371,9103,4605,6</td></td>	4002349921892835468701,5403,1404502246861772665128161,4402,9405002143821682514847711,3602,7805502041781592394597321,2902,6406001939741522284386991,2402,5206501838711452184206691,1802,4107001736681402094036431,1402,3207501735661352023896191,0902,2308001634631301953755981,0602,16085016336111261893635791,0202,0909001532591221833525619922,0209501531581181783425459631,9601,0001430561151733335309371,9101,1001428531091643165038901,8101,2001327511041563014808491,7301,300122547961442774	4002349921892835468701,5403,1405,6804502246861772665128161,4402,9405,3305002143821682514847711,3602,7805,0305502041781592394597321,2902,6404,7806001939741522284386991,2402,5204,5606501838711452184206691,1802,4104,3607001736681402094036431,1402,3204,0408001634631301953755981,0602,1603,9008501633611261893635791,0202,0903,7809001532591221833525619922,0203,6609501531581181783425459631,9603,2801,0001430561151733335309371,9103,4601,1001428531091643165038901,8103,2801,2001327511041563014808491,7303,1301,40012 </td <td>4002349921892835468701,5403,1405,6809,1904502246861772665128161,4402,9405,3308,6205002143821682514847711,3602,7805,0308,1505502041781592394597321,2902,6404,7807,7406001939741522284386991,2402,5204,5607,3806501838711452184206691,1802,4104,3607,0707001736681402094036431,1402,3204,0406,5407501735661352023896191,0902,2304,0406,5408001634631301953755981,0602,1603,9006,3208501633611261893635791,0202,0903,7806,1109001532591221833525619922,0203,6605,9309501531581181783425459631,9603,5505,7601,0001430561151733335309371,9103,4605,6</td>	4002349921892835468701,5403,1405,6809,1904502246861772665128161,4402,9405,3308,6205002143821682514847711,3602,7805,0308,1505502041781592394597321,2902,6404,7807,7406001939741522284386991,2402,5204,5607,3806501838711452184206691,1802,4104,3607,0707001736681402094036431,1402,3204,0406,5407501735661352023896191,0902,2304,0406,5408001634631301953755981,0602,1603,9006,3208501633611261893635791,0202,0903,7806,1109001532591221833525619922,0203,6605,9309501531581181783425459631,9603,5505,7601,0001430561151733335309371,9103,4605,6

Note: All table entries are rounded to 3 significant digits.

Table 6.2.1(c) Schedule 40 Metallic Pipe

-	-	-	-	-	-		<u>Gas:</u>	<u>Natural</u>				
-	_	_	_	_	-	Inlet	Pressure:	Less tha	<u>n 2 psi</u>			
-	_	_	_	_	-	<u>3.0 in. w</u>	3.0 in. w.c.					
-	_	-	-	-	-	<u>Specifi</u>	<u>c Gravity:</u>	<u>0.60</u>	-			
Ī	NTEND	ED USE	: Initial	supply	pressu	re of 8.0 ir	<u>. w.c. or g</u>	<u>reater</u>				
_		NDED USE: Initial supply pressure of 8.0 in. w.c. or greater Pipe Size (in.)										
Nominal:	¹ /2											
Actual ID:	<u>0.622</u>	<u>0.824</u>	<u>1.049</u>	<u>1.380</u>	<u>1.610</u>	<u>2.067</u>	<u>2.469</u>	<u>3.068</u>	<u>4.026</u>			
Length (ft)			Cap	acity in	Thousa	ands of Bt	<u>u per Hou</u>	<u>r</u>	·			
10	454	949	1,790	3,670	5,500	10,600	16,900	29,800	60,800			
20	312	652	1,230	2,520	3,780	7,280	11,600	20,500	41,800			
30	250	524	986	2,030	3,030	5,840	9,310	16,500	33,600			
40	214	448	844	1,730	2,600	5,000	7,970	14,100	28,700			
50	190	397	748	1,540	2,300	4,430	7,060	12,500	25,500			
60	172	360	678	1,390	2,090	4,020	6,400	11,300	23,100			

-	_	_	-	-	_		<u>Gas:</u>	<u>Natural</u>	
_	_	_	_	_	_	Inlet	Pressure:	Less tha	<u>n 2 psi</u>
_	_	_	_	_	_	Press	ure Drop:	3.0 in. w	.c.
-	_	_	_	_	_	Specifi	c Gravity:	0.60	
		ED USE	: Initial	- vlaauz	pressu		. w.c. or g		
						<u>ize (in.)</u>	3		
- <u>Nominal:</u>	¹ /2	³ /4	<u>1</u>	<u>11/4</u>	<u>1¹/2</u>	<u>2</u>	<u>2</u> ¹ / ₂	<u>3</u>	<u>4</u>
Actual ID:	0.622	0.824	1.049	1.380	<u>1.610</u>	2.067	2.469	<u>3.068</u>	4.026
Length (ft)							<u>u per Hour</u>		
70	158	331	624	1,280	1,920	3,690	5,890	10,400	21,200
80	147	308	580	1,190	1,790	3,440	5,480	9,690	19,800
90	138	289	544	1,120	1,670	3,230	5,140	9,090	18,500
100	131	273	514	1,060	1,580	3,050	4,860	8,580	17,500
125	116	242	456	936	1,400	2,700	4,300	7,610	15,500
150	105	219	413	848	1,270	2,450	3,900	6,890	14,100
175	96	202	380	780	1,170	2,250	3,590	6,340	12,900
200	90	188	353	726	1,090	2,090	3,340	5,900	12,000
250	80	166	313	643	964	1,860	2,960	5,230	10,700
300	72	151	284	583	873	1,680	2,680	4,740	9,660
350	66	139	261	536	803	1,550	2,470	4,360	8,890
400	62	129	243	499	747	1,440	2,290	4,050	8,270
450	58	121	228	468	701	1,350	2,150	3,800	7,760
500	55	114	215	442	662	1,280	2,030	3,590	7,330
550	52	109	204	420	629	1,210	1,930	3,410	6,960
600	50	104	195	400	600	1,160	1,840	3,260	6,640
650	47	99	187	384	575	1,110	1,760	3,120	6,360
700	46	95	179	368	552	1,060	1,690	3,000	6,110
750	44	92	173	355	532	1,020	1,630	2,890	5,890
800	42	89	167	343	514	989	1,580	2,790	5,680
850	41	86	162	332	497	957	1,530	2,700	5,500
900	40	83	157	322	482	928	1,480	2,610	5,330
950	39	81	152	312	468	901	1,440	2,540	5,180
1000	38	79	148	304	455	877	1,400	2,470	5,040
1100	36	75	141	289	432	833	1,330	2,350	4,780
1200	34	71	134	275	412	794	1,270	2,240	4,560
1300	33	68	128	264	395	761	1,210	2,140	4,370
1400	31	65	123	253	379	731	1,160	2,060	4,200
1500	30	63	119	244	366	704	1,120	1,980	4,050
1600	29	61	115	236	353	680	1,080	1,920	3,910
1700	28	59	111	228	342	658	1,050	1,850	3,780
1800	27	57	108	221	331	638	1,020	1,800	3,670
1900	27	56	105	215	322	619	987	1,750	3,560
2000	26	54	102	209	313	602	960	1,700	3,460

Note: All table entries are rounded to 3 significant digits. Table 6.2.1(d) Schedule 40 Metallic Pipe Gas: Natural Inlet Pressure: Less than 2 psi Pressure Drop: 6.0 in. w.c. Specific Gravity: 0.6 INTENDED USE: Initial supply pressure of 11.0 in. w.c. or greater Pipe Size (in.) 3⁄4 Nominal: 1/2 1 11/4 11/2 2 **2**¹/₂ 3 4 Actual ID: 0.622 0.824 1.049 1.38 2.067 1.61 2.469 3.068 4.026 Length (ft) Capacity in Cubic Feet of Gas per Hour 10 2,600 660 1,380 5,340 8,000 15,400 24,600 43,400 88,500 20 454 949 1,790 3,670 5,500 10,600 16,900 29,800 60,800 30 364 762 1,440 2,950 4,410 8,500 13,600 24,000 48,900 40 312 652 1,230 2,520 3,780 7,280 11,600 20,500 41,800 50 276 2,240 3,350 6,450 10,300 578 1,090 18,200 37,100 250 60 524 986 2,030 3,030 5,840 9,310 16,500 33,600 70 230 482 907 1,860 2,790 5,380 8,570 15,100 30,900 80 214 448 844 1,730 2,600 5,000 7,970 14,100 28,700 90 201 420 792 1,630 2,440 4,690 7,480 13,200 27,000 100 190 397 748 1,540 2,300 4,430 7,060 12,500 25,500 125 168 352 663 1,360 2,040 3,930 6,260 11,100 22,600 1,230 20,500 150 153 319 601 1,850 3,560 5,670 10,000 175 5,220 140 293 553 1,140 1,700 3,270 9,230 18,800 8,580 200 131 514 1.056 1,580 4,860 17,500 273 3,050 250 116 242 456 936 1,400 2,700 4,300 7,610 15,500 300 413 848 3,900 105 219 1,270 2,450 6,890 14,100 350 96 202 380 780 1,170 2,250 3,590 6,340 12,900 400 90 188 353 726 1,090 2,090 3,340 5,900 12,000 450 84 176 332 681 1,020 1,960 3,130 5,540 11,300 500 313 643 1,860 2,960 5,230 10,700 80 166 964 550 76 158 297 611 915 1,760 2,810 4,970 10,100 600 72 151 284 583 873 1,680 2,680 4,740 9,660 650 69 144 272 558 836 1,610 2,570 4,540 9,250 700 66 139 261 536 803 1,550 2,470 4,360 8,890 750 64 134 252 516 774 1,490 2,380 4,200 8,560 1,440 2,290 800 62 129 243 499 747 4,050 8,270 850 60 125 235 483 723 1,390 2,220 3,920 8,000 900 58 121 228 468 701 1,350 2,150 3,800 7,760 950 56 118 221 454 681 1,310 2,090 3,690 7,540 55 215 442 1,280 2,030 1,000 114 662 3,590 7,330 1,100 52 109 204 420 629 1,210 1,930 6,960 3,410 1,200 50 104 195 400 600 1,160 1,840 3,260 6,640

1,300	47	99	187	384	575	1,110	1,760	3,120	6,360
1,400	46	95	179	368	552	1,060	1,690	3,000	6,110
1,500	44	92	173	355	532	1,020	1,630	2,890	5,890
1,600	42	89	167	343	514	989	1,580	2,790	5,680
1,700	41	86	162	332	497	957	1,530	2,700	5,500
1,800	40	83	157	322	482	928	1,480	2,610	5,330
1,900	39	81	152	312	468	901	1,440	2,540	5,180
2,000	38	79	148	304	455	877	1,400	2,470	5,040
Note: All table	entries	are rou	nded to :	3 signific	ant digits	3.			
Table 6.2.1(e				-	5				
	,						Gaoi	Notura	
-	-	-	-	-	-		<u>Gas:</u>	Natura	<u>.</u>
-	-	-	-	-	-		Pressure:	<u>2.0 psi</u>	
-	-	-	-	-	-	Pres	<u>sure Drop:</u>	<u>1.0 psi</u>	
-	-	-	-	-	-	<u>Specif</u>	ic Gravity:	<u>0.60</u>	
-					Pipe Si	<u>ze (in.)</u>			
Nominal:	1 <u>/</u> 2	³ /4	<u>1</u>	<u>11/4</u>	<u>11/</u> 2	<u>2</u>	<u>2</u> ¹ / ₂	<u>3</u>	<u>4</u>
Actual ID:	<u>0.622</u>	<u>0.824</u>	<u>1.049</u>	<u>1.380</u>	<u>1.610</u>	<u>2.067</u>	<u>2.469</u>	<u>3.068</u>	<u>4.026</u>
Length (ft)			<u>Cap</u>	acity in	Cubic F	eet of Gas	<u>per Hour</u>		
10	1,510	3,040	5,560	11,400	17,100	32,900	52,500	92,800	189,000
20	1,070	2,150	3,930	8,070	12,100	23,300	37,100	65,600	134,000
30	869	1,760	3,210	6,590	9,880	19,000	30,300	53,600	109,000
40	753	1,520	2,780	5,710	8,550	16,500	26,300	46,400	94,700
50	673	1,360	2,490	5,110	7,650	14,700	23,500	41,500	84,700
60	615	1,240	2,270	4,660	6,980	13,500	21,400	37,900	77,300
70	569	1,150	2,100	4,320	6,470	12,500	19,900	35,100	71,600
80	532	1,080	1,970	4,040	6,050	11,700	18,600	32,800	67,000
90	502	1,010	1,850	3,810	5,700	11,000	17,500	30,900	63,100
100	462	004							=
125	102	934	1,710	3,510	5,260	10,100	16,100	28,500	58,200
150	414	934 836	1,710 1,530	3,510 3,140	5,260 4,700	10,100 9,060	16,100 14,400	28,500 25,500	58,200 52,100
100									
175	414	836	1,530	3,140	4,700	9,060	14,400 13,000 12,000	25,500	52,100
	414 372	836 751	1,530 1,370	3,140 2,820	4,700 4,220	9,060 8,130	14,400 13,000	25,500 22,900	52,100 46,700
175	414 372 344	836 751 695	1,530 1,370 1,270	3,140 2,820 2,601	4,700 4,220 3,910	9,060 8,130 7,530	14,400 13,000 12,000	25,500 22,900 21,200	52,100 46,700 43,300
175 200	414 372 344 318	836 751 695 642	1,530 1,370 1,270 1,170	3,140 2,820 2,601 2,410	4,700 4,220 3,910 3,610	9,060 8,130 7,530 6,960	14,400 13,000 12,000 11,100	25,500 22,900 21,200 19,600	52,100 46,700 43,300 40,000
175 200 250	414 372 344 318 279	836 751 695 642 583	1,530 1,370 1,270 1,170 1,040	3,140 2,820 2,601 2,410 2,140	4,700 4,220 3,910 3,610 3,210	9,060 8,130 7,530 6,960 6,180	14,400 13,000 12,000 11,100 9,850	25,500 22,900 21,200 19,600 17,400	52,100 46,700 43,300 40,000 35,500
175 200 250 300	414 372 344 318 279 253	836 751 695 642 583 528	1,530 1,370 1,270 1,170 1,040 945	3,140 2,820 2,601 2,410 2,140 1,940	4,700 4,220 3,910 3,610 3,210 2,910	9,060 8,130 7,530 6,960 6,180 5,600	14,400 13,000 12,000 11,100 9,850 8,920	25,500 22,900 21,200 19,600 17,400 15,800	52,100 46,700 43,300 40,000 35,500 32,200
175 200 250 300 350	414 372 344 318 279 253 232	836 751 695 642 583 528 486	1,530 1,370 1,270 1,170 1,040 945 869	3,140 2,820 2,601 2,410 2,140 1,940 1,790	4,700 4,220 3,910 3,610 3,210 2,910 2,670	9,060 8,130 7,530 6,960 6,180 5,600 5,150	14,400 13,000 12,000 11,100 9,850 8,920 8,210	25,500 22,900 21,200 19,600 17,400 15,800 14,500	52,100 46,700 43,300 40,000 35,500 32,200 29,600
175 200 250 300 350 400	414 372 344 318 279 253 232 216	836 751 695 642 583 528 486 452	1,530 1,370 1,270 1,170 1,040 945 869 809	3,140 2,820 2,601 2,410 2,140 1,940 1,790 1,660	4,700 4,220 3,910 3,610 3,210 2,910 2,670 2,490	9,060 8,130 7,530 6,960 6,180 5,600 5,150 4,790	14,400 13,000 12,000 11,100 9,850 8,920 8,210 7,640	25,500 22,900 21,200 19,600 17,400 15,800 14,500 13,500	52,100 46,700 43,300 40,000 35,500 32,200 29,600 27,500
175 200 250 300 350 400 450	414 372 344 318 279 253 232 216 203	836 751 695 642 583 528 486 452 424	1,530 1,370 1,270 1,170 1,040 945 869 809 759	3,140 2,820 2,601 2,410 2,140 1,940 1,790 1,660 1,560	4,700 4,220 3,910 3,610 3,210 2,910 2,670 2,490 2,330	9,060 8,130 7,530 6,960 6,180 5,600 5,150 4,790 4,500	14,400 13,000 12,000 11,100 9,850 8,920 8,210 7,640 7,170	25,500 22,900 21,200 19,600 17,400 15,800 14,500 13,500 12,700 12,000 11,400	52,100 46,700 43,300 40,000 35,500 32,200 29,600 27,500 25,800
175 200 250 300 350 400 450 500 550 600	414 372 344 318 279 253 232 216 203 192	836 751 695 642 583 528 486 452 424 401	1,530 1,370 1,270 1,170 1,040 945 869 809 759 717	3,140 2,820 2,601 2,410 2,140 1,940 1,790 1,660 1,560 1,470	4,700 4,220 3,910 3,610 3,210 2,910 2,670 2,490 2,330 2,210 2,090 2,000	9,060 8,130 7,530 6,960 6,180 5,600 5,150 4,790 4,500 4,250	14,400 13,000 12,000 11,100 9,850 8,920 8,210 7,640 7,170 6,770	25,500 22,900 21,200 17,400 15,800 14,500 13,500 12,700 12,000	52,100 46,700 43,300 40,000 35,500 32,200 29,600 27,500 25,800 24,400
175 200 250 300 350 400 450 500	414 372 344 318 279 253 232 216 203 192 182	836 751 695 642 583 528 486 452 424 401 381	1,530 1,370 1,270 1,170 1,040 945 869 809 759 717 681	3,140 2,820 2,601 2,410 2,140 1,940 1,790 1,660 1,560 1,470 1,400	4,700 4,220 3,910 3,610 3,210 2,910 2,670 2,490 2,330 2,210 2,090	9,060 8,130 7,530 6,960 6,180 5,600 5,150 4,790 4,500 4,250 4,030	14,400 13,000 12,000 11,100 9,850 8,920 8,210 7,640 7,170 6,770 6,430	25,500 22,900 21,200 19,600 17,400 15,800 14,500 13,500 12,700 12,000 11,400	52,100 46,700 43,300 40,000 35,500 32,200 29,600 27,500 25,800 24,400 23,200

-	-	-	_	-	-		<u>Gas:</u>	Natura	<u> </u>
_	_	_	_	_	_	Inlet	Pressure:	2.0 psi	
_	_	_	_	_	_	Press	sure Drop:	1.0 psi	
-		-	-	-	-		ic Gravity:		
	_				- <u>Pipe S</u>	ize_(in.)			
Nominal:	1/2	3/4	<u>1</u>	<u>11/4</u>	<u>11/2</u>	2	<u>2</u> ¹ / ₂	<u>3</u>	<u>4</u>
Actual ID:	<u>0.622</u>	<u>0.824</u>	<u>1.049</u>	1.380	<u>1.610</u>	2.067	2.469	3.068	<u>4.026</u>
Length (ft)			Cap		Cubic F	eet of Gas	per Hour		
750	154	322	576	1,180	1,770	3,410	5,440	9,610	19,600
800	149	311	556	1,140	1,710	3,290	5,250	9,280	18,900
850	144	301	538	1,100	1,650	3,190	5,080	8,980	18,300
900	139	292	522	1,070	1,600	3,090	4,930	8,710	17,800
950	135	283	507	1,040	1,560	3,000	4,780	8,460	17,200
1,000	132	275	493	1,010	1,520	2,920	4,650	8,220	16,800
1,100	125	262	468	960	1,440	2,770	4,420	7,810	15,900
1,200	119	250	446	917	1,370	2,640	4,220	7,450	15,200
1,300	114	239	427	878	1,320	2,530	4,040	7,140	14,600
1,400	110	230	411	843	1,260	2,430	3,880	6,860	14,000
1,500	106	221	396	812	1,220	2,340	3,740	6,600	13,500
1,600	102	214	382	784	1,180	2,260	3,610	6,380	13,000
1,700	99	207	370	759	1,140	2,190	3,490	6,170	12,600
1,800	96	200	358	736	1,100	2,120	3,390	5,980	12,200
1,900	93	195	348	715	1,070	2,060	3,290	5,810	11,900
1,900 2,000	93 91	195 189	348 339	715 695	1,070 1,040	2,060 2,010	3,290 3,200	5,810 5,650	11,900 11,500
	91	189	339	695	1,040	2,010			
2,000 ote: All table	91 entries	189 are rou	339 nded to	695 3 signific	1,040	2,010			
2,000 ote: All table	91 entries	189 are rou	339 nded to	695 3 signific	1,040	2,010			
2,000 ote: All table	91 entries	189 are rou	339 nded to	695 3 signific	1,040	2,010 s.	3,200 <u>Gas:</u>	5,650 Natural	
2,000	91 entries	189 are rou	339 nded to	695 3 signific	1,040	2,010 s. <u>Inlet F</u>	3,200 <u>Gas:</u> Pressure:	5,650 <u>Natural</u> <u>3.0 psi</u>	
2,000 ote: All table	91 entries	189 are rou	339 nded to	695 3 signific	1,040	2,010 s. <u>Inlet F</u> <u>Press</u>	3,200 <u>Gas:</u> Pressure: ure Drop:	5,650 Natural 3.0 psi 2.0 psi	
2,000 ote: All table	91 entries	189 are rou	339 nded to	695 3 signific	1,040 cant digit - - - -	2,010 s. <u>Inlet F</u> <u>Press</u> <u>Specific</u>	3,200 <u>Gas:</u> Pressure:	5,650 Natural 3.0 psi 2.0 psi	
2,000 ote: All table able 6.2.1(f) - - - - - -	91 e entries Schedu - - - -	189 are roui ile 40 M - - - -	339 nded to etallic P - - - -	695 3 signific ipe - - - -	1,040 cant digit - - - - - - - - - - - - -	2,010 s. <u>Inlet F</u> <u>Pressi Specific</u> ize (in.)	3,200 Gas: Pressure: ure Drop: Gravity:	5,650 <u>Natural</u> <u>3.0 psi</u> <u>2.0 psi</u> <u>0.60</u>	11,500
2,000 ote: All table able 6.2.1(f) - - - - - - Nominal:	91 e entries Schedu - - - - 1/2	189 are roun ile 40 M - - - - 3 <u>⁄</u> 4	339 nded to etallic P - - - - - 1	695 3 signific ipe - - - - - - - -	1,040 cant digit - - - - <u>-</u> - <u>-</u> - <u>Pipe S <u>1</u>½</u>	2,010 s. <u>Inlet F</u> <u>Pressi Specific</u> ize (in.) <u>2</u>	3,200 <u>Gas:</u> <u>Pressure:</u> <u>ure Drop:</u> <u>: Gravity:</u> <u>2</u> ¹ / ₂	5,650 <u>Natural</u> <u>3.0 psi</u> <u>2.0 psi</u> <u>0.60</u> <u>3</u>	<u>11,500</u>
2,000 ote: All table able 6.2.1(f) - - - - Nominal: Actual ID:	91 e entries Schedu - - - -	189 are roui ile 40 M - - - -	339 nded to etallic P - - - - 1 <u>1</u> 1.049	695 3 signific ipe - - - - - - 1 <u>1/</u> 4 <u>1.380</u>	1,040 cant digit - - - <u>-</u> - <u>-</u> <u>-</u> <u>-</u> <u>-</u> <u>-</u> <u>-</u> <u>-</u>	2,010 s. <u>Inlet F</u> <u>Presse</u> <u>Specific</u> <u>ize (in.)</u> <u>2</u> <u>2.067</u>	3,200 <u>Gas:</u> <u>Pressure:</u> <u>ure Drop:</u> <u>c Gravity:</u> <u>2¹/2</u> <u>2.469</u>	5,650 <u>Natural</u> <u>3.0 psi</u> <u>2.0 psi</u> <u>0.60</u>	11,500
2,000 ote: All table able 6.2.1(f) - - - - - <u>-</u> - <u>-</u> - <u>-</u> <u>-</u> <u>-</u> <u>-</u> <u></u>	91 e entries Schedu - - - 1/2 0.622	189 are roun ile 40 Mr - - - 3/4 <u>0.824</u>	339 nded to etallic P - - - <u>1</u> <u>1.049</u> <u>Cap</u>	695 3 signific ipe - - - - <u>11/4</u> <u>1.380</u> acity in	1,040 cant digit - - - <u>-</u> - <u>-</u> <u>-</u> <u>1½</u> <u>1.610</u> Cubic F	2,010 s. <u>Inlet F</u> <u>Pressi Specific</u> <u>ize (in.)</u> <u>2</u> <u>2.067</u> <u>eet of Gas</u>	3,200 <u>Gas:</u> <u>Pressure:</u> <u>ure Drop:</u> <u>21/2</u> <u>2.469</u> <u>per Hour</u>	5,650 Natural 3.0 psi 2.0 psi 0.60 3 3.068	<u>4</u> <u>4</u>
2,000 ote: All table able 6.2.1(f) - - - - <u>-</u> - Nominal: <u>Actual ID:</u> Length (ft) 10	91 e entries Schedu - - - 1/2 0.622 2,350	189 are roun ile 40 M - - - 3 <u>/</u> 4 0.824 4,920	339 nded to etallic P - - - - <u>1</u> <u>1.049</u> 9,270	695 3 signific ipe - - - - - - <u>11/4</u> <u>1.380</u> acity in 19,000	1,040 cant digit - - - <u>-</u> <u>-</u> <u>-</u> <u>-</u> <u>1¹/2 <u>1.610</u> <u>Cubic F</u> 28,500</u>	2,010 s. <u>Inlet F</u> <u>Presse</u> <u>Specific</u> ize (in.) <u>2</u> <u>2.067</u> <u>eet of Gas</u> 54,900	3,200 <u>Gas:</u> <u>Pressure:</u> <u>ure Drop:</u> <u>c Gravity:</u> <u>21/2</u> <u>2.469</u> <u>a per Hour</u> 87,500	5,650 Natural 3.0 psi 2.0 psi 0.60 3.068 3.068 155,000	<u>4</u> <u>4.026</u> 316,000
2,000 ote: All table able 6.2.1(f) - - - - - <u>-</u> - Nominal: Actual ID: Length (ft) 10 20	91 e entries Schedu - - - 1/2 0.622 2,350 1,620	189 are roun ile 40 Mr - - - 3/4 0.824 4,920 3,380	339 nded to etallic P - - - <u>1</u> <u>1.049</u> 9,270 6,370	695 3 signific ipe - - - - <u>11/4</u> <u>1.380</u> acity in 19,000 13,100	1,040 cant digit - - - <u>-</u> <u>-</u> <u>1½</u> <u>1.610</u> <u>Cubic F</u> 28,500 19,600	2,010 s. <u>Inlet F</u> <u>Pressi Specific</u> <u>ize (in.)</u> <u>2</u> <u>2.067</u> <u>eet of Gas</u> 54,900 37,700	3,200 <u>Gas:</u> <u>Pressure:</u> <u>ure Drop:</u> <u>21/2</u> <u>2.469</u> <u>per Hour</u> 87,500 60,100	5,650 Natural 3.0 psi 2.0 psi 0.60 3 155,000 106,000	<u>4</u> <u>4.026</u> 316,000 217,000
2,000 ote: All table able 6.2.1(f) - - - - - <u>-</u> - Nominal: Actual ID: Length (ft) 10 20 30	91 e entries Schedu - - - 1/2 0.622 2,350 1,620 1,300	189 are roun ile 40 Ma - - - 3 <u>/</u> 4 0.824 4,920 3,380 2,720	339 nded to etallic P - - - 1 1.049 9,270 6,370 5,110	695 3 signific ipe - - - - - - 1 <u>1/4</u> <u>1.380</u> 19,000 13,100 10,500	1,040 cant digit - - - - <u>-</u> - <u>-</u> - <u>-</u> - <u>-</u> - <u>-</u> - <u>-</u> - 2 8,500 19,600 15,700	2,010 s. <u>Inlet F</u> <u>Pressa</u> <u>Specific</u> ize (in.) <u>2</u> <u>2.067</u> <u>eet of Gas</u> 54,900 37,700 30,300	3,200 <u>Gas:</u> <u>Pressure:</u> <u>ure Drop:</u> <u>c Gravity:</u> <u>21/2</u> <u>2.469</u> <u>6 per Hour</u> 87,500 60,100 48,300	5,650 Natural 3.0 psi 2.0 psi 0.60 3.068 155,000 106,000 85,400	11,500 <u>4</u> <u>4.026</u> 316,000 217,000 174,000
2,000 ote: All table able 6.2.1(f) - - - - - - Nominal: Actual ID: Length (ft) 10 20 30 40	91 e entries Schedu - - - 1/2 0.622 2,350 1,620 1,300 1,110	189 are roun ile 40 Mi - - - - 3 <u>⁄</u> 4 0.824 4,920 3,380 2,720 2,320	339 nded to etallic P - - - - <u>1</u> <u>1.049</u> 9,270 6,370 5,110 4,380	695 3 signific ipe - - - - - 1 <u>1/4</u> <u>1.380</u> <u>acity in</u> 19,000 13,100 10,500 8,990	1,040 cant digit - - - - <u>-</u> - <u>-</u> - <u>-</u> - <u>-</u> - <u>-</u> - 2 <u>Pipe Si</u> <u>1½</u> <u>1.610</u> <u>28,500</u> 19,600 15,700 13,500	2,010 s. <u>Inlet F</u> <u>Pressi</u> <u>Specific</u> <u>ize (in.)</u> <u>2</u> <u>2.067</u> <u>eet of Gas</u> 54,900 37,700 30,300 25,900	3,200 <u>Gas:</u> <u>Pressure:</u> <u>ure Drop:</u> <u>21/2</u> <u>21/2</u> <u>2.469</u> <u>9er Hour</u> 87,500 60,100 48,300 41,300	5,650 Natural 3.0 psi 2.0 psi 0.60 3 3.068 3.068 155,000 106,000 85,400 73,100	<u>4</u> <u>4.026</u> 316,000 217,000 174,000 149,000
2,000 ote: All table able 6.2.1(f) - - - - - Nominal: Actual ID: Length (ft) 10 20 30 40 50	91 e entries Schedu - - - - 1/2 0.622 2,350 1,620 1,300 1,110 985	189 are roun ile 40 Ma - - - - 3 <u>⁄</u> 4 0.824 4,920 3,380 2,720 2,320 2,060	339 nded to etallic P - - - - 1 1.049 9,270 6,370 5,110 4,380 3,880	695 3 signific ipe - - - - - - - - - - - - -	1,040 cant digit - - - - - - - - - - - - - - - - - - -	2,010 s. <u>Inlet F</u> <u>Pressi Specific</u> ize (in.) <u>2</u> <u>2.067</u> <u>2.067</u> <u>eet of Gas</u> 54,900 37,700 30,300 25,900 23,000	3,200 <u>Gas:</u> <u>Pressure:</u> <u>ure Drop:</u> <u>5 Gravity:</u> <u>21/2</u> <u>2.469</u> <u>9 per Hour</u> 87,500 60,100 48,300 41,300 36,600	5,650 Natural 3.0 psi 2.0 psi 2.0 psi 0.60 3.068 105,000 106,000 85,400 73,100 64,800	11,500 <u>4</u> <u>4.026</u> 316,000 217,000 174,000 132,000
2,000 ote: All table able 6.2.1(f) - - - - - - Nominal: Actual ID: Length (ft) 10 20 30 40	91 e entries Schedu - - - 1/2 0.622 2,350 1,620 1,300 1,110	189 are roun ile 40 Mi - - - - 3 <u>⁄</u> 4 0.824 4,920 3,380 2,720 2,320	339 nded to etallic P - - - - <u>1</u> <u>1.049</u> 9,270 6,370 5,110 4,380	695 3 signific ipe - - - - - 1 <u>1/4</u> <u>1.380</u> <u>acity in</u> 19,000 13,100 10,500 8,990	1,040 cant digit - - - - <u>-</u> - <u>-</u> - <u>-</u> - <u>-</u> - <u>-</u> - 2 <u>Pipe Si</u> <u>1½</u> <u>1.610</u> <u>28,500</u> 19,600 15,700 13,500	2,010 s. <u>Inlet F</u> <u>Pressi</u> <u>Specific</u> <u>ize (in.)</u> <u>2</u> <u>2.067</u> <u>eet of Gas</u> 54,900 37,700 30,300 25,900	3,200 <u>Gas:</u> <u>Pressure:</u> <u>ure Drop:</u> <u>21/2</u> <u>21/2</u> <u>2.469</u> <u>9er Hour</u> 87,500 60,100 48,300 41,300	5,650 Natural 3.0 psi 2.0 psi 0.60 3 3.068 3.068 155,000 106,000 85,400 73,100	<u>11,500</u>

-	-	_	_	-	-		<u>Gas:</u>	<u>Natural</u>	
_	_	_	_	_	_	Inlet	Pressure:	<u>3.0 psi</u>	
_	_	_	_	_	_	Press	ure Drop:	<u>2.0 psi</u>	
_	_	_	_	_	_	<u>Specifi</u>	c Gravity:	0.60	
					Pipe S	ize (in.)			
Nominal:	1/2	3/4	1	<u>11/4</u>	<u>1¹/2</u>	2	<u>2</u> ¹ / ₂	<u>3</u>	<u>4</u>
Actual ID:	0.622	<u>0.824</u>	<u>1.049</u>	1.380	<u>1.610</u>	<u></u> <u>2.067</u>	<u>2.469</u>	3.068	4.026
Length (ft)		<u></u>				1	<u>s per Hour</u>		
90	717	1,500	2,820	5,800	8,680	16,700	26,700	47,100	96,100
100	677	1,420	2,670	5,470	8,200	15,800	25,200	44,500	90,800
125	600	1,250	2,360	4,850	7,270	14,000	22,300	39,500	80,500
150	544	1,140	2,140	4,400	6,590	12,700	20,200	35,700	72,900
175	500	1,050	1,970	4,040	6,060	11,700	18,600	32,900	67,100
200	465	973	1,830	3,760	5,640	10,900	17,300	30,600	62,400
250	412	862	1,620	3,330	5,000	9,620	15,300	27,100	55,300
300	374	781	1,470	3,020	4,530	8,720	13,900	24,600	50,100
350	344	719	1,350	2,780	4,170	8,020	12,800	22,600	46,100
400	320	669	1,260	2,590	3,870	7,460	11,900	21,000	42,900
450	300	627	1,180	2,430	3,640	7,000	11,200	19,700	40,200
500	283	593	1,120	2,290	3,430	6,610	10,500	18,600	38,000
550	269	563	1,060	2,180	3,260	6,280	10,000	17,700	36,100
600	257	537	1,010	2,080	3,110	5,990	9,550	16,900	34,400
650	246	514	969	1,990	2,980	5,740	9,150	16,200	33,000
700	236	494	931	1,910	2,860	5,510	8,790	15,500	31,700
750	228	476	897	1,840	2,760	5,310	8,470	15,000	30,500
800	220	460	866	1,780	2,660	5,130	8,180	14,500	29,500
850	213	445	838	1,720	2,580	4,960	7,910	14,000	28,500
900	206	431	812	1,670	2,500	4,810	7,670	13,600	27,700
950	200	419	789	1,620	2,430	4,670	7,450	13,200	26,900
1,000	195	407	767	1,580	2,360	4,550	7,240	12,800	26,100
1,100	185	387	729	1,500	2,240	4,320	6,890	12,200	24,800
1,200	177	369	695	1,430	2,140	4,120	6,570	11,600	23,700
1,300	169	353	666	1,370	2,050	3,940	6,290	11,100	22,700
1,400	162	340	640	1,310	1,970	3,790	6,040	10,700	21,800
1,500	156	327	616	1,270	1,900	3,650	5,820	10,300	21,000
1,600	151	316	595	1,220	1,830	3,530	5,620	10,000	20,300
1,700	146	306	576	1,180	1,770	3,410	5,440	9,610	19,600
1,800	142	296	558	1,150	1,720	3,310	5,270	9,320	19,000
1,900	138	288	542	1,110	1,670	3,210	5,120	9,050	18,400
2,000	134	280	527	1,080	1,620	3,120	4,980	8,800	18,000
lote: All table able 6.2.1(g				-	cant digit	S.			
	, conou						Gas:	Natural	

_	_	_	_	_	_	Inlet	Pressure:	<u>5.0 psi</u>	
_	_	_	_	_	_	Press	sure Drop:	<u>3.5 psi</u>	
-	-	-	-	-	-		ic Gravity:	0.60	
	-		-	-	- Pipe Si	ize (in.)			
- Nominal:	1 <u>/2</u>	³ /4	1	<u>1</u> ¹ /4	<u><u>1</u>¹/₂</u>	<u>2</u>	<u>2</u> ¹ / ₂	<u>3</u>	<u>4</u>
	0.622	<u>0.824</u>		<u>1.380</u>					
Actual ID:	<u>U.022</u>	<u>0.024</u>	<u>1.049</u>	1	<u>1.610</u>	<u>2.067</u>	<u>2.469</u>	<u>3.068</u>	<u>4.026</u>
Length (ft)	0.400	0.400					s per Hour	100.000	404.000
10	3,190	6,430		24,200		69,700	111,000	196,000	401,000
20	2,250	4,550	8,320		25,600	49,300	78,600	139,000	283,000
30	1,840	3,720	6,790	14,000		40,300	64,200	113,000	231,000
40	1,590	3,220	5,880	12,100	18,100	34,900	55,600	98,200	200,000
50	1,430	2,880	5,260	10,800	16,200	31,200	49,700	87,900	179,000
60	1,300	2,630	4,800	9,860	14,800	28,500	45,400	80,200	164,000
70	1,200	2,430	4,450	9,130	13,700	26,400	42,000	74,300	151,000
80	1,150	2,330	4,260	8,540	12,800	24,700	39,300	69,500	142,000
90	1,060	2,150	3,920	8,050	12,100	23,200	37,000	65,500	134,000
100	979	1,980	3,620	7,430	11,100	21,400	34,200	60,400	123,000
125	876	1,770	3,240	6,640	9,950	19,200	30,600	54,000	110,000
150	786	1,590	2,910	5,960	8,940	17,200	27,400	48,500	98,900
175	728	1,470	2,690	5,520	8,270	15,900	25,400	44,900	91,600
200	673	1,360	2,490	5,100	7,650	14,700	23,500	41,500	84,700
250	558	1,170	2,200	4,510	6,760	13,000	20,800	36,700	74,900
300	506	1,060	1,990	4,090	6,130	11,800	18,800	33,300	67,800
350	465	973	1,830	3,760	5,640	10,900	17,300	30,600	62,400
400	433	905	1,710	3,500	5,250	10,100	16,100	28,500	58,100
450	406	849	1,600	3,290	4,920	9,480	15,100	26,700	54,500
500	384	802	1,510	3,100	4,650	8,950	14,300	25,200	51,500
550	364	762	1,440	2,950	4,420	8,500	13,600	24,000	48,900
600	348	727	1,370	2,810	4,210	8,110	12,900	22,900	46,600
650	333	696	1,310	2,690	4,030	7,770	12,400	21,900	44,600
700	320	669	1,260	2,590	3,880	7,460	11,900	21,000	42,900
750	308	644	1,210	2,490	3,730	7,190	11,500	20,300	41,300
800	298	622	1,170	2,410	3,610	6,940	11,100	19,600	39,900
850	288	602	1,130	2,330	3,490	6,720	10,700	18,900	38,600
900	279	584	1,100	2,260	3,380	6,520	10,400	18,400	37,400
950	271	567	1,070	2,190	3,290	6,330	10,100	17,800	36,400
1,000	264	551	1,040	2,130	3,200	6,150	9,810	17,300	35,400
1,100	250	524	987	2,030	3,030	5,840	9,320	16,500	33,600
1,200	239	500	941	1,930	2,900	5,580	8,890	15,700	32,000
1,300	229	478	901	1,850	2,770	5,340	8,510	15,000	30,700
1,400	220	460	866	1,780	2,660	5,130	8,180	14,500	29,500
1,500	212	443	834	1,710	2,570	4,940	7,880	13,900	28,400
1,600	205	428	806	1,650	2,480	4,770	7,610	13,400	27,400

	I	I	I	I	I			I	I		I
1,700	198				·	2,400	4,620			8,000	26,500
1,800	192				·	2,330	4,480			2,600	25,700
1,900	186				·	2,260	4,350	· · ·		2,300	25,000
2,000	18	1 37	9 7	14 1	,470	2,200	4,230	6,74	40 11	,900	24,300
Note: All ta	ble entr	ies are	rounde	d to 3 s	significa	ant digit	s.				
Table 6.2. ²	I(h) Sen	nirigid (Copper	Tubing							
-	-	-	-	-	-	_	-		<u>Gas:</u>	Natu	<u>iral</u>
_	_	_	_	_	_	_	_	Inlet Pr	ressure:	Less than 2 psi	
_	_	_	_	_	_	_	_	<u>Pressu</u>	re Drop:	<u>0.3 i</u>	n. w.c.
									<u>Specific</u> <u>Gravity:</u>		
-	-	-	-	-	-	- Tube	- Size (i				
-	- K &	<u>Tube Size (in.)</u>									
Nominal:	<u>L:</u>	1 <u>/4</u>	³ ⁄8	1 <u>/2</u>	⁵ ⁄8	3⁄4	<u>1</u>	<u>1¼</u>	4 <u>1</u> ¹ /2		<u>2</u>
	ACR:	³ ⁄8	1 <u>/2</u>	5 <u>⁄8</u>	³ /4	⁷ /8	<u>11/8</u>	<u>1³⁄</u> 8			=
<u>0</u>	<u>utside:</u>	<u>0.375</u>	<u>0.500</u>	<u>0.625</u>	<u>0.750</u>	<u>0.875</u>	<u>1.125</u>	<u>1.375</u>	<u>1.625</u>		2.125
<u>h</u>	nside: [*]	<u>0.305</u>	<u>0.402</u>	<u>0.527</u>	<u>0.652</u>	<u>0.745</u>	<u>0.995</u>	<u>1.245</u>	<u>1.481</u>		<u>1.959</u>
<u>Length</u>	<u>(ft)</u>			<u>Cap</u>	acity i	n Cubio	: Feet c	of Gas pe	er Hour		
10		20	42	85	148	210	448	806	1,270	2	2,650
20		14	29	58	102	144	308	554	873	1	1,820
30		11	23	47	82	116	247	445	701	1	1,460
40		10	20	40	70	99	211	381	600	1	1,250
50		NA	17	35	62	88	187	337	532	1	1,110
60		NA	16	32	56	79	170	306	482	1	,000,I
70		NA	14	29	52	73	156	281	443		924
80		NA	13	27	48	68	145	262	413		859
90		NA	13	26	45	64	136	245	387		806
100		NA	12	24	43	60	129	232	366		761
125		NA	11	22	38	53	114	206	324		675
150		NA	10	20	34	48	103	186	294		612
175		NA	NA	18	31	45	95	171	270		563
200		NA	NA	17	29	41	89	159	251		523
250		NA	NA	15	26	37	78	141	223		464
300		NA	NA	13	23	33	71	128	202		420
350		NA	NA	12	22	31	65	118	186		387
400		NA	NA	11	20	28	61	110	173		360
450		NA	NA	11	19	27	57	103	162		338
500		NA	NA	10	18	25	54	97	153		319
550		NA	NA	NA	17	24	51	92	145		303
600		NA	NA	NA	16	23	49	88	139		289
650		NA	NA	NA	15	22	47	84	133		277
700		NA	NA	NA	15	21	45	81	128		266

750	NA	NA	NA	14	20	43	78	123	256
800	NA	NA	NA	14	20	42	75	119	247
850	NA	NA	NA	13	19	40	73	115	239
900	NA	NA	NA	13	18	39	71	111	232
950	NA	NA	NA	13	18	38	69	108	225
1,000	NA	NA	NA	12	17	37	67	105	219
1,100	NA	NA	NA	12	16	35	63	100	208
1,200	NA	NA	NA	11	16	34	60	95	199
1,300	NA	NA	NA	11	15	32	58	91	190
1,400	NA	NA	NA	10	14	31	56	88	183
1,500	NA	NA	NA	NA	14	30	54	84	176
1,600	NA	NA	NA	NA	13	29	52	82	170
1,700	NA	NA	NA	NA	13	28	50	79	164
1,800	NA	NA	NA	NA	13	27	49	77	159
1,900	NA	NA	NA	NA	12	26	47	74	155
2,000	NA	NA	NA	NA	12	25	46	72	151

Note: All table entries are rounded to 3 significant digits.

^{*}Table capacities are based on Type K copper tubing inside diameter (shown), which has the smallest inside diameter of the copper tubing products.

Table 6.2.1(i) Semirigid Copper Tubing

								Gasi	Natural		
-	-	-	-	-	-	-		<u>Gas:</u>			
-	-	-	-	-	-	-		ressure:	Less the		
-	-	-	-	-	-	-	<u>Pressu</u>	ire Drop:	<u>0.5 in. w.c.</u>		
-	_	-	_	_	-	-	<u>Specific</u>	Gravity:	<u>0.60</u>		
_	-					Tube S	<u> Size (in.)</u>				
	<u>K & L:</u>	1/4	³ /8	1 <u>/2</u>	5 <u>⁄8</u>	³ /4	<u>1</u>	<u>1</u> ¹ /4	<u>1</u> ¹ / ₂	<u>2</u>	
Nominal:	ACR:	³ ⁄8	1 <u>/2</u>	⁵ /8	³ /4	7 <u>∕</u> 8	<u>1</u> ½	<u>1</u> ³ /8	=	=	
<u>0</u>	utside:	<u>0.375</u>	<u>0.500</u>	<u>0.625</u>	<u>0.750</u>	<u>0.875</u>	<u>1.125</u>	<u>1.375</u>	<u>1.625</u>	<u>2.125</u>	
Į	nside: [*]	<u>0.305</u>	<u>0.402</u>	<u>0.527</u>	<u>0.652</u>	<u>0.745</u>	<u>0.995</u>	<u>1.245</u>	<u>1.481</u>	<u>1.959</u>	
<u>Length</u>	<u>(ft)</u>			Capa	city in	Cubic F	Feet of Ga	as per Ho	ur		
10		27	55	111	195	276	590	1,060	1,680	3,490	
20		18	38	77	134	190	406	730	1,150	2,400	
30		15	30	61	107	152	326	586	925	1,930	
40		13	26	53	92	131	279	502	791	1,650	
50		11	23	47	82	116	247	445	701	1,460	
60		10	21	42	74	105	224	403	635	1,320	
70		NA	19	39	68	96	206	371	585	1,220	
80		NA	18	36	63	90	192	345	544	1,130	
90		NA	17	34	59	84	180	324	510	1,060	
100		NA	16	32	56	79	170	306	482	1,000	
125		NA	14	28	50	70	151	271	427	890	

-	-	-	_	-	-	-		<u>Gas:</u>	<u>Natural</u>	
_	_	_	_	_	_	_	Inlet F	Pressure:	Less the	an 2 psi
-	_	_	_	_	_	_	Pressu	ure Drop:	<u>0.5 in. v</u>	/.C.
_	_	_	_	_	_	_	Specific	Gravity:	0.60	
						Tube S	<u>Size (in.)</u>			
_	<u>-</u> K & L:	1/4	3/8	1/2	5/8	3/4	1	<u>1</u> ¹ /4	<u>11/2</u>	2
Nominal:	ACR:	3/8	1/2	5/8	3/4	7/8	<u>1</u> ¹ /8	<u>1</u> ³ /8		_
C)utside:	0.375	0.500	0.625	0.750	0.875	1.125	1.375	1.625	2.125
	Inside: [*]	0.305	0.402	0.527	0.652	0.745	0.995	1.245	1.481	1.959
		0.303	0.402					<u>1.245</u> as per Ho		1.303
Length		NA	13	26	45		136			806
150						64		245	387 256	
175 200		NA NA	12 11	24 22	41 39	59 55	125 117	226 210	356 331	742 690
200		NA	NA	22	39 34	55 48	103	186	294	690 612
300		NA	NA	18	31	40	94	169	294	554
350		NA	NA	16	28	44 40	94 86	155	200 245	554 510
400		NA	NA	15	26	38	80	144	243	474
450		NA	NA	14	25	35	75	135	214	445
500		NA	NA	13	23	33	71	128	202	420
550		NA	NA	13	22	32	68	122	192	399
600		NA	NA	12	21	30	64	116	183	381
650		NA	NA	12	20	29	62	111	175	365
700		NA	NA	11	20	28	59	107	168	350
750		NA	NA	11	19	27	57	103	162	338
800)	NA	NA	10	18	26	55	99	156	326
850)	NA	NA	10	18	25	53	96	151	315
900)	NA	NA	NA	17	24	52	93	147	306
950)	NA	NA	NA	17	24	50	90	143	297
1,00	0	NA	NA	NA	16	23	49	88	139	289
1,10	0	NA	NA	NA	15	22	46	84	132	274
1,20	0	NA	NA	NA	15	21	44	80	126	262
1,30	0	NA	NA	NA	14	20	42	76	120	251
1,40	0	NA	NA	NA	13	19	41	73	116	241
1,50	0	NA	NA	NA	13	18	39	71	111	232
1,60	0	NA	NA	NA	13	18	38	68	108	224
1,70	0	NA	NA	NA	12	17	37	66	104	217
1,80	0	NA	NA	NA	12	17	36	64	101	210
1,90		NA	NA	NA	11	16	35	62	98	204
2,00	0	NA	NA	NA	11	16	34	60	95	199

Note: All table entries are rounded to 3 significant digits.

^{*}Table capacities are based on Type K copper tubing inside diameter (shown), which has the smallest inside diameter of the copper tubing products.

-	_	_	_	_	-	_		Gas:	<u>Natural</u>	
_	_	_	_	_	_	_	Inlet P	ressure:	Less the	an 2 psi
_	_	_	_	_	_	_	Pressu	ire Drop:	<u>1.0 in. v</u>	/.C.
-	-	-	-	-	-	_	Specific	Gravity:	0.60	
	- DED US	E: Tub	- e Sizin	- a Betwo	- een Ho	- use Lin		tor and th		nce.
				<u> </u>			bize (in.)			
-	- K & L:	1/4	3⁄8	1/2	5/8	3/4	<u>1</u>	<u>1</u> ¼	<u>1</u> ½	2
Nominal:	ACR:	^{7_4} ³ ⁄8	1 <u>/2</u>	5 <u>⁄8</u>	^{7_0} ³ /4	7_4		<u>1</u> ³ / ₈	1 /2	<u> </u>
				-		-	<u>11/8</u>			
	outside:	<u>0.375</u>	<u>0.500</u>	<u>0.625</u>	<u>0.750</u>	<u>0.875</u>	<u>1.125</u>	<u>1.375</u>	<u>1.625</u>	<u>2.125</u>
	nside:*	<u>0.305</u>	<u>0.402</u>	<u>0.527</u>	<u>0.652</u>	<u>0.745</u>	<u>0.995</u>	<u>1.245</u>	<u>1.481</u>	<u>1.959</u>
<u>Length</u>	<u>(ft)</u>						eet of Ga	as per Hou	<u>ur</u>	1
10		39	80	162	283	402	859	1,550	2,440	5,080
20		27	55	111	195	276	590	1,060	1,680	3,490
30		21	44	89	156	222	474	853	1,350	2,800
40		18	38	77	134	190	406	730	1,150	2,400
50		16	33	68	119	168	359	647	1,020	2,130
60		15	30	61	107	152	326	586	925	1,930
70		13	28	57	99	140	300	539	851	1,770
80		13	26	53	92	131	279	502	791	1,650
90		12	24	49	86	122	262	471	742	1,550
100		11	23	47	82	116	247	445	701	1,460
125		NA	20	41	72	103	219	394	622	1,290
150		NA	18	37	65	93	198	357	563	1,170
175		NA	17	34	60	85	183	329	518	1,080
200		NA	16	32	56	79	170	306	482	1,000
250		NA	14	28	50	70	151	271	427	890
300		NA	13	26	45	64	136	245	387	806
350		NA	12	24	41	59	125	226	356	742
400		NA	11	22	39	55	117	210	331	690
450		NA	10	21	36	51	110	197	311	647
500		NA	NA	20	34	48	103	186	294	612
550		NA	NA	19	32	46	98	177	279	581
600		NA	NA	18	31	44	94	169	266	554
650		NA	NA	17	30	42	90	162	255	531
700		NA	NA	16	28	40	86	155	245	510
750		NA	NA	16	27	39	83	150	236	491
800		NA	NA	15	26	38	80	144	228	474
850		NA	NA	15	26	36	78	140	220	459
900		NA	NA	14	25	35	75	135	214	445
950		NA	NA	14	24	34	73	132	207	432
1,00		NA NA	NA NA	13 13	23 22	33 32	71 68	128 122	202 192	420 399

1,200	NA	NA	12	21	30	64	116	183	381
1,300	NA	NA	12	20	29	62	111	175	365
1,400	NA	NA	11	20	28	59	107	168	350
1,500	NA	NA	11	19	27	57	103	162	338
1,600	NA	NA	10	18	26	55	99	156	326
1,700	NA	NA	10	18	25	53	96	151	315
1,800	NA	NA	NA	17	24	52	93	147	306
1,900	NA	NA	NA	17	24	50	90	143	297
2,000	NA	NA	NA	16	23	49	88	139	289

Note: All table entries are rounded to 3 significant digits.

*Table capacities are based on Type K copper tubing inside diameter (shown), which has the smallest inside diameter of the copper tubing products.

Table 6.2.1(k) Semirigid Copper Tubing

-	_	-	_	-	-	-		<u>Gas:</u>	<u>Natural</u>	
_	_	_	_	_	_	_	Inlet P	ressure:	<u>Less tha</u>	<u>n 2.0 psi</u>
_	_	_	_	_	_	_	Pressu	re Drop:	17.0 in. v	V.C.
							Specific	Gravity:	0.60	
	-	-	-	-	-	Tube	Size (in.)			
-	- K & L:	1/4	3⁄8	1/2	5/8	3/4	<u> </u>	<u>1¼</u>	<u>1</u> ½	<u>2</u>
Nominal:	ACR:	- ³ ⁄8	- 1/2	- 5 <u>⁄8</u>	3/4	7/8		<u>1³⁄8</u>	=	
0	utside:		0.500	0.625	<u></u>	0.875	<u>1.125</u>	<u>1.375</u>	<u> </u>	<u></u> <u>2.125</u>
	nside:*	0.305	0.402	0.527	0.652	0.745	0.995	1.245	1.481	1.959
Length	n_(ft)					Cubic	Feet of G		our	<u> </u>
10		190	391	796	1,390	1,970	4,220	7,590	12,000	24,900
20		130	269	547	956	1,360	2,900	5,220	8,230	17,100
30		105	216	439	768	1,090	2,330	4,190	6,610	13,800
40		90	185	376	657	932	1,990	3,590	5,650	11,800
50		79	164	333	582	826	1,770	3,180	5,010	10,400
60		72	148	302	528	749	1,600	2,880	4,540	9,460
70		66	137	278	486	689	1,470	2,650	4,180	8,700
80		62	127	258	452	641	1,370	2,460	3,890	8,090
90		58	119	243	424	601	1,280	2,310	3,650	7,590
100		55	113	229	400	568	1,210	2,180	3,440	7,170
125	5	48	100	203	355	503	1,080	1,940	3,050	6,360
150)	44	90	184	321	456	974	1,750	2,770	5,760
175	;	40	83	169	296	420	896	1,610	2,540	5,300
200)	38	77	157	275	390	834	1,500	2,370	4,930
250)	33	69	140	244	346	739	1,330	2,100	4,370
300)	30	62	126	221	313	670	1,210	1,900	3,960
350)	28	57	116	203	288	616	1,110	1,750	3,640
400)	26	53	108	189	268	573	1,030	1,630	3,390

-	_	-	_	-	-	_		<u>Gas:</u>	Nat	ural	
_	_	-	_	_	_	_	Inlet P	ressure:	Les	s thar	<u>1 2.0 psi</u>
_	_	_	_	_	_	_	Pressu	ire Drop:	17.0) in. w	. <u></u>
							Specific	Gravity:	0.60)	
	_	_		-	-	Tube	<u>Size (in.)</u>			-	
-	- K & L:	1/4	3⁄8	1 <u>/2</u>	5/8	3/4	<u>1</u>	<u>1</u> ¼	1	1/2	<u>2</u>
Nominal:		^{7_4} ³ ⁄8		5 <u>/8</u>	³ /4	7/8					
	<u>ACR:</u>	<u>/</u> 8 0.375	¹ / ₂				<u>1</u> ¹ / <u>8</u>	<u>1³/8</u>		=	2 1 2 5
	utside:		0.500	0.625	0.750	0.875	<u>1.125</u>	<u>1.375</u>		<u>625</u>	2.125
-	nside:*	<u>0.305</u>	<u>0.402</u>	<u>0.527</u>	<u>0.652</u>	0.745	<u>0.995</u>	<u>1.245</u>		<u>481</u>	<u>1.959</u>
<u>Length</u>								<u>ias per Ho</u>			
450		24	50	102	177	252	538	968		530	3,180
500		23	47	96	168	238	508	914		40	3,000
550		22	45	91	159	226	482	868		370	2,850
600		21	43	87	152	215	460	829		810	2,720
650		20	41	83	145	206	441	793	1,2	250	2,610
700		19	39	80	140	198	423	762	1,2	200	2,500
750		18	38	77	135	191	408	734	1,1	60	2,410
800		18	37	74	130	184	394	709	1,1	20	2,330
850		17	35	72	126	178	381	686	1,0	080	2,250
900		17	34	70	122	173	370	665	1,0)50	2,180
950		16	33	68	118	168	359	646	1,0)20	2,120
1,000	C	16	32	66	115	163	349	628	99	91	2,060
1,10	С	15	31	63	109	155	332	597	94	41	1,960
1,200	С	14	29	60	104	148	316	569	89	98	1,870
1,300	С	14	28	57	100	142	303	545	86	60	1,790
1,400	C	13	27	55	96	136	291	524	82	26	1,720
1,500	C	13	26	53	93	131	280	505	79	96	1,660
1,600	C	12	25	51	89	127	271	487	76	68	1,600
1,70	C	12	24	49	86	123	262	472	74	14	1,550
1,800	C	11	24	48	84	119	254	457	72	21	1,500
1,900	C	11	23	47	81	115	247	444	70	00	1,460
2,000	C	11	22	45	79	112	240	432	68	31	1,420
ote: All ta āble capa nallest ins able 6.2.1	acities ai side diar	re base neter of	d on Ty f the co	pe K co pper tul	opper tu	bing in		eter (show	/n), v	vhich I	has the
_	_	_	_	_	_			G	as:	Natur	al
-	-	-	-	-	-	-	Inl	et Pressu	_	2.0 ps	
-	-	-	-	-	-	-		essure Dr		1.0 ps	
-	-	-	-	-	-	-		cific Grav		0.60	_
-	-	-	-	-	-	- Tubo	Size (in.)		<u></u>	<u></u>	
-	-	1.	2,	4.	E /				.		
Nominal:	K & L:	1/4	3/8	1/2	5/8	3/4	1	<u><u>1</u>¹/2</u>	4	<u>1¹/2</u>	<u>2</u>

<u>AC</u>	R: 3/8	1 <u>/2</u>	⁵ /8	³ /4	⁷ /8	<u>11/8</u>	<u>1³⁄</u> 8	=	=
<u>Outsic</u>	de: 0.375	<u>0.500</u>	<u>0.625</u>	<u>0.750</u>	<u>0.875</u>	<u>1.125</u>	<u>1.375</u>	<u>1.625</u>	<u>2.125</u>
Insid	<u>e:* 0.305</u>	<u>0.402</u>	<u>0.527</u>	<u>0.652</u>	<u>0.745</u>	<u>0.995</u>	<u>1.245</u>	<u>1.481</u>	<u>1.959</u>
Length (ft)			Capac	city in C	ubic Fe	et of Gas	per Hour		
10	245	506	1,030	1,800	2,550	5,450	9,820	15,500	32,200
20	169	348	708	1,240	1,760	3,750	6,750	10,600	
30	135	279	568	993	1,410	3,010	5,420	8,550	17,800
40	116	239	486	850	1,210	2,580	4,640	7,310	15,200
50	103	212	431	754	1,070	2,280	4,110	6,480	13,500
60	93	192	391	683	969	2,070	3,730	5,870	12,200
70	86	177	359	628	891	1,900	3,430	5,400	11,300
80	80	164	334	584	829	1,770	3,190	5,030	10,500
90	75	154	314	548	778	1,660	2,990	4,720	9,820
100	71	146	296	518	735	1,570	2,830	4,450	9,280
125	63	129	263	459	651	1,390	2,500	3,950	8,220
150	57	117	238	416	590	1,260	2,270	3,580	7,450
175	52	108	219	383	543	1,160	2,090	3,290	6,850
200	49	100	204	356	505	1,080	1,940	3,060	6,380
250	43	89	181	315	448	956	1,720	2,710	5,650
300	39	80	164	286	406	866	1,560	2,460	5,120
350	36	74	150	263	373	797	1,430	2,260	4,710
400	33	69	140	245	347	741	1,330	2,100	4,380
450	31	65	131	230	326	696	1,250	1,970	4,110
500	30	61	124	217	308	657	1,180	1,870	3,880
550	28	58	118	206	292	624	1,120	1,770	3,690
600	27	55	112	196	279	595	1,070	1,690	3,520
650	26	53	108	188	267	570	1,030	1,620	3,370
700	25	51	103	181	256	548	986	1,550	3,240
750	24	49	100	174	247	528	950	1,500	3,120
800	23	47	96	168	239	510	917	1,450	3,010
850	22	46	93	163	231	493	888	1,400	2,920
900	22	44	90	158	224	478	861	1,360	2,830
950	21	43	88	153	217	464	836	1,320	2,740
1,000	20	42	85	149	211	452	813	1,280	2,670
1,100	19	40	81	142	201	429	772	1,220	2,540
1,200	18	38	77	135	192	409	737	1,160	2,420
1,300	18	36	74	129	183	392	705	1,110	2,320
1,400	17	35	71	124	176	376	678	1,070	2,230
1,500	16	34	68	120	170	363	653	1,030	2,140
1,600	16	33	66	116	164	350	630	994	2,070
1,700	15	31	64	112	159	339	610	962	2,000
1,800	15	30	62	108	154	329	592	933	1,940
1,900	14	30	60	105	149	319	575	906	1,890
2,000	14	29	59	102	145	310	559	881	1,830

	ide diam				y produc					
Table 6.2.1(m) Semi	irigid Co	pper Tu	bing					1	
-	-	-	-	-	-	-		<u>Gas:</u>	Natura	<u>l</u>
-	-	-	-	-	-	-	Inlet P	ressure:	<u>2.0 psi</u>	
-	-	-	_	_	_	_	<u>Pressu</u>	<u>re Drop:</u>	<u>1.5 psi</u>	
-	-	-	_	-	-	_		<u>Specific</u> Gravity:	<u>0.60</u>	
INTENDED	D USE: F	Pipe Siz						House L	ine Reg	ulator
					d Suppl		-			
<u>Si</u>	<u>ngle Ho</u>	use Lin	<u>e Regul</u>	ator No				Feet per	Hour.*	
-	_				<u></u>	ube Size	<u>ə (in.)</u>	1		
Nominal:	<u>K & L:</u>	1/4	³ /8	1 <u>/2</u>	⁵ ⁄8	³ /4	1	<u>1¼</u>	<u>1½</u>	<u>2</u>
<u>Nominal.</u>	<u>ACR:</u>	³ /8	1 <u>/</u> 2	⁵ ⁄8	³ /4	⁷ /8	<u>1</u> ½	<u>1³⁄</u> 8	=	=
<u>0</u>	utside:	<u>0.375</u>	<u>0.500</u>	<u>0.625</u>	<u>0.750</u>	<u>0.875</u>	<u>1.125</u>	<u>1.375</u>	<u>1.625</u>	<u>2.12</u>
<u>lı</u>	nside:†	0.305	0.402	<u>0.527</u>	<u>0.652</u>	<u>0.745</u>	<u>0.995</u>	<u>1.245</u>	<u>1.481</u>	1.95
Length	(ft)			Capaci	ty in Cເ	bic Fee	t of Gas	per Hou	r	1
10		303	625	1,270	2,220	3,150	6,740	12,100	-	39,80
20		208	430	874	1,530	2,170	4,630	8,330	13,100	27,40
30		167	345	702	1,230	1,740	3,720	6,690	10,600	22,00
40		143	295	601	1,050	1,490	3,180	5,730	9,030	18,80
50		127	262	532	931	1,320	2,820	5,080	8,000	16,70
60		115	237	482	843	1,200	2,560	4,600	7,250	15,10
70		106	218	444	776	1,100	2,350	4,230	6,670	13,90
80		98	203	413	722	1,020	2,190	3,940	6,210	12,90
90		92	190	387	677	961	2,050	3,690	5,820	12,10
100		87	180	366	640	907	1,940	3,490	5,500	11,50
125		77	159	324	567	804	1,720	3,090	4,880	10,20
150		70	144	294	514	729	1,560	2,800	4,420	9,200
175		64	133	270	472	670	1,430	2,580	4,060	8,460
200		60 53	124	252	440	624	1,330	2,400	3,780	7,870
250 300		48	110 99	223 202	390 353	553 501	1,180 1,070	2,130 1,930	3,350 3,040	6,980 6,320
350		40 44	99 91	186	325	461	984	1,930	2,790	5,820
400		41	85	173	302	429	916	1,650	2,600	5,410
450		39	80	162	283	402	859	1,550	2,440	5,080
500		36	75	153	268	380	811	1,460	2,300	4,800
550		35	72	146	254	361	771	1,390	2,190	4,560
600		33	68	139	243	344	735	1,320	2,090	4,350
650		32	65	133	232	330	704	1,270	2,000	4,160
700		30	63	128	223	317	676	1,220	1,920	4,000
750		29	60	123	215	305	652	1,170	1,850	3,850

800	28	58	119	208	295	629	1,130	1,790	3,720
850	27	57	115	201	285	609	1,100	1,730	3,600
900	27	55	111	195	276	590	1,060	1,680	3,490
950	26	53	108	189	268	573	1,030	1,630	3,390
1,000	25	52	105	184	261	558	1,000	1,580	3,300
1,100	24	49	100	175	248	530	954	1,500	3,130
1,200	23	47	95	167	237	505	910	1,430	2,990
1,300	22	45	91	160	227	484	871	1,370	2,860
1,400	21	43	88	153	218	465	837	1,320	2,750
1,500	20	42	85	148	210	448	806	1,270	2,650
1,600	19	40	82	143	202	432	779	1,230	2,560
1,700	19	39	79	138	196	419	753	1,190	2,470
1,800	18	38	77	134	190	406	731	1,150	2,400
1,900	18	37	74	130	184	394	709	1,120	2,330
2,000	17	36	72	126	179	383	690	1,090	2,270

*When this table is used to size the tubing upstream of a line pressure regulator, the pipe or tubing downstream of the line pressure regulator shall be sized using a pressure drop no greater than 1 in. w.c.

†Table capacities are based on Type K copper tubing inside diameter (shown), which has the smallest inside diameter of the copper tubing products.

Table 6.2.1(n) Semirigid Copper Tubing

	()	J -		5						_
-	-	-	-	-	-	-		<u>Gas:</u>	Natura	
-	-	-	_	_	-	_	Inlet F	Pressure:	<u>5.0 psi</u>	
_	-	-	_	_	_	_	Press	ure Drop:	<u>3.5 psi</u>	
_	_	_	_	_	_	_	<u>Specific</u>	<u>: Gravity:</u>	0.60	
-	-	<u>Tube Size (in.)</u>							1	
	<u>K & L:</u>	$\frac{1}{4} \frac{1}{4} \frac{3}{8} \frac{1}{2} \frac{5}{8} \frac{3}{4} \frac{1}{1} \frac{1^{1}}{4}$								<u>2</u>
Nominal:	ACR:	³ ⁄8	1 <u>/2</u>	⁵ ⁄8	³ /4	⁷ /8	<u>1</u> ½	<u>1³⁄</u> 8	=	=
<u>C</u>	Outside:	<u>0.375</u>	<u>0.500</u>	<u>0.625</u>	<u>0.750</u>	<u>0.875</u>	<u>1.125</u>	<u>1.375</u>	<u>1.625</u>	<u>2.125</u>
	Inside:*	<u>0.305</u>	<u>0.402</u>	<u>0.527</u>	<u>0.652</u>	<u>0.745</u>	<u>0.995</u>	<u>1.245</u>	<u>1.481</u>	<u>1.959</u>
<u>Length</u>	<u>(ft)</u>			Capac	<u>ity in C</u>	ubic Fe	et of Gas	per Hour		
10		511	1,050	2,140	3,750	5,320	11,400	20,400	32,200	67,100
20		351	724	1,470	2,580	3,650	7,800	14,000	22,200	46,100
30		282	582	1,180	2,070	2,930	6,270	11,300	17,800	37,000
40		241	498	1,010	1,770	2,510	5,360	9,660	15,200	31,700
50		214	441	898	1,570	2,230	4,750	8,560	13,500	28,100
60		194	400	813	1,420	2,020	4,310	7,750	12,200	25,500
70		178	368	748	1,310	1,860	3,960	7,130	11,200	23,400
80		166	342	696	1,220	1,730	3,690	6,640	10,500	21,800
90		156	321	653	1,140	1,620	3,460	6,230	9,820	20,400
100	ength (ft) 10 5 20 3 30 2 40 2 50 2 60 1 70 1 80 1 90 1 100 1		303	617	1,080	1,530	3,270	5,880	9,270	19,300
125		130	269	547	955	1,360	2,900	5,210	8,220	17,100

-	-	-	_	_	-	-		<u>Gas:</u>	Natura	<u>1</u>
_	-	_	_	_	_	_	Inlet I	Pressure:	<u>5.0 psi</u>	
_	_	_	_	_	_	_	Press	ure Drop:	<u>3.5 psi</u>	
							Specific	c Gravity:	0.60	
		-			1	- Fube Siz				
_	<u>-</u> <u>K & L:</u>	1 <u>/4</u>	³ /8	1 <u>/2</u>	5 <u>⁄8</u>	3/4	<u>1</u>	<u>1</u> ¹ /4	<u>1½</u>	<u>2</u>
Nominal:	ACR:	3/8	1/2	⁵ /8	3/4	7⁄8	<u>1</u> 1/8	<u>1</u> ³ /8	=	=
C	Dutside:	0.375	0.500	0.625	0.750	0.875	1.125	1.375	1.625	2.125
	Inside:*	0.305	0.402	0.527	0.652	0.745	0.995	1.245	1.481	1.959
Length	 n (ft)			Capac	ity in C	ubic Fe	et of Gas	per Hour		
150		118	243	495	866	1,230	2,620	4,720	7,450	15,500
175		109	224	456	796	1,130	2,410	4,350	6,850	14,300
200		101	208	424	741	1,050	2,250	4,040	6,370	13,300
250		90	185	376	657	932	1,990	3,580	5,650	11,800
300		81	167	340	595	844	1,800	3,250	5,120	10,700
350		75	154	313	547	777	1,660	2,990	4,710	9,810
400		69	143	291	509	722	1,540	2,780	4,380	9,120
450		65	134	273	478	678	1,450	2,610	4,110	8,560
500)	62	127	258	451	640	1,370	2,460	3,880	8,090
550		58	121	245	429	608	1,300	2,340	3,690	7,680
600		56	115	234	409	580	1,240	2,230	3,520	7,330
650		53	110	224	392	556	1,190	2,140	3,370	7,020
700		51	106	215	376	534	1,140	2,050	3,240	6,740
750		49	102	207	362	514	1,100	1,980	3,120	6,490
800		48	98	200	350	497	1,060	1,910	3,010	6,270
850		46	95	194	339	481	1,030	1,850	2,910	6,070
900		45	92	188	328	466	1,000	1,790	2,820	5,880
950		43	90	182	319	452	967	1,740	2,740	5,710
1,00	0	42	87	177	310	440	940	1,690	2,670	5,560
1,10	0	40	83	169	295	418	893	1,610	2,530	5,280
1,20	0	38	79	161	281	399	852	1,530	2,420	5,040
1,30	0	37	76	154	269	382	816	1,470	2,320	4,820
1,40	0	35	73	148	259	367	784	1,410	2,220	4,630
1,50	0	34	70	143	249	353	755	1,360	2,140	4,460
1,60	0	33	68	138	241	341	729	1,310	2,070	4,310
1,70	0	32	65	133	233	330	705	1,270	2,000	4,170
1,80	0	31	63	129	226	320	684	1,230	1,940	4,040
1,90	0	30	62	125	219	311	664	1,200	1,890	3,930
2,00	0	29	60	122	213	302	646	1,160	1,830	3,820

*Table capacities are based on Type K copper tubing inside diameter (shown), which has the smallest inside diameter of the copper tubing products.

Table 6.2.1(o) Corrugated Stainless Steel Tubing (CSST)

-	-	-	-	-	-	-	-	-	-	-		<u>Gas:</u>	<u>Natura</u>	1 <u>1</u>
_	_	_	_	_	_	_	_	_	_	_	Pro	Inlet essure:	<u>Less t</u> <u>2 psi</u>	<u>han</u>
-	_	_	_	_	_	_	_	_	_	_	<u>Pı</u>	<u>essure</u> <u>Drop:</u>	<u>0.5 in.</u>	<u>w.c.</u>
_	_	_	_	_	_	_	_	_	_	_		<u>pecific</u> Gravity:	<u>0.60</u>	
_								Tub	e Siz	ze (EH	<u>D)</u>			
Flow Designation:	<u>13</u>	<u>15</u>	<u>18</u>	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	<u>46</u>	<u>48</u>	<u>60</u>	<u>62</u>
<u>Length (ft</u>)					Ca	oaci	<u>ty in</u>	Cul	oic F	eet of	Gas pe	r Hour		
5	46	63	115	134	225	270	471	546	895	1,037	1,790	2,070	3,660	4,140
10	32	44	82	95	161	192	330	383	639	746	1,260	1,470	2,600	2,930
15	25	35	66	77	132	157	267	310	524	615	1,030	1,200	2,140	2,400
20	22	31	58	67	116	137	231	269	456	536	888	1,050	1,850	2,080
25	19	27	52	60	104	122	206	240	409	482	793	936	1,660	1,860
30	18	25	47	55	96	112	188	218	374	442	723	856	1,520	1,700
40	15	21	41	47	83	97	162	188	325	386	625	742	1,320	1,470
50	13	19	37	42	75	87	144	168	292	347	559	665	1,180	1,320
60	12	17	34	38	68	80	131	153	267	318	509	608	1,080	1,200
70	11	16	31	36	63	74	121	141	248	295	471	563	1,000	1,110
80	10	15	29	33	60	69	113	132	232	277	440	527	940	1,040
90	10	14	28	32	57	65	107	125	219	262	415	498	887	983
100	9	13	26	30	54	62	101	118	208	249	393	472	843	933
150	7	10	20	23	42	48	78	91	171	205	320	387	691	762
200	6	9	18	21	38	44	71	82	148	179	277	336	600	661
250	5	8	16	19	34	39	63	74	133	161	247	301	538	591
300	5	7	15	17	32	36	57	67	95	148	226	275	492	540

EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency between different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing. Notes:

(1) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger numbers of bends and/or fittings shall be increased by an equivalent length of tubing to the following equation: L = 1.3n, where L is additional length (ft) of tubing and n is the number of additional fittings and/or bends.

(2) All table entries are rounded to 3 significant digits.

Table 6.2.1(p) Corrugated Stainless Steel Tubing (CSST)

_	_	_	_	_	-	_	-	-	-	-	Gas: Natural
-	_	_	_	_	_	_	_	_	_	_	Inlet Less than Pressure: 2 psi
-	_	_	_	_	_	_	_	_	_	-	Pressure Drop: 3.0 in. w.c.
-	_	_	_	_	_	_	_	_	_	_	<u>Specific</u> <u>Gravity:</u> 0.60

<u>IN</u>		DED	USE	: In	itial	<u>Sup</u>	<u>ply Pr</u>	essur	e of 8.	0 in. v	<u>w.c. or</u>	Greate	<u>ər.</u>	
_							Ţ	ube S	<u>ize (El</u>	<u>HD)</u>				
<u>Flow</u> Designation:	<u>13</u>	<u>15</u>	<u>18</u>	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	<u>46</u>	<u>48</u>	<u>60</u>	<u>62</u>
<u>Length (ft)</u>					<u>Ca</u>	<u>paci</u>	<u>ty in C</u>	Cubic	Feet o	f Gas	per H	<u>our</u>		
5	120	160	277	327	529	649	1,180	1,370	2,140	2423	4,430	5,010	8,800	10,100
10	83	112	197	231	380	462	828	958	1,530	1740	3,200	3,560	6,270	7,160
15	67	90	161	189	313	379	673	778	1,250	1433	2,540	2,910	5,140	5,850
20	57	78	140	164	273	329	580	672	1,090	1249	2,200	2,530	4,460	5,070
25	51	69	125	147	245	295	518	599	978	1123	1,960	2,270	4,000	4,540
30	46	63	115	134	225	270	471	546	895	1029	1,790	2,070	3,660	4,140
40	39	54	100	116	196	234	407	471	778	897	1,550	1,800	3,180	3,590
50	35	48	89	104	176	210	363	421	698	806	1,380	1,610	2,850	3,210
60	32	44	82	95	161	192	330	383	639	739	1,260	1,470	2,600	2,930
70	29	41	76	88	150	178	306	355	593	686	1,170	1,360	2,420	2,720
80	27	38	71	82	141	167	285	331	555	644	1,090	1,280	2,260	2,540
90	26	36	67	77	133	157	268	311	524	609	1,030	1,200	2,140	2,400
100	24	34	63	73	126	149	254	295	498	579	974	1,140	2,030	2,280
150	19	27	52	60	104	122	206	240	409	477	793	936	1,660	1,860
200	17	23	45	52	91	106	178	207	355	415	686	812	1,440	1,610
250	15	21	40	46	82	95	159	184	319	373	613	728	1,290	1,440
300	13	19	37	42	75	87	144	168	234	342	559	665	1,180	1,320

EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency between different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing.

Notes:

(1) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger numbers of bends and/or fittings shall be increased by an equivalent length of tubing to the following equation: L = 1.3n, where L is additional length (ft) of tubing and n is the number of additional fittings and/or bends.

(2) All table entries are rounded to 3 significant digits.

Table 6.2.1(q) Corrugated Stainless Steel Tubing (CSST)

_	_	_	_	_	-	_	_	_	-	_		<u>Gas:</u>	Natura	<u>l</u>
-	_	_	_	_	_	_	_	_	_	_	Pres	<u>Inlet</u> ssure:	<u>Less</u> 2 psi	than
-	_	_	_	_	_	_	_	_	-	_		<u>ssure</u> Drop:	<u>6.0 in.</u>	w.c.
-	_	_	_	_	_	_	_	_	_	_		ecific avity:	<u>0.60</u>	
INT	ENC	DED	USE	: Ini	tial	<u>Sup</u> p	<u>oly Pre</u>	essure	e of 11	.0 in.	w.c. o	r Grea	ter.	
-							I	ube S	<u>ize (E</u>	<u>HD)</u>				
Flow Designation:	<u>13</u>	<u>15</u>	<u>18</u>	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	<u>46</u>	<u>48</u>	<u>60</u>	<u>62</u>
Length (ft)					<u>Ca</u>	<u>paci</u>	<u>ty in C</u>	Cubic	Feet c	of Gas	<u>per H</u>	our		
5	173	229	389	461	737	911	1,690	1,950	3,000	3375	6,280	7,050	12,400	14,260

Interview Interview <t< th=""><th>_</th><th>_</th><th>_</th><th></th><th>_</th><th></th><th>_</th><th>-</th><th>_</th><th>_</th><th>_</th><th></th><th><u>Gas:</u></th><th>Nat</th><th>ural</th></t<>	_	_	_		_		_	-	_	_	_		<u>Gas:</u>	Nat	ural
Internet												Dro			
Interve Top: 6.0 in. w.c. Specific Gravity: 0.60 Interve Specific 0.60 Interve Specific 0.60 Designation: 13 15 18 19 23 25 30 31 37 39 46 48 60 62 Length (ft) Capacity in Cubic Feed Gas per Hour 0.60 7.210 8.800 1.010 15 96 130 227 267 36 52 960 1.110 1.760 1996 3.610 4.100 7.210 8.260 20 83 112 197 23 855 1.370 1440 3.102 3.60 6.270 7.160 25 74 99 176 207 342 417 739 855 1.370 1.60 2.700 3.100 5.620 6.400 30 67 78 140 164 23.920 5.50 5.70	-	-	-	-	-	-	-	-	-	-	-			<u>z p</u> :	51
Internet Gravity: 0.60 Internet Gravity: 0.60 Persignation: 13 15 18 19 23 25 30 31 37 39 46 48 60 62 Length (f) Image: Im	-	_	_	_	_	-	_	-	_	-	_	Pre		<u>6.0</u>	<u>in. w.c.</u>
INTENDED USE: Initial Supply Pressure of 11.0 in. w.c. or Greater. Elow Designation: 13 15 18 19 23 25 30 31 37 39 46 48 60 62 Length (ft) Capacity in Cubic Feet of Gas per Hour Capacity in Cubic Feet of Gas per Hour 8,800 10,100 10 120 160 277 327 529 649 1,80 1,370 2,140 2423 4,430 5,010 8,800 10,100 10 120 160 277 327 529 649 1,180 1,370 2,140 3,120 3,560 6,270 7,160 20 83 112 197 231 380 672 1,090 1249 2,000 3,140 5,620 6,400 30 67 90 161 189 313 379 673 778 1,250 1,433 2,540 2,510 6,400 6,070 5,070 5,01 5,00 3														0 60	h
Flow 13 15 18 19 23 25 30 31 37 39 46 48 60 62 Length (ft) Capacity in Cubic Feet of Gas per Hour 10 120 160 277 527 649 1,80 1,370 2,140 2423 4,430 5.010 8,800 10,100 15 96 130 227 527 429 458 1,530 1740 3,120 3,560 6,270 7,160 20 83 112 197 231 380 662 828 958 1,530 1543 2,900 5,140 5,850 40 57 78 140 164 273 329 580 672 1,090 1249 2,000 2,530 4,460 5,070 50 51 69 125 147 245 255 505 800 956 1,600 3,900 3,840 3,90 <t< td=""><td>- INT</td><td>- FNF</td><td></td><td></td><td>- Ini</td><td>- tial 9</td><td>- Suni</td><td>- olv Pr</td><td>-</td><td>- of 11</td><td>- 0 in</td><td></td><td></td><td></td><td>2</td></t<>	- INT	- FNF			- Ini	- tial 9	- Suni	- olv Pr	-	- of 11	- 0 in				2
Flow Designation: 13 15 18 19 23 25 30 31 37 39 46 48 60 62 Length (ft) Capacity in Cubic Feet of Gas per Hour 10 120 160 277 327 529 649 1,10 1,70 2,40 2423 4,430 5,010 8,800 10,100 15 96 130 227 67 436 532 960 1,110 1,760 1996 3,610 4,100 7,210 8,260 25 74 99 176<207												<u></u>			
Designation: 13 15 18 19 23 25 30 31 37 39 46 48 60 62 Length (ft) Image: Capacity in Cubic Feet of Gas per Hour Capacity in Cubic Feet of Gas per Hour 8.800 10,100 15 96 130 227 67 36 52 960 1,110 1,760 1996 3,610 4,100 7.210 8,260 20 83 112 197 21 380.462 828 958 1,530 1740 3,120 5,620 6,400 25 74 99 176 207 342 1580 1,370 1564 2,700 3,100 5,620 6,400 30 67 90 161 189 313 2,50 1433 2,540 2,910 5,40 5,50 6,60 1,920 3,800 6,60 4,40 6,50 400 162 147 245 50 50 5	- Flow										/				
10 120 160 277 327 529 649 1,180 1,370 2,140 2423 4,430 5,010 8,800 10,100 15 96 130 227 267 436 532 960 1,110 1,760 1996 3,610 4,100 7,210 8,260 20 83 112 197 231 380 462 828 958 1,530 1740 3,120 3,560 6,270 7,160 25 74 99 176 207 342 414 739 855 1,370 1542 2,900 2,530 4,460 5,070 50 51 69 125 147 252 518 599 978 1123 1,900 2,070 3,600 4,140 70 42 58 106 124 209 2,350 3,800 3,800 3,900 3,390 3,840 80 10,110 1,320 3,340 3,550 3,210 3,50 3,210 3,50 3,210 3,50 3		<u>13</u>	<u>15</u>	<u>18</u>	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	<u>46</u>	<u>48</u>	<u>60</u>	<u>) 62</u>
15 96 130 227 267 436 532 960 1,110 1,760 1996 3,610 4,100 7,210 8,260 20 83 112 197 231 380 462 828 958 1,530 1740 3,120 3,560 6,270 7,160 25 74 99 176 207 342 414 739 855 1,370 1564 2,790 3,190 5,620 6,400 30 67 90 161 189 313 379 673 778 1,250 1433 2,540 2,910 5,140 5,850 40 57 78 140 164 273 329 580 672 1,900 1249 2,200 2,530 4,460 5,070 50 51 69 125 147 245 295 518 599 978 1,50 1,800 3,180 3,590 3,840 70 42 58 106 124 209 2,43 37	Length (ft)					<u>Ca</u>	<u>paci</u>	<u>ty in (</u>	Cubic	Feet o	of Gas	<u>per H</u>	our		
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	10	120	160	277	327	529	649	1,180	1,370	2,140	2423	4,430	5,010	8,80	00 10,100
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	15	96	130	227	267	436	532	960	1,110	1,760	1996	3,610	4,100	7,21	10 8,260
30 67 90 161 189 313 379 673 778 1,250 1433 2,540 2,910 5,140 5,850 40 57 78 140 164 273 329 580 672 1,090 1249 2,200 2,530 4,460 5,070 50 51 69 125 147 245 295 518 599 978 1123 1,960 2,270 4,000 4,540 60 46 63 115 134 225 270 471 546 895 1029 1,790 2,070 3,660 4,140 70 42 58 106 124 209 20 435 505 830 956 1,660 1,920 3,390 3,840 80 39 54 100 116 196 234 407 471 778 897 1,50 1,800 3,180 3,590 90 37 51 94 109 185 2138 441 735 </td <td>20</td> <td>83</td> <td>112</td> <td>197</td> <td>231</td> <td>380</td> <td>462</td> <td>828</td> <td>958</td> <td>1,530</td> <td>1740</td> <td>3,120</td> <td>3,560</td> <td>6,27</td> <td>70 7,160</td>	20	83	112	197	231	380	462	828	958	1,530	1740	3,120	3,560	6,27	70 7,160
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	25	74	99	176	207	342	414	739	855	1,370	1564	2,790	3,190	5,62	20 6,400
50 51 69 125 147 245 295 518 599 978 1123 1,960 2,270 4,000 4,540 60 46 63 115 134 225 270 471 546 895 1029 1,790 2,070 3,600 4,140 70 42 58 106 124 209 250 435 505 830 956 1,660 1,920 3,390 3,840 80 39 54 100 116 196 234 407 471 778 897 1,550 1,800 3,180 3,590 3,390 3,840 90 37 51 94 109 185 221 383 444 735 848 1,410 1,700 3,000 3,390 3,000 3,200 2,2340 2,630 100 35 48 89 104 176 210 362 4,474 520 879 974 1,140 2,030 2,280 250 21	30	67	90	161	189	313	379	673	778	1,250	1433	2,540	2,910	5,14	40 5,850
60 46 63 115 134 225 270 471 546 895 1029 1,790 2,070 3,660 4,140 70 42 58 106 124 209 250 435 505 830 956 1,660 1,920 3,390 3,840 80 39 54 100 116 196 234 407 471 778 897 1,550 1,800 3,180 3,590 90 37 51 94 109 185 221 383 444 735 848 1,460 1,700 3,000 3,390 100 35 48 89 104 176 210 363 421 698 806 1,380 1,610 2,850 3,210 150 28 39 73 85 145 172 294 342 573 664 1,130 1,320 2,340 2,630 200 24 34 63 73 126 149 257 98	40	57	78	140	164	273	329	580	672	1,090	1249	2,200	2,530	4,46	60 5,070
70 42 58 106 124 209 250 435 505 830 956 1,660 1,920 3,390 3,840 80 39 54 100 116 196 234 407 471 778 897 1,550 1,800 3,180 3,590 90 37 51 94 109 185 221 383 444 735 848 1,460 1,700 3,000 3,390 100 35 48 89 104 176 210 363 421 698 806 1,380 1,610 2,850 3,210 150 28 39 73 85 145 172 294 342 573 664 1,130 1,320 2,340 2,630 200 24 34 63 73 126 149 254 295 498 579 974 1,140 2,030 2,840 2,040 300 19 27 52 60 104 122 206	50	51	69	125	147	245	295	518	599	978	1123	1,960	2,270	4,00	00 4,540
80 39 54 100 116 196 234 407 471 778 897 1,550 1,800 3,180 3,590 90 37 51 94 109 185 221 383 444 735 848 1,460 1,700 3,000 3,390 100 35 48 89 104 176 210 363 421 698 806 1,380 1,610 2,850 3,210 150 28 39 73 85 145 172 294 342 573 664 1,130 1,320 2,340 2,630 200 24 34 63 73 126 149 254 295 498 579 974 1,140 2,030 2,280 250 21 30 57 66 114 134 226 263 447 520 870 1,020 1,820 2,040 300 19 27 52 60 104 122 206 240 4	60	46	63	115	134	225	270	471	546	895	1029	1,790	2,070	3,66	60 4,140
90 37 51 94 109 185 221 383 444 735 848 1,460 1,700 3,000 3,390 100 35 48 89 104 176 210 363 421 698 806 1,380 1,610 2,850 3,210 150 28 39 73 85 145 172 294 342 573 664 1,130 1,320 2,340 2,630 200 24 34 63 73 126 149 254 295 498 579 974 1,140 2,030 2,280 250 21 30 57 66 114 134 226 263 447 520 870 1,020 1,820 2,040 300 19 27 52 60 104 122 206 240 409 477 793 936 1,660 1,860 EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency between uimbers of bends and/or	70	42	58	106	124	209	250	435	505	830	956	1,660	1,920	3,39	90 3,840
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	80	39	54	100	116	196	234	407	471	778	897	1,550	1,800	3,18	30 3,590
150283973851451722943425736641,1301,3202,3402,630200243463731261492542954985799741,1402,0302,280250213057661141342262634475208701,0201,8202,040300192752601041222062404094777939361,6601,860EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency betweendifferent tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing.Notes:1) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger numbers of bends and/or fittings shall be increased by an equivalent length of tubing to the ollowing equation: $L = 1.3n$, where L is additional length (ft) of tubing and n is the number of additional fittings and/or bends.2) All table entries are rounded to 3 significant digits.Table 6.2.1(r) Corrugated Stainless Steel Tubing (CSST)Inlet Pressure: Drop:1.0 psiSpecificSpecific	90	37	51	94	109	185	221	383	444	735	848	1,460	1,700	3,00	00 3,390
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	100	35	48	89	104	176	210	363	421	698	806	1,380	1,610	2,85	50 3,210
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	150	28	39	73	85	145	172	294	342	573	664	1,130	1,320	2,34	40 2,630
300 19 27 52 60 104 122 206 240 409 477 793 936 1,660 1,860 EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency between different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing. Notes: 1) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger numbers of bends and/or fittings shall be increased by an equivalent length of tubing to the ollowing equation: <i>L</i> = 1.3 <i>n</i> , where <i>L</i> is additional length (ft) of tubing and <i>n</i> is the number of additional fittings and/or bends. 2) All table entries are rounded to 3 significant digits. Table 6.2.1(r) Corrugated Stainless Steel Tubing (CSST) Gas: Natural Inlet Pressure: 2.0 psi Pressure: 2.0 psi Pressure: 2.0 psi Image: Image: Image: Image: Image:	200	24	34	63	73	126	149	254	295	498	579	974	1,140	2,03	30 2,280
EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency between different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing. Notes: 1) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger numbers of bends and/or fittings shall be increased by an equivalent length of tubing to the following equation: $L = 1.3n$, where L is additional length (ft) of tubing and n is the number of additional fittings and/or bends. 2) All table entries are rounded to 3 significant digits. Table 6.2.1(r) Corrugated Stainless Steel Tubing (CSST) Image: the state of the s	250	21	30	57	66	114	134	226	263	447	520	870	1,020	1,82	20 2,040
different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing. Notes: 1) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger numbers of bends and/or fittings shall be increased by an equivalent length of tubing to the following equation: L = 1.3n, where L is additional length (ft) of tubing and n is the number of additional fittings and/or bends. 2) All table entries are rounded to 3 significant digits. Table 6.2.1(r) Corrugated Stainless Steel Tubing (CSST)	300	19	27	52	60	104	122	206	240	409	477	793	936	1,66	30 1,860
Table 6.2.1(r) Corrugated Stainless Steel Tubing (CSST) Gas: Natural Inlet Pressure: 2.0 psi Pressure Drop: 1.0 psi Specific	different tubing Notes: 1) Table include numbers of ben ollowing equati	sizes es lo ds a on: <i>L</i>	s. Th sses nd/c _ = 1	ne gr s for or fitti .3 <i>n</i> ,	four ngs whe	r the 90 c shal	legre	ue of E ee ber increa	EHD, th ids and sed by	ne grea d two e v an eq	ater th end fitt juivale	tings. T ent leng	capacit Fubing i gth of tu	y of t runs ubing	the tubing. with larger
Gas: Natural Gas: Natural Inlet Pressure: 2.0 psi Pressure Drop: 1.0 psi Specific	(2) All table enti	ries a	are r	ound	ded t	io 3 s	signi	ficant	digits.						
Inlet Pressure: Drop: 1.0 psi	Table 6.2.1(r) C	Corru	gate	ed St	ainle	ess S	Steel	Tubin	g (CSS	ST)					
Pressure: 2.0 psi Pressure: 2.0 psi Pressure: Drop: Specific	_	-	-	-	-	-			-		-	-	G	as:	Natural
<u>Drop:</u> <u>1.0 psi</u>	_	_	_	_	_	_	-		_		-	_ !			<u>2.0 psi</u>
<u>Specific</u>															1.0 psi
	-	-	-	-	-	-	-	-	-		-	-	<u>Spec</u>	ific	

<u>Tube Size (EHD)</u>

<u>Flow</u> <u>Designation:</u>	<u>13</u>	<u>15</u>	<u>18</u>	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	<u>46</u>	<u>48</u>	<u>60</u>	<u>62</u>
Length (ft)					Ca	pacity	<u>/ in Cι</u>	ubic Fe	et of	<u>Gas p</u>	er Ho	ur		
10	270	353	587	700	1,100	1,370	2,590	2,990	4,510	5,037	9,600	10,700	18,600	21,600
25	166	220	374	444	709	876	1,620	1,870	2,890	3,258	6,040	6,780	11,900	13,700
30	151	200	342	405	650	801	1,480	1,700	2,640	2,987	5,510	6,200	10,900	12,500
40	129	172	297	351	567	696	1,270	1,470	2,300	2,605	4,760	5,380	9,440	10,900
50	115	154	266	314	510	624	1,140	1,310	2,060	2,343	4,260	4,820	8,470	9,720
75	93	124	218	257	420	512	922	1,070	1,690	1,932	3,470	3,950	6,940	7,940
80	89	120	211	249	407	496	892	1,030	1,640	1,874	3,360	3,820	6,730	7,690
100	79	107	189	222	366	445	795	920	1,470	1,685	3,000	3,420	6,030	6,880
150	64	87	155	182	302	364	646	748	1,210	1,389	2,440	2,800	4,940	5,620
200	55	75	135	157	263	317	557	645	1,050	1,212	2,110	2,430	4,290	4,870
250	49	67	121	141	236	284	497	576	941	1,090	1,890	2,180	3,850	4,360
300	44	61	110	129	217	260	453	525	862	999	1,720	1,990	3,520	3,980
400	38	52	96	111	189	225	390	453	749	871	1,490	1,730	3,060	3,450
500	34	46	86	100	170	202	348	404	552	783	1,330	1,550	2,740	3,090

EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency between different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing.

Notes:

(1) Table does not include effect of pressure drop across the line regulator. Where regulator loss exceeds $\frac{3}{4}$ psi, do not use this table. Consult with regulator manufacturer for pressure drops and capacity factors. Pressure drops across a regulator may vary with flow rate.

(2) CAUTION: Capacities shown in table may exceed maximum capacity for a selected regulator. Consult with regulator or tubing manufacturer for guidance.

(3) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger number of bends and/or fittings shall be increased by an equivalent length of tubing according to the following equation: L = 1.3n, where L is additional length (ft) of tubing and n is the number of additional fittings and/or bends.

(4) All table entries are rounded to 3 significant digits.

Table 6.2.1(s) Corrugated Stainless Steel Tubing (CSST)

							<u> </u>	,						
-	-	-	-	-	_	-	-	-	-	_		<u>Gas:</u>	Natura	<u>al</u>
												Inlet		
-	-	-	-	-	-	-	-	-	-	-	<u>Pre</u>	<u>ssure:</u>	<u>5.0 ps</u>	<u>i</u>
											Pre	<u>essure</u>		
-	-	-	-	-	-	-	-	-	-	-		Drop:	<u>3.5 ps</u>	<u>i</u>
												pecific		
	-	-	-	-	-	-	-	-	-	-	<u>G</u>	<u>ravity:</u>	<u>0.60</u>	
							<u>Tub</u>	<u>e Size</u>	<u>(EHD</u>)				
Flow														
Designation:	<u>13</u>	<u>15</u>	<u>18</u>	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	<u>46</u>	<u>48</u>	<u>60</u>	<u>6</u>
<u>Length (ft)</u>					<u>Cap</u>	acity	in Cul	oic Fe	et of G	<u>as pe</u>	<u>r Hour</u>			
10	523	674	1,080	1,300	2,000	2,530	4,920	5,660	8,300	9,140	18,100	19,800	34,400	40,
25	322	420	691	827	1,290	1,620	3,080	3,540	5,310	5,911	11,400	12,600	22,000	25,
30	292	382	632	755	1,180	1,480	2,800	3,230	4,860	5,420	10,400	11,500	20,100	23,

-	-	-	-	-	-	-	-	-	-	-		<u>Gas:</u>	Natura	al
											Dre	Inlet		
-	-	-	-	-	-	-	-		-	-	Pre	essure:	<u>5.0 ps</u>	<u>!</u>
_	_	_	_	_	_	_	_	_	_	_	<u>Pr</u>	<u>essure</u> Drop:	<u>3.5 ps</u>	i
												pecific Gravity:		
	-	-					- Tub	- e Size	- (EHD)		/_		
 Flow							<u></u>		<u>\</u>					
Designation:	<u>13</u>	<u>15</u>	<u>18</u>	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	<u>46</u>	<u>48</u>	<u>60</u>	6
<u>Length (ft)</u>					Cap	oacity	in Cul	oic Fe	et of G	<u>as pe</u>	<u>r Hour</u>			
40	251	329	549	654	1,030	1,280	2,420	2,790	4,230	4,727	8,970	10,000	17,400	20,
50	223	293	492	586	926	1,150	2,160	2,490	3,790	4,251	8,020	8,930	15,600	18,
75	180	238	403	479	763	944	1,750	2,020	3,110	3,506	6,530	7,320	12,800	14,
80	174	230	391	463	740	915	1,690	1,960	3,020	3,400	6,320	7,090	12,400	14,
100	154	205	350	415	665	820	1,510	1,740	2,710	3,057	5,650	6,350	11,100	12,
150	124	166	287	339	548	672	1,230	1,420	2,220	2,521	4,600	5,200	9,130	10,
200	107	143	249	294	478	584	1,060	1,220	1,930	2,199	3,980	4,510	7,930	9,0
250	95	128	223	263	430	524	945	1,090	1,730	1,977	3,550	4,040	7,110	8,1
300	86	116	204	240	394	479	860	995	1,590	1,813	3,240	3,690	6,500	7,4
400	74	100	177	208	343	416	742	858	1,380	1,581	2,800	3,210	5,650	6,4
500	66	89	159	186	309	373	662	766	1,040	1,422	2,500	2,870	5,060	5,7

EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency between different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing.

Notes:

(1) Table does not include effect of pressure drop across line regulator. Where regulator loss exceeds 1 psi, do not use this table. Consult with regulator manufacturer for pressure drops and capacity factors. Pressure drop across regulator may vary with the flow rate.

(2) CAUTION: Capacities shown in table may exceed maximum capacity of selected regulator. Consult with tubing manufacturer for guidance.

(3) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger numbers of bends and/or fittings shall be increased by an equivalent length of tubing to the following equation: L = 1.3n, where L is additional length (ft) of tubing and n is the number of additional fittings and/or bends.

(4) All table entries are rounded to 3 significant digits.

Table 6.2.1(t) Polyethylene Plastic Pipe

-	-	_			Gas:	Natural				
-	-	-		Inlet P	ressure:	Less tha	<u>n 2 psi</u>			
_	-	-		Pressu	ire Drop:	<u>0.3 in. w</u>	<u>. w.c.</u>			
_	-	-		<u>Specific</u>	Gravity:	<u>0.60</u>				
-			<u>Pipe Si</u>	<u>ze (in.)</u>			-	-		
Nominal OD:	1 <u>/2</u>	³ /4	<u>1</u>	<u>1¼</u>	<u>1</u> ½	<u>2</u>	<u>3</u>	<u>4</u>		
Designation:	<u>SDR 9.3</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 10</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>		
Actual ID:	<u>0.660</u>	<u>0.860</u>	<u>1.077</u>	<u>1.328</u>	<u>1.554</u>	<u>1.943</u>	<u>2.864</u>	<u>3.682</u>		

Length (ft)		<u>c</u>	<u>apacity ir</u>	n Cubic F	eet of Ga	<u>s per Hou</u>	<u>ır</u>	
10	153	305	551	955	1,440	2,590	7,170	13,900
20	105	210	379	656	991	1,780	4,920	9,520
30	84	169	304	527	796	1,430	3,950	7,640
40	72	144	260	451	681	1,220	3,380	6,540
50	64	128	231	400	604	1,080	3,000	5,800
60	58	116	209	362	547	983	2,720	5,250
70	53	107	192	333	503	904	2,500	4,830
80	50	99	179	310	468	841	2,330	4,500
90	46	93	168	291	439	789	2,180	4,220
100	44	88	159	275	415	745	2,060	3,990
125	39	78	141	243	368	661	1,830	3,530
150	35	71	127	221	333	598	1,660	3,200
175	32	65	117	203	306	551	1,520	2,940
200	30	60	109	189	285	512	1,420	2,740
250	27	54	97	167	253	454	1,260	2,430
300	24	48	88	152	229	411	1,140	2,200
350	22	45	81	139	211	378	1,050	2,020
400	21	42	75	130	196	352	974	1,880
450	19	39	70	122	184	330	914	1,770
500	18	37	66	115	174	312	863	1,670

Table 6.2.1(u) Polyethylene Plastic Pipe

_	-	_			<u>Gas:</u>	<u>Natural</u>			
_	-	_	Inlet Pressure: Less than 2 psi Pressure Drop: 0.5 in. w.c. Specific Gravity: 0.60 Pipe Size (in.) 0.60 1 $1^{1/4}$ $1^{1/2}$ 2 3 4 11 SDR 11 SDR 10 SDR 11 S						
-	-	-	$\begin{tabular}{ c c c c c c c } \hline V & V &$						
_	-	_		<u>Specific</u>	Gravity:	<u>0.60</u>			
-				<u>Pipe Si</u>	<u>ze (in.)</u>				
Nominal OD:	1 <u>/</u> 2	³ /4	1	<u>1</u> ¼	<u>1</u> ½	<u>2</u>	<u>3</u>	<u>4</u>	
Designation:	SDR 9.3	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 10</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>	
Actual ID:	<u>0.660</u>	<u>0.860</u>	<u>1.077</u>	<u>1.328</u>	<u>1.554</u>	<u>1.943</u>	<u>2.864</u>	<u>3.682</u>	
<u>Length (ft)</u>		<u>C</u>	apacity ir	n Cubic F	eet of Gas	<u>s per Hou</u>	<u>r</u>		
10	201	403	726	1,260	1,900	3,410	9,450	18,260	
20	138	277	499	865	1,310	2,350	6,490	12,550	
30	111	222	401	695	1,050	1,880	5,210	10,080	
40	95	190	343	594	898	1,610	4,460	8,630	
50	84	169	304	527	796	1,430	3,950	7,640	
60	76	153	276	477	721	1,300	3,580	6,930	
70	70	140	254	439	663	1,190	3,300	6,370	
80	65	131	236	409	617	1,110	3,070	5,930	
90	61	123	221	383	579	1,040	2,880	5,560	
100	58	116	209	362	547	983	2,720	5,250	

-	-	-	Specific Gravity: 0.60 Pipe Size (in.)41 $1\frac{1}{4}$ $1\frac{1}{2}$ 234R 11SDR 11SDR 10SDR 11SDR 11SDR 11SDR 11SDR 113601.0771.3281.5541.9432.8643.6GalaxiesCapacity in Cubic Feet of Gas per Hour031853214858712,4104,6631682914397892,1804,2261542684047262,0103,8601442493766751,8703,6111272213335981,6603,20						
-	-	-	Inlet Pressure:Less than 2 psiPressure Drop: 0.5 in. w.c.Specific Gravity: 0.60 Pipe Size (in.)111½23411SDR 11SDR 10SDR 11SDR 11SDR 11SDR 1301.0771.3281.5541.9432.8643.682Capacity in Cubic Feet of Gas per Hour31853214858712.4104.6601682914397892.1804.2201542684047262.0103.8801442493766751.8703.6101272213335981.6603.2001152003025421.5002.9001061842784991.3802.670						
-	-	-							
-	-	-				0.00			
-	1.	37				•	•		
Nominal OD:	1 <u>/</u> 2	³ /4	<u>1</u>	<u>1'/</u> 4	<u>1'/</u> 2	2	<u>3</u>	<u>4</u>	
Designation:	<u>SDR 9.3</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 10</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>	
Actual ID:	<u>0.660</u>	<u>0.860</u>	<u>1.077</u>	<u>1.328</u>	<u>1.554</u>	<u>1.943</u>	<u>2.864</u>	<u>3.682</u>	
Length (ft)		<u>C</u>	<u>apacity ir</u>	Cubic Fe	eet of Gas	<u>s per Hou</u>	r		
125	51	103	185	321	485	871	2,410	4,660	
150	46	93	168	291	439	789	2,180	4,220	
175	43	86	154	268	404	726	2,010	3,880	
200	40	80	144	249	376	675	1,870	3,610	
250	35	71	127	221	333	598	1,660	3,200	
300	32	64	115	200	302	542	1,500	2,900	
350	29	59	106	184	278	499	1,380	2,670	
400	27	55	99	171	258	464	1,280	2,480	
450	26	51	93	160	242	435	1,200	2,330	
	24	48	88	152	229	411	1,140	2,200	

Table 6.2.1(v) Polyethylene Plastic Pipe

					Gas:	Natural				
-										
-	-	-		Inlet P	ressure:	<u>2.0 psi</u>				
-	-	-		Pressu	re Drop:	<u>1.0 psi</u>				
-	-	-		<u>Specific</u>	Gravity:	<u>0.60</u>				
-		<u>Pipe Size (in.)</u>								
Nominal OD:	1 <u>/2</u>	³ /4	<u>1</u>	<u>1</u> 1/4	<u>1</u> ½	<u>2</u>	<u>3</u>	<u>3</u>		
Designation:	<u>SDR 9.3</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 10</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>		
Actual ID:	<u>0.660</u>	<u>0.860</u>	<u>1.077</u>	<u>1.328</u>	<u>1.554</u>	<u>1.943</u>	<u>2.864</u>	<u>3.682</u>		
<u>Length (ft)</u>		<u>C</u>	<u>apacity ir</u>	n Cubic Fo	eet of Ga	<u>s per Hou</u>	<u>r</u>			
10	1,860	3,720	6,710	11,600	17,600	31,600	87,300	169,000		
20	1,280	2,560	4,610	7,990	12,100	21,700	60,000	116,000		
30	1,030	2,050	3,710	6,420	9,690	17,400	48,200	93,200		
40	878	1,760	3,170	5,490	8,300	14,900	41,200	79,700		
50	778	1,560	2,810	4,870	7,350	13,200	36,600	70,700		
60	705	1,410	2,550	4,410	6,660	12,000	33,100	64,000		
70	649	1,300	2,340	4,060	6,130	11,000	30,500	58,900		
80	603	1,210	2,180	3,780	5,700	10,200	28,300	54,800		
90	566	1,130	2,050	3,540	5,350	9,610	26,600	51,400		
100	535	1,070	1,930	3,350	5,050	9,080	25,100	48,600		
125	474	949	1,710	2,970	4,480	8,050	22,300	43,000		

-	-	-			<u>Gas:</u>	<u>Natural</u>			
-	-	-		Inlet P	ressure:	<u>2.0 psi</u>			
_	_	_		Pressu	re Drop:	<u>1.0 psi</u>			
				Specific	Gravity:	0.60			
			1	Pipe Si					
Nominal OD:	1 <u>/2</u>	3/4	<u>1</u>	<u>1</u> ¹ /4	<u>1</u> ¹ /2	<u>2</u>	<u>3</u>	<u>3</u>	
Designation:	SDR 9.3	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 10</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>		
Actual ID:	0.660	0.860	<u>1.077</u>	<u>1.328</u>	1.554	1.943	2.864	<u>3.682</u>	
Length (ft)		<u>C</u>	apacity ir	n Cubic Fo	et of Gas	<u>s per Hou</u>	r		
150	429	860	1,550	2,690	4,060	7,290	20,200	39,000	
175	395	791	1,430	2,470	3,730	6,710	18,600	35,900	
200	368	736	1,330	2,300	3,470	6,240	17,300	33,400	
250	326	652	1,180	2,040	3,080	5,530	15,300	29,600	
300	295	591	1,070	1,850	2,790	5,010	13,900	26,800	
350	272	544	981	1,700	2,570	4,610	12,800	24,700	
400	253	506	913	1,580	2,390	4,290	11,900	22,900	
450	237	475	856	1,480	2,240	4,020	11,100	21,500	
500	224	448	809	1,400	2,120	3,800	10,500	20,300	
550	213	426	768	1,330	2,010	3,610	9,990	19,300	
600	203	406	733	1,270	1,920	3,440	9,530	18,400	
650	194	389	702	1,220	1,840	3,300	9,130	17,600	
700	187	374	674	1,170	1,760	3,170	8,770	16,900	
750	180	360	649	1,130	1,700	3,050	8,450	16,300	
800	174	348	627	1,090	1,640	2,950	8,160	15,800	
850	168	336	607	1,050	1,590	2,850	7,890	15,300	
900	163	326	588	1,020	1,540	2,770	7,650	14,800	
950	158	317	572	990	1,500	2,690	7,430	14,400	
1,000	154	308	556	963	1,450	2,610	7,230	14,000	
1,100	146	293	528	915	1,380	2,480	6,870	13,300	
1,200	139	279	504	873	1,320	2,370	6,550	12,700	
1,300	134	267	482	836	1,260	2,270	6,270	12,100	
1,400	128	257	463	803	1,210	2,180	6,030	11,600	
1,500	124	247	446	773	1,170	2,100	5,810	11,200	
1,600	119	239	431	747	1,130	2,030	5,610	10,800	
1,700	115	231	417	723	1,090	1,960	5,430	10,500	
1,800	112	224	404	701	1,060	1,900	5,260	10,200	
1,900	109	218	393	680	1,030	1,850	5,110	9,900	
2,000	106	212	382	662	1,000	1,800	4,970	9,600	

Table 6.2.1(w) Polyethylene Plastic Tubing

-	<u>Gas:</u>	<u>Natural</u>
-	Inlet Pressure:	Less than 2.0 psi

_	Pressure Drop:	0.3 in. w.c.
	Specific Gravity:	0.60
-	Plastic Tubing	<u>Size (CTS) (in.)</u>
Nominal OD:	1 <u>/</u> 2	1
Designation:	<u>SDR 7</u>	<u>SDR 11</u>
Actual ID:	0.445	0.927
Length (ft)		eet of Gas per Hour
10	54	372
20	37	256
30	30	205
40	26	176
50	23	156
60	21	141
70	19	130
80	18	121
90	17	113
100	16	107
125	14	95
150	13	86
175	12	79
200	11	74
225	10	69
250	NA	65
275	NA	62
300	NA	59
350	NA	54
400	NA	51
450	NA	47
500	NA	45
CTS: Copper tube size.		
NA: A flow of less than 1	0 cfh.	
Note: All table entries are	e rounded to 3 significant digits.	
Table 6.2.1(x) Polyethyle	• •	
	<u>Gas:</u>	Natural
-		Less than 2.0 psi
-	Pressure Drop:	
-	<u>Specific Gravity:</u>	
-		<u>Size (CTS) (in.)</u>
- Nominal OD:		
		<u><u>1</u> <u>SDR 11</u></u>
Designation:	<u>SDR 7</u>	
Actual ID:	<u>0.445</u>	<u>0.927</u>

Length (ft)	Capacity in Cubic F	Feet of Gas per Hour
10	72	490
20	49	337
30	39	271
40	34	232
50	30	205
60	27	186
70	25	171
80	23	159
90	22	149
100	21	141
125	18	125
150	17	113
175	15	104
200	14	97
225	13	91
250	12	86
275	11	82
300	11	78
350	10	72
400	NA	67
450	NA	63
500	NA	59

CTS: Copper tube size.

NA: A flow of less than 10 cfh.

Note: All table entries are rounded to 3 significant digits.

6.2.2

Section 6.4 shall be used in conjunction with one of the methods described in 6.1.2 through 6.1.4 for non-corrugated stainless steel tubing.

6.3 Sizing Propane Piping Systems.

Sizing of piping systems shall be in accordance with 6.3.1 or 6.3.2.

6.3.1

Table 6.3.1(a) through Table 6.3.1(m) shall be used in conjunction with one of the methods described in 6.1.2 through 6.1.4 for piping materials other than non-corrugated stainless steel tubing.

Table 6.3.1(a) Schedule 40 Metallic Pipe

-	-	-	-	-	-		<u>Gas:</u>	Undiluted Propane	1			
_	_	_	_	_	_	Inlet I	Pressure:	<u>10.0 psi</u>				
						Press	ure Drop:	<u>1.0 psi</u>	1.0 psi			
-	-	-	-	-	-		c Gravity:	1.50				
		- E: Pipe S	- Sizing B	etween	- First-Sta) <u>Regulato</u>	or and			
		Se	cond-St	<u>age (Lov</u>	w-Press	ure) Reg	ulator.					
-		<u>Pipe Size (in.)</u>										
<u>Nominal</u>												
Inside:	1 <u>/</u> 2	3/4	<u>1</u>	<u>1¼</u>	<u>11/</u> 2	<u>2</u>	<u>2</u> ¹ / ₂	<u>3</u>	<u>4</u>			
Actual:	<u>0.622</u>	<u>0.824</u>	<u>1.049</u>	<u>1.380</u>	<u>1.610</u>	<u>2.067</u>	<u>2.469</u>	<u>3.068</u>	<u>4.026</u>			
<u>.ength (ft)</u>			<u>Cap</u>	acity in	Thousa	nds of B	tu per Hou	ir				
10	3,320	6,950	13,100	26,900	40,300	77,600	124,000	219,000	446,000			
20	2,280	4,780	9,000	18,500	27,700	53,300	85,000	150,000	306,000			
30	1,830	3,840	7,220	14,800	22,200	42,800	68,200	121,000	246,000			
40	1,570	3,280	6,180	12,700	19,000	36,600	58,400	103,000	211,000			
50	1,390	2,910	5,480	11,300	16,900	32,500	51,700	91,500	187,000			
60	1,260	2,640	4,970	10,200	15,300	29,400	46,900	82,900	169,000			
70	1,160	2,430	4,570	9,380	14,100	27,100	43,100	76,300	156,000			
80	1,080	2,260	4,250	8,730	13,100	25,200	40,100	70,900	145,000			
90	1,010	2,120	3,990	8,190	12,300	23,600	37,700	66,600	136,000			
100	956	2,000	3,770	7,730	11,600	22,300	35,600	62,900	128,000			
125	848	1,770	3,340	6,850	10,300	19,800	31,500	55,700	114,000			
150	768	1,610	3,020	6,210	9,300	17,900	28,600	50,500	103,000			
175	706	1,480	2,780	5,710	8,560	16,500	26,300	46,500	94,700			
200	657	1,370	2,590	5,320	7,960	15,300	24,400	43,200	88,100			
250	582	1,220	2,290	4,710	7,060	13,600	21,700	38,300	78,100			
300	528	1,100	2,080	4,270	6,400	12,300	19,600	34,700	70,800			
350	486	1,020	1,910	3,930	5,880	11,300	18,100	31,900	65,100			
400	452	945	1,780	3,650	5,470	10,500	16,800	29,700	60,600			
450	424	886	1,670	3,430	5,140	9,890	15,800	27,900	56,800			
500	400	837	1,580	3,240	4,850	9,340	14,900	26,300	53,700			
550	380	795	1,500	3,070	4,610	8,870	14,100	25,000	51,000			
600	363	759	1,430	2,930	4,400	8,460	13,500	23,900	48,600			
650	347	726	1,370	2,810	4,210	8,110	12,900	22,800	46,600			
700	334	698	1,310	2,700	4,040	7,790	12,400	21,900	44,800			
750	321	672	1,270	2,600	3,900	7,500	12,000	21,100	43,100			
800	310	649	1,220	2,510	3,760	7,240	11,500	20,400	41,600			
850	300	628	1,180	2,430	3,640	7,010	11,200	19,800	40,300			
900	291	609	1,150	2,360	3,530	6,800	10,800	19,200	39,100			

	950	283	592	1,110	2,290	3,430	6,600	10,500	18,600	37,900
_	1,000	275	575	1,080	2,230	3,330	6,420	10,200	18,100	36,900
	1,100	261	546	1,030	2,110	3,170	6,100	9,720	17,200	35,000
	1,200	249	521	982	2,020	3,020	5,820	9,270	16,400	33,400
	1,300	239	499	940	1,930	2,890	5,570	8,880	15,700	32,000
	1,400	229	480	903	1,850	2,780	5,350	8,530	15,100	30,800
_	1,500	221	462	870	1,790	2,680	5,160	8,220	14,500	29,600
	1,600	213	446	840	1,730	2,590	4,980	7,940	14,000	28,600
	1,700	206	432	813	1,670	2,500	4,820	7,680	13,600	27,700
	1,800	200	419	789	1,620	2,430	4,670	7,450	13,200	26,900
	1,900	194	407	766	1,570	2,360	4,540	7,230	12,800	26,100
	2,000	189	395	745	1,530	2,290	4,410	7,030	12,400	25,400

Table 6.3.1(b) Schedule 40 Metallic Pipe

_		,			·			
	-	_	-	-	-	-	<u>Gas:</u>	ndiluted ropane
	-	_	_	_	_	_	Inlet Pressure: 1	<u>0.0 psi</u>
	-	_	_	_	_	_	Pressure Drop: 3	. <u>0 psi</u>
	_	_	_	_	_	_	Specific Gravity: 1	.50

INTENDED USE: Pipe Sizing Between First-Stage (High-Pressure) Regulator and Second-Stage (Low-Pressure) Regulator.

-		<u>Pipe Size (in.)</u>									
<u>Nominal</u> Inside:	1 <u>/</u> 2	³ /4	<u>1</u>	<u>11/4</u>	<u>11/2</u>	2	<u>2</u> ¹ / ₂	<u>3</u>	4		
Actual:	<u>0.622</u>	<u>0.824</u>	<u>1.049</u>	<u>1.380</u>	<u>1.610</u>	<u>2.067</u>	<u>2.469</u>	<u>3.068</u>	<u>4.026</u>		
Length (ft)			Cap	acity in	Thousa	nds of Bt	u per Hou	ir	<u>.</u>		
10	5,890	12,300	23,200	47,600	71,300	137,000	219,000	387,000	789,000		
20	4,050	8,460	15,900	32,700	49,000	94,400	150,000	266,000	543,000		
30	3,250	6,790	12,800	26,300	39,400	75,800	121,000	214,000	436,000		
40	2,780	5,810	11,000	22,500	33,700	64,900	103,000	183,000	373,000		
50	2,460	5,150	9,710	19,900	29,900	57,500	91,600	162,000	330,000		
60	2,230	4,670	8,790	18,100	27,100	52,100	83,000	147,000	299,000		
70	2,050	4,300	8,090	16,600	24,900	47,900	76,400	135,000	275,000		
80	1,910	4,000	7,530	15,500	23,200	44,600	71,100	126,000	256,000		
90	1,790	3,750	7,060	14,500	21,700	41,800	66,700	118,000	240,000		
100	1,690	3,540	6,670	13,700	20,500	39,500	63,000	111,000	227,000		
125	1,500	3,140	5,910	12,100	18,200	35,000	55,800	98,700	201,000		
150	1,360	2,840	5,360	11,000	16,500	31,700	50,600	89,400	182,000		
175	1,250	2,620	4,930	10,100	15,200	29,200	46,500	82,300	167,800		
200	1,160	2,430	4,580	9,410	14,100	27,200	43,300	76,500	156,100		
250	1,030	2,160	4,060	8,340	12,500	24,100	38,400	67,800	138,400		
300	935	1,950	3,680	7,560	11,300	21,800	34,800	61,500	125,400		
350	860	1,800	3,390	6,950	10,400	20,100	32,000	56,500	115,300		

-	_	_	_	_	_		<u>Gas</u>	Undilute Propane	
						Inlet F	Pressure	: <u>10.0 psi</u>	
-	-	-	-	-	-		ure Drop		
-	-	-	-	-	-		Gravity		
-	-	-	-	-	-		G		
INTENDE	DUSE					<u>ge (High-</u> ire) Regul		e) Regulato	or and
-			1	1	Pipe S	ize (in.)	1		1
<u>Nominal</u> Inside:	¹ /2	³ /4	<u>1</u>	<u>11/4</u>	<u>1½</u>	2	<u>2</u> ¹ / ₂	<u>3</u>	<u>4</u>
Actual:	<u>0.622</u>	<u>0.824</u>	<u>1.049</u>	<u>1.380</u>	<u>1.610</u>	<u>2.067</u>	<u>2.469</u>	<u>3.068</u>	<u>4.026</u>
Length (ft)			<u>Cap</u>	acity in	Thousa	nds of Bt	<u>u per Ho</u>	<u>ur</u>	
400	800	1,670	3,150	6,470	9,690	18,700	29,800	52,600	107,300
450	751	1,570	2,960	6,070	9,090	17,500	27,900	49,400	100,700
500	709	1,480	2,790	5,730	8,590	16,500	26,400	46,600	95,100
550	673	1,410	2,650	5,450	8,160	15,700	25,000	44,300	90,300
600	642	1,340	2,530	5,200	7,780	15,000	23,900	42,200	86,200
650	615	1,290	2,420	4,980	7,450	14,400	22,900	40,500	82,500
700	591	1,240	2,330	4,780	7,160	13,800	22,000	38,900	79,300
750	569	1,190	2,240	4,600	6,900	13,300	21,200	37,400	76,400
800	550	1,150	2,170	4,450	6,660	12,800	20,500	36,200	73,700
850	532	1,110	2,100	4,300	6,450	12,400	19,800	35,000	71,400
900	516	1,080	2,030	4,170	6,250	12,000	19,200	33,900	69,200
950	501	1,050	1,970	4,050	6,070	11,700	18,600	32,900	67,200
1,000	487	1,020	1,920	3,940	5,900	11,400	18,100	32,000	65,400
1,100	463	968	1,820	3,740	5,610	10,800	17,200	30,400	62,100
1,200	442	923	1,740	3,570	5,350	10,300	16,400	29,000	59,200
1,300	423	884	1,670	3,420	5,120	9,870	15,700	27,800	56,700
1,400	406	849	1,600	3,280	4,920	9,480	15,100	26,700	54,500
1,500	391	818	1,540	3,160	4,740	9,130	14,600	25,700	52,500
1,600	378	790	1,490	3,060	4,580	8,820	14,100	24,800	50,700
1,700	366	765	1,440	2,960	4,430	8,530	13,600	24,000	49,000
1,800	355	741	1,400	2,870	4,300	8,270	13,200	23,300	47,600
1,900	344	720	1,360	2,780	4,170	8,040	12,800	22,600	46,200
2,000	335	700	1,320	2,710	4,060	7,820	12,500	22,000	44,900
ote: All table able 6.3.1(c)				•	ant digit	S.			
-	_	-	-	-	-		<u>Gas:</u>	Undiluted	Propane
-	-	-	-	-	-	Inlet Pre	essure:	<u>2.0 psi</u>	
-	_	_	_	-	_	Pressure	Drop:	<u>1.0 psi</u>	
	_					<u>Specific G</u>	iravity:	<u>1.50</u>	
INTENDE	USE:	Pipe Siz	zing Bet	ween 2	psig Se	rvice and	Line Pre	essure Reg	ulator.
					Pipe Si	70 (in)			

Nominal:	¹ /2	³ /4	1	<u>1¼</u>	<u><u>1</u>¹/2</u>	<u>2</u>	<u>2</u> ¹ / ₂	<u>3</u>	<u>4</u>
Actual ID:	<u>0.622</u>	<u>0.824</u>	<u>1.049</u>	<u>1.380</u>	<u>1.610</u>	<u>2.067</u>	<u>2.469</u>	<u>3.068</u>	<u>4.026</u>
<u>ength (ft)</u>			<u>Ca</u>	<u>pacity i</u>	n Thous	sands of I	<u> Stu per Ho</u>	<u>our</u>	
10	2,680	5,590	10,500	21,600	32,400	62,400	99,500	176,000	359,000
20	1,840	3,850	7,240	14,900	22,300	42,900	68,400	121,000	247,000
30	1,480	3,090	5,820	11,900	17,900	34,500	54,900	97,100	198,000
40	1,260	2,640	4,980	10,200	15,300	29,500	47,000	83,100	170,000
50	1,120	2,340	4,410	9,060	13,600	26,100	41,700	73,700	150,000
60	1,010	2,120	4,000	8,210	12,300	23,700	37,700	66,700	136,000
70	934	1,950	3,680	7,550	11,300	21,800	34,700	61,400	125,000
80	869	1,820	3,420	7,020	10,500	20,300	32,300	57,100	116,000
90	815	1,700	3,210	6,590	9,880	19,000	30,300	53,600	109,000
100	770	1,610	3,030	6,230	9,330	18,000	28,600	50,600	103,000
125	682	1,430	2,690	5,520	8,270	15,900	25,400	44,900	91,500
150	618	1,290	2,440	5,000	7,490	14,400	23,000	40,700	82,900
175	569	1,190	2,240	4,600	6,890	13,300	21,200	37,400	76,300
200	529	1,110	2,080	4,280	6,410	12,300	19,700	34,800	71,000
250	469	981	1,850	3,790	5,680	10,900	17,400	30,800	62,900
300	425	889	1,670	3,440	5,150	9,920	15,800	27,900	57,000
350	391	817	1,540	3,160	4,740	9,120	14,500	25,700	52,400
400	364	760	1,430	2,940	4,410	8,490	13,500	23,900	48,800
450	341	714	1,340	2,760	4,130	7,960	12,700	22,400	45,800
500	322	674	1,270	2,610	3,910	7,520	12,000	21,200	43,200
550	306	640	1,210	2,480	3,710	7,140	11,400	20,100	41,100
600	292	611	1,150	2,360	3,540	6,820	10,900	19,200	39,200
650	280	585	1,100	2,260	3,390	6,530	10,400	18,400	37,500
700	269	562	1,060	2,170	3,260	6,270	9,990	17,700	36,000
750	259	541	1,020	2,090	3,140	6,040	9,630	17,000	34,700
800	250	523	985	2,020	3,030	5,830	9,300	16,400	33,500
850	242	506	953	1,960	2,930	5,640	9,000	15,900	32,400
900	235	490	924	1,900	2,840	5,470	8,720	15,400	31,500
950	228	476	897	1,840	2,760	5,310	8,470	15,000	30,500
1,000	222	463	873	1,790	2,680	5,170	8,240	14,600	29,700
1,100	210	440	829	1,700	2,550	4,910	7,830	13,800	28,200
1,200	201	420	791	1,620	2,430	4,680	7,470	13,200	26,900
1,300	192	402	757	1,550	2,330	4,490	7,150	12,600	25,800
1,400	185	386	727	1,490	2,240	4,310	6,870	12,100	24,800
1,500	178	372	701	1,440	2,160	4,150	6,620	11,700	23,900
1,600	172	359	677	1,390	2,080	4,010	6,390	11,300	23,000
1,700	166	348	655	1,340	2,010	3,880	6,180	10,900	22,300
1,800	161	337	635	1,300	1,950	3,760	6,000	10,600	21,600
1,900	157	327	617	1,270	1,900	3,650	5,820	10,300	21,000
2,000	152	318	600	1,230	1,840	3,550	5,660	10,000	20,400

Note: All table entries are rounded to 3 significant digits.

_	_	_	_	_	_		<u>Gas:</u>	<u>Undiluted</u> Propane	<u>k</u>
_	_	_	_	_	_	Inlet F	Pressure:	<u>11.0 in. w</u>	.c.
-	-	-	-	-	-	Pressi	ure Drop:	0.5 in. w.	 C.
-	-	-	-	-	-		Gravity:	1.50	
-	-	-	-	-	-				
INTENL	<u>150 031</u>	E: Pipe a	<u>Sizing E</u> Rec	gulator a	and App	liance.	<u>10-5tage (</u>	Low-Pres	<u>sure</u>)
						ize (in.)			
Nominal									
Inside:	1/2	3/4	<u>1</u>	<u>11/4</u>	<u>11/2</u>	<u>2</u>	<u>2</u> ¹ / ₂	<u>3</u>	4
Actual:	0.622	0.824	 1.049	1.380	1.610	 2.067	2.469	3.068	<u> </u>
.ength (ft)	0.011	0.021					tu per Hou		
10	291	608	1,150	2,350	3,520	6,790	10,800	<u>19,100</u>	39,000
20	200	418	787	1,620	2,420	4,660	7,430	13,100	26,800
30	160	336	632	1,300	1,940	3,750	5,970	10,600	20,000
30 40	137	287	541	1,110	1,660	3,210	5,110	9,030	18,400
50	122	255	480	985	1,480	2,840	4,530	8,000	16,300
60	110	231	434	892	1,340	2,570	4,100	7,250	14,800
70	101	212	400	821	1,230	2,370	3,770	6,670	13,600
80	94	197	372	763	1,140	2,200	3,510	6,210	12,700
90	89	185	349	716	1,070	2,070	3,290	5,820	11,900
100	84	175	330	677	1,010	1,950	3,110	5,500	11,200
125	74	155	292	600	899	1,730	2,760	4,880	9,950
150	67	140	265	543	814	1,570	2,500	4,420	9,010
175	62	129	243	500	749	1,440	2,300	4,060	8,290
200	58	120	227	465	697	1,340	2,140	3,780	7,710
250	51	107	201	412	618	1,190	1,900	3,350	6,840
300	46	97	182	373	560	1,080	1,720	3,040	6,190
350	42	89	167	344	515	991	1,580	2,790	5,700
400	40	83	156	320	479	922	1,470	2,600	5,300
450	37	78	146	300	449	865	1,380	2,440	4,970
500	35	73	138	283	424	817	1,300	2,300	4,700
550	33	70	131	269	403	776	1,240	2,190	4,460
600	32	66	125	257	385	741	1,180	2,090	4,260
650	30	64	120	246	368	709	1,130	2,000	4,080
700	29	61	115	236	354	681	1,090	1,920	3,920
750	28	59	111	227	341	656	1,050	1,850	3,770
800	27	57	107	220	329	634	1,010	1,790	3,640
850	26	55	104	213	319	613	978	1,730	3,530
900	25	53	100	206	309	595	948	1,680	3,420
950	25	52	97	200	300	578	921	1,630	3,320
1,000 1,100	24 23	50 48	95 90	195	292	562	895	1,580	3,230

			1	1	1					
1,200	22	46	86	176	264	50	9 8	311	1,430	2,930
1,300	21	44	82	169	253	48	87 7	77	1,370	2,800
1,400	20	42	79	162	243	3 46	8 7	' 46	1,320	2,690
1,500	19	40	76	156	234	45	51 7	' 19	1,270	2,590
1,600	19	39	74	151	226	6 43	6 6	694	1,230	2,500
1,700	18	38	71	146	219	42	2 6	672	1,190	2,420
1,800	18	37	69	142	212	2 40	9 6	52	1,150	2,350
1,900	17	36	67	138	206	39	07 6	33	1120	2280
2,000	17	35	65	134	200) 38	6 6	615	1090	2220
ote: All tab able 6.3.1					nificant o	ligits.	1		1	
-	_		_	-	-	_		<u>Gas:</u>	<u>Undilut</u> Propan	
_	_	_	_	_	_	_	Inlet P	ressure:	<u>10.0 ps</u>	
-	-	-	_	-	-	-	E	Pressure Drop:	<u>1.0 psi</u>	
-	_	-	_	_	-	_		<u>Specific</u> Gravity:	<u>1.50</u>	
INTEND	DED USI						<u>High-Pro</u> Regulate		<u>Regulato</u>	r and
		56	econa-a							
_	_	<u>56</u>	cona-a			ube Siz				
-	- K &	<u>56</u>	econa-a							
- Nominal:	- <u>K &</u> L:	<u>5</u>	3 <u>⁄8</u>	1 <u>/2</u>				<u>1</u> ¹ /4	<u>1</u> ¹ / ₂	2
- Nominal:					1	ube Siz	<u>:e (in.)</u>	<u>11/4</u> <u>13/8</u>	<u>1½</u>	2
	<u>L:</u>	1/4	3/8	1/2	<u>]</u>	ube Siz	<u>e (in.)</u>		<u>1½</u> <u> </u>	<u>2</u> = <u>2.125</u>
<u>0</u>	<u>L:</u> <u>ACR:</u>	1/4 3/8	³ /8 1/2	1 <u>/2</u>	<u>5⁄8</u> <u>3⁄4</u>	<u>ube Siz</u> 3 <u>/4</u> 7 <u>/</u> 8	<u>e (in.)</u> <u>1</u> <u>1</u> ¹ / ₈	<u><u>1</u>³/₈</u>	=	=
<u>0</u> 1	<u>ACR:</u> utside: nside:*	1/4 3/8 0.375	³ <u>⁄</u> 8 ¹ <u>⁄</u> 2 <u>0.500</u>	1½ 5½ 0.625 0.527	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u>	3/4 7/8 0.875 0.745	<u>1</u> <u>1</u> <u>11%</u> <u>1.125</u> <u>0.995</u>	<u>1³/₈</u> <u>1.375</u> <u>1.245</u>	<u> </u>	<u> </u>
<u>O</u> Length	<u>ACR:</u> utside: nside:*	1/4 3/8 0.375 0.305	³ / ₈ 1/2 0.500 0.402	¹ / ₂ ⁵ / ₆ <u>0.625</u> <u>0.527</u> <u>Capac</u>	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u>	<u>ube Siz</u> <u>3/4</u> <u>7/8</u> <u>0.875</u> <u>0.745</u> housan	<u>e (in.)</u> <u>1</u> <u>1½</u> <u>1.125</u> <u>0.995</u> ds of Bt	<u>1³⁄₈</u> <u>1.375</u> <u>1.245</u> u per Ho	<u> </u>	 2.125 1.959
<u>O</u> <u>I</u> <u>Length</u> 10	<u>ACR:</u> utside: nside:*	1 <u>/4</u> 3 <u>/8</u> 0.375 0.305 513	3 <u>⁄</u> 8 1 <u>⁄</u> 2 0.500 0.402 1,060	1½ 5½ 0.625 0.527 Capac 2,150	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760	3/4 7/8 0.875 0.745 housan 5,330	<u>1</u> <u>1</u> <u>1½</u> <u>1.125</u> <u>0.995</u> <u>ds of Bt</u> 11,400	<u>1</u> ³ / _∞ <u>1.375</u> <u>1.245</u> <u>u per Ho</u> 20,500		<u>2.125</u> <u>1.959</u> 67,400
0 <u>Length</u> 10 20	<u>ACR:</u> utside: nside:*	1/4 3/8 0.375 0.305	³ / ₆ 1/2 0.500 0.402 1,060 727	1/2 5/8 0.625 0.527 <u>Capac</u> 2,150 1,480	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760 2,580	3/4 7/8 0.875 0.745 housan 5,330 3,670	<u>1</u> <u>1½8</u> <u>1.125</u> <u>0.995</u> <u>ds of Bt</u> 11,400 7,830	<u>1</u> ³ <u>∕</u> <u>8</u> <u>1.375</u> <u>1.245</u> <u>u per Ho</u> 20,500 14,100	= <u>1.625</u> <u>1.481</u> <u>ur</u> 32,300 22,200	<u>2.125</u> <u>1.959</u> 67,400 46,300
<u>O</u> <u>I</u> <u>Length</u> 10	<u>ACR:</u> utside: nside:*	1 <u>/4</u> 3 <u>/8</u> 0.375 0.305 0.305 513 352	3 <u>⁄</u> 8 1 <u>⁄</u> 2 0.500 0.402 1,060	1½ 5½ 0.625 0.527 Capac 2,150	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760	3/4 7/8 0.875 0.745 housan 5,330 3,670 2,940	<u>1</u> <u>1</u> <u>1½</u> <u>1.125</u> <u>0.995</u> <u>ds of Bt</u> 11,400	<u>1</u> ³ / _∞ <u>1.375</u> <u>1.245</u> <u>u per Ho</u> 20,500		2.125 2.125 1.959 67,400 46,300 37,200
<u>O</u> <u>Length</u> 10 20 30	<u>ACR:</u> utside: nside:*	1 <u>/4</u> 3 <u>/8</u> 0.375 0.305 0.305 513 352 283	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584	1½ 5½ 0.625 0.527 Capac 2,150 1,480 1,190	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760 2,580 2,080	3/4 7/8 0.875 0.745 housan 5,330 3,670	<u>1</u> <u>11/8</u> <u>1.125</u> <u>0.995</u> <u>ds of Bt</u> 11,400 7,830 6,290	<u>1</u> 3 ³ ⁄ _∞ <u>1.375</u> <u>1.245</u> <u>u per Ho</u> 20,500 14,100 11,300	I.625 1.481 ur 32,300 22,200 17,900	
0 <u>Length</u> 10 20 30 40	<u>ACR:</u> utside: nside:*	1 <u>/4</u> 3 <u>/8</u> 0.375 0.305 513 352 283 242	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500	1½ 5% 0.625 0.527 Capac 2,150 1,480 1,190 1,020	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760 2,580 2,080 1,780	3⁄4 7⁄≴ 0.875 0.745 housan 5,330 3,670 2,940 2,520	<u>1</u> <u>1½</u> <u>11½</u> <u>0.995</u> <u>0.995</u> <u>0.995</u> <u>0.995</u> <u>0.995</u> <u>0.995</u> 0.5,380	<u>1</u> ³ <u>∕</u> <u>8</u> <u>1.375</u> <u>1.245</u> <u>20,500</u> 14,100 11,300 9,690	Image: line with the second system 1.625 1.481 ur 32,300 22,200 17,900 15,300	2.125 2.125 1.959 67,400 46,300 37,200 31,800 28,200
0 <u>Length</u> 10 20 30 40 50	<u>ACR:</u> utside: nside:*	1 <u>/</u> 4 3 <u>/</u> 8 0.375 0.305 0.305 0.305 0.305 2.13 352 2.83 2.42 2.15	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500 443	1½ 5% 0.625 0.527 2,150 1,480 1,190 1,020 901	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760 2,580 2,080 1,780 1,570	Jube Siz 3/4 7/8 0.875 0.745 housan 5,330 3,670 2,940 2,520 2,230	1 1½ 1½ 1.125 0.995 ds of Bt 11,400 7,830 6,290 5,380 4,770	<u>1</u> ³ <u>∕</u> ⁶ <u>1.375</u> <u>1.245</u> <u>u per Ho</u> 20,500 14,100 11,300 9,690 8,590	I.625 1.481 ur 32,300 22,200 17,900 15,300 13,500	2.125 1.959 67,400 46,300 37,200 31,800 28,200 25,600
0 <u>Length</u> 10 20 30 40 50 60	<u>ACR:</u> utside: nside:*	1 <u>/4</u> 3 <u>/8</u> 0.375 0.305 0.305 513 352 283 242 215 242 215 194	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500 443 401	1½ 5% 0.625 0.527 Capac 2,150 1,480 1,190 1,020 901 816	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760 2,580 2,080 1,780 1,570 1,430	3⁄4 7⁄≴ 0.875 0.745 housan 5,330 3,670 2,940 2,520 2,230 2,020	<u>1</u> <u>1½</u> <u>1.125</u> <u>0.995</u> <u>ds of Bt</u> 11,400 7,830 6,290 5,380 4,770 4,320	<u>13%</u> <u>1.375</u> <u>1.245</u> <u>20,500</u> 14,100 11,300 9,690 8,590 7,780	Image: marked line 1.625 1.481 ur 32,300 22,200 17,900 15,300 13,500 12,300	2.125 2.125 1.959 67,400 46,300 37,200 31,800 28,200 25,600 23,500
0 <u>Length</u> 10 20 30 40 50 60 70	<u>ACR:</u> utside: nside:*	1 <u>/</u> 4 3 <u>/</u> 8 0.375 0.305 0.305 0.305 0.305 2.13 352 2.83 2.42 2.15 2.15 1.94 1.79	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500 443 401 369	1½ 5⁄8 0.625 0.527 2,150 1,480 1,190 1,020 901 816 751	1 5½ 3¼ 0.750 0.652 ity in T 3,760 2,580 2,080 1,780 1,570 1,430 1,310	3/4 7/8 0.875 0.745 housan 5,330 3,670 2,940 2,520 2,230 2,020 1,860	1 1½ 1½ 1.125 0.995 ds of Bt 11,400 7,830 6,290 5,380 4,770 4,320 3,980	<u>13%</u> <u>1.375</u> <u>1.245</u> <u>u per Ho</u> 20,500 14,100 11,300 9,690 8,590 7,780 7,160	I.625 1.481 ur 32,300 22,200 17,900 15,300 13,500 12,300 11,300	2.125 1.959 67,400 46,300 37,200 31,800 28,200 23,500 21,900
0 <u>Length</u> 10 20 30 40 50 60 70 80	<u>ACR:</u> utside: nside:*	1 <u>/4</u> 3 <u>/6</u> 0.375 0.305	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500 443 401 369 343	1½ 5% 0.625 0.527 Capac 2,150 1,480 1,190 1,020 901 816 751 699	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760 2,580 2,080 1,780 1,570 1,430 1,310 1,220	3⁄4 7⁄8 0.875 0.745 housan 5,330 3,670 2,940 2,520 2,020 1,860 1,730	<u>1</u> <u>1½</u> <u>11½</u> <u>1.125</u> <u>0.995</u> <u>ds of Bt</u> 11,400 7,830 6,290 5,380 4,770 4,320 3,980 3,700	<u>13%</u> <u>1.375</u> <u>1.245</u> <u>20,500</u> 14,100 11,300 9,690 8,590 7,780 7,160 6,660	I.625 1.481 ur 32,300 22,200 17,900 15,300 13,500 12,300 10,500	2.125 1.959 67,400 46,300 37,200 31,800 28,200 23,500 21,900 20,500
0 10 20 30 40 50 60 70 80 90	<u>ACR:</u> utside: nside:*	1 <u>/</u> 4 3 <u>/</u> 8 0.375 0.305	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500 443 401 369 343 322	1½ 5⁄8 0.625 0.527 2,150 1,480 1,190 1,020 901 816 751 699 655	<u>5%</u> <u>3⁄4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760 2,580 2,080 1,780 1,570 1,430 1,310 1,220 1,150	3/4 7/8 0.875 0.745 0.745 5,330 3,670 2,940 2,520 2,230 2,020 1,860 1,730 1,630	1 1½ 1½ 1.125 0.995 ds of Bt 11,400 7,830 6,290 5,380 4,770 4,320 3,980 3,700 3,470	<u>13%</u> <u>1.375</u> <u>1.245</u> <u>1.245</u> <u>1.245</u> 20,500 14,100 11,300 9,690 8,590 7,780 7,160 6,660 6,250	I.625 1.481 ur 32,300 22,200 17,900 15,300 13,500 12,300 11,300 10,500 9,850	2.125 1.959 67,400 46,300 37,200 31,800 28,200 25,600 21,900 20,500 19,400
0 10 20 30 40 50 60 70 80 90 100	<u>ACR:</u> utside: nside:*	1/4 3/8 0.375 0.30	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500 443 401 369 343 322 304	1½ 5% 0.625 0.527 Capac 2,150 1,480 1,190 1,020 901 816 751 699 655 619	<u>5</u> <u>%</u> <u>3</u> <u>⁄</u> 4 <u>0.750</u> <u>0.652</u> <u>ity in T</u> 3,760 2,580 2,080 1,780 1,570 1,430 1,220 1,150 1,080	3⁄4 7⁄8 0.875 0.745 housan 5,330 3,670 2,940 2,520 2,020 1,860 1,730 1,630 1,540	<u>1</u> <u>1½</u> <u>11½</u> <u>1.125</u> <u>0.995</u> <u>ds of Bt</u> 11,400 7,830 6,290 5,380 4,770 4,320 3,980 3,700 3,470 3,280	<u>13%</u> <u>1.375</u> <u>1.245</u> <u>1.245</u> <u>20,500</u> 14,100 14,100 11,300 9,690 8,590 7,780 7,780 7,780 6,660 6,250 5,900	I.625 1.481 32,300 22,200 17,900 15,300 13,500 12,300 10,500 9,850 9,310	2.125 2.125 1.959 67,400 46,300 37,200 31,800 28,200 23,500 23,500 21,900 20,500 19,400 17,200
0 10 20 30 40 50 60 70 80 90 100 125	<u>ACR:</u> utside: nside:*	1/4 3/8 0.375 0.30	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500 443 500 443 401 369 343 322 304 270	1½ 5% 0.625 0.527 Capac 2,150 1,480 1,190 1,020 901 816 751 699 655 619 549	5% 3⁄4 0.750 0.652 ity in T 3,760 2,580 2,080 1,780 1,570 1,430 1,220 1,150 1,080 959	3/4 3/4 7/8 0.875 0.745 housan 5,330 3,670 2,940 2,520 2,230 2,020 1,860 1,730 1,630 1,360	1 1¹⅓ 1.125 0.995 ds of Bt 11,400 7,830 6,290 5,380 4,770 4,320 3,980 3,700 3,470 3,280 2,910	<u>1</u> 3% <u>1.375</u> <u>1.245</u> <u>1.245</u> <u>1.245</u> <u>1.245</u> <u>1.245</u> <u>1.375</u> <u>1.245</u> <u>1.250</u> <u>7,780</u> <u>7,780</u> <u>7,780</u> <u>7,780</u> <u>7,780</u> <u>5,900</u> <u>5,230</u>	I.625 1.481 ur 32,300 22,200 17,900 15,300 13,500 12,300 11,300 10,500 9,850 9,310 8,250	2.125 1.959 67,400 46,300 37,200 31,800 28,200 23,500 21,900 20,500 19,400 15,600
0 10 20 30 40 50 60 70 80 90 100 125 150	<u>ACR:</u> utside: nside:*	1⁄4 3⁄8 0.375 0.30	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500 443 401 369 343 322 304 270 244	1½ 5% 0.625 0.527 Capac 2,150 1,480 1,190 1,020 901 816 751 699 655 619 549 497	<u>5</u> <u>3</u> <u>4</u> <u>0.750</u> <u>0.652</u> <u>ity in T</u> <u>3,760</u> 2,580 2,080 1,780 1,570 1,430 1,570 1,430 1,220 1,150 1,080 959 869	3⁄4 7⁄8 0.875 0.740 1,860 1,230	1 1½ 1½ 1.125 0.995 ds of Bt 11,400 7,830 6,290 5,380 4,770 4,320 3,980 3,700 3,280 2,910 2,630	<u>13%</u> <u>1.375</u> <u>1.245</u> <u>20,500</u> 14,100 11,300 9,690 8,590 7,780 7,780 7,760 6,660 6,250 5,900 5,230 4,740	I.625 1.481 32,300 22,200 17,900 15,300 13,500 12,300 10,500 9,850 9,310 8,250 7,470	2.125 2.125 1.959 67,400 46,300 37,200 31,800 28,200 23,500 23,500 21,900 20,500 19,400 17,200 15,600 14,300
Length 10 20 30 40 50 60 70 80 90 100 125 150 175	<u>ACR:</u> utside: nside:*	1/4 3/8 0.375 0.30	3 <u>%</u> 1 <u>/</u> 2 0.500 0.402 1,060 727 584 500 443 500 443 401 369 343 322 304 270 244 225	1½ 5% 0.625 0.527 Capac 2,150 1,480 1,190 1,020 901 816 751 699 655 619 549 497 457	1 5½ 3⁄4 0.750 0.652 ity in T 3,760 2,580 2,080 1,780 1,570 1,430 1,220 1,150 1,080 959 869 799	3/4 3/4 7/8 0.875 0.745 bousan 5,330 3,670 2,940 2,520 2,230 2,020 1,860 1,730 1,630 1,230 1,130	1 1¹⅓ 1.125 0.995 ds of Bt 11,400 7,830 6,290 5,380 4,770 4,320 3,980 3,700 3,470 3,280 2,910 2,630 2,420	<u>1</u> 3% <u>1.375</u> <u>1.245</u> <u>1.250</u> <u>5,900</u> <u>5,230</u> <u>4,740</u> <u>4,360</u>	I.625 1.481 ur 32,300 22,200 17,900 15,300 13,500 12,300 11,300 10,500 9,850 9,310 8,250 7,470 6,880	 <u>2.125</u>

350	75	155	314	549	779	1,660	3,000	4,730	9,840
400	70	144	292	511	725	1,550	2,790	4,400	9,160
450	65	135	274	480	680	1,450	2,620	4,130	8,590
500	62	127	259	453	643	1,370	2,470	3,900	8,120
550	59	121	246	430	610	1,300	2,350	3,700	7,710
600	56	115	235	410	582	1,240	2,240	3,530	7,350
650	54	111	225	393	558	1,190	2,140	3,380	7,040
700	51	106	216	378	536	1,140	2,060	3,250	6,770
750	50	102	208	364	516	1,100	1,980	3,130	6,520
800	48	99	201	351	498	1,060	1,920	3,020	6,290
850	46	96	195	340	482	1,030	1,850	2,920	6,090
900	45	93	189	330	468	1,000	1,800	2,840	5,910
950	44	90	183	320	454	970	1,750	2,750	5,730
1,000	42	88	178	311	442	944	1,700	2,680	5,580
1,100	40	83	169	296	420	896	1,610	2,540	5,300
1,200	38	79	161	282	400	855	1,540	2,430	5,050
1,300	37	76	155	270	383	819	1,470	2,320	4,840
1,400	35	73	148	260	368	787	1,420	2,230	4,650
1,500	34	70	143	250	355	758	1,360	2,150	4,480
1,600	33	68	138	241	343	732	1,320	2,080	4,330
1,700	32	66	134	234	331	708	1,270	2,010	4,190
1,800	31	64	130	227	321	687	1,240	1,950	4,060
1,900	30	62	126	220	312	667	1,200	1,890	3,940
2,000	29	60	122	214	304	648	1,170	1,840	3,830

Note: All table entries are rounded to 3 significant digits.

*Table capacities are based on Type K copper tubing inside diameter (shown), which has the smallest inside diameter of the copper tubing products.

Table 6.3.1(f) Semirigid Copper Tubing

-	_	_	_	_	_	-		<u>Gas:</u>	Undilute Propane	
-	_	_	_	_	_	_	Inlet Pr	<u>essure:</u>	<u>11.0 in.</u>	<u>w.c.</u>
_	_	_	_	_	_	_	<u>P</u>	<u>ressure</u> <u>Drop:</u>	<u>0.5 in. w</u>	<u>.c.</u>
-	-	-	_	-	-	-		<u>Specific</u> Gravity:	<u>1.50</u>	
INTEN	DED US	<u>SE: Tub</u>				gle- or S Appliance		<u>Stage (Lo</u>	ow-Press	<u>ure</u>)
-	_]	Tube Siz	<u>ze (in.)</u>			
Nemineli	<u>K & L:</u>	1 <u>/</u> 4	³ ⁄8	1 <u>/</u> 2	⁵ ⁄8	³ /4	<u>1</u>	<u>1¼</u>	<u>11/</u> 2	<u>2</u>
Nominal:	ACR:	³ ⁄8	1 <u>/2</u>	⁵ /8	3/4	7 <u>⁄8</u>	<u>11/8</u>	<u>1³⁄8</u>	=	=
<u>0</u>	utside:	<u>0.375</u>	<u>0.500</u>	<u>0.625</u>	<u>0.750</u>	<u>0.875</u>	<u>1.125</u>	<u>1.375</u>	<u>1.625</u>	<u>2.125</u>
Ī	nside:*	<u>0.305</u>	<u>0.402</u>	<u>0.527</u>	<u>0.652</u>	<u>0.745</u>	<u>0.995</u>	<u>1.245</u>	<u>1.481</u>	<u>1.959</u>
<u>Length</u>	<u>(ft)</u>			Capac	<u>ity in T</u>	housan	ds of Bt	<u>u per Ho</u>	ur	<u>.</u>

10	45	93	188	329	467	997	1,800	2,830	5,890
20	31	64	129	226	321	685	1,230	1,950	4,050
30	25	51	104	182	258	550	991	1,560	3,250
40	21	44	89	155	220	471	848	1,340	2,780
50	19	39	79	138	195	417	752	1,180	2,470
60	17	35	71	125	177	378	681	1,070	2,240
70	16	32	66	115	163	348	626	988	2,060
80	15	30	61	107	152	324	583	919	1,910
90	14	28	57	100	142	304	547	862	1,800
100	13	27	54	95	134	287	517	814	1,700
125	11	24	48	84	119	254	458	722	1,500
150	10	21	44	76	108	230	415	654	1,360
175	NA	20	40	70	99	212	382	602	1,250
200	NA	18	37	65	92	197	355	560	1,170
250	NA	16	33	58	82	175	315	496	1,030
300	NA	15	30	52	74	158	285	449	936
350	NA	14	28	48	68	146	262	414	861
400	NA	13	26	45	63	136	244	385	801
450	NA	12	24	42	60	127	229	361	752
500	NA	11	23	40	56	120	216	341	710
550	NA	11	22	38	53	114	205	324	674
600	NA	10	21	36	51	109	196	309	643
650	NA	NA	20	34	49	104	188	296	616
700	NA	NA	19	33	47	100	180	284	592
750	NA	NA	18	32	45	96	174	274	570
800	NA	NA	18	31	44	93	168	264	551
850	NA	NA	17	30	42	90	162	256	533
900	NA	NA	17	29	41	87	157	248	517
950	NA	NA	16	28	40	85	153	241	502
1,000	NA	NA	16	27	39	83	149	234	488
1,100	NA	NA	15	26	37	78	141	223	464
1,200	NA	NA	14	25	35	75	135	212	442
1,300	NA	NA	14	24	34	72	129	203	423
1,400	NA	NA	13	23	32	69	124	195	407
1,500	NA	NA	13	22	31	66	119	188	392
1,600	NA	NA	12	21	30	64	115	182	378
1,700	NA	NA	12	20	29	62	112	176	366
1,800	NA	NA	11	20	28	60	108	170	355
1,900	NA	NA	11	19	27	58	105	166	345
2,000	NA	NA	11	19	27	57	102	161	335

NA: A flow of less than 10,000 Btu/hr.

Note: All table entries are rounded to 3 significant digits.

*Table capacities are based on Type K copper tubing inside diameter (shown), which has the smallest inside diameter of the copper tubing products.

-	_	_	_	_	_	-		<u>Gas:</u>	<u>Undiluted</u> Propane	<u>k</u>
							Inlet P	ressure:	<u>2.0 psi</u>	
-	-	-	-	-	-	-		re Drop:	1.0 psi	
-	-	-	-	-	-	-		<u>Specific</u> Gravity:	1.50	
		- E: Tuba	- Sizina	- N Dotw	- 	-	nuico ono		ssure Reg	wlatar
			<u>- 312111</u>	<u>J Delw</u>	<u>een z p</u>				<u>ssule Re</u> t	<u>juiator.</u>
-	-					<u>adu I</u>	<u>Size (in.</u>)		
Nominal:	<u>K &</u> <u>L:</u>	1 <u>/4</u>	³ ⁄8	1 <u>/</u> 2	⁵ /8	3⁄4	<u>1</u>	<u>1¼</u>	<u>1</u> ½	2
	ACR:	³ ⁄8	1 <u>/</u> 2	5 <u>⁄</u> 8	³ /4	7 <u>∕</u> 8	<u>11/8</u>	<u>1³⁄8</u>	=	=
<u>O</u>	utside:	<u>0.375</u>	<u>0.500</u>	<u>0.625</u>	<u>0.750</u>	<u>0.875</u>	<u>1.125</u>	<u>1.375</u>	<u>1.625</u>	<u>2.125</u>
<u>h</u>	nside:*	<u>0.305</u>	<u>0.402</u>	0.527	0.652	<u>0.745</u>	<u>0.995</u>	<u>1.245</u>	<u>1.481</u>	<u>1.959</u>
Length	(ft)			Сар	acity ir	า Thous	sands of	Btu per H	lour	1
10		413	852	1,730	3,030	4,300	9,170	16,500	26,000	54,200
20		284	585		2,080		6,310	11,400	17,900	37,300
30		228	470	956	1,670	2,370	5,060	9,120	14,400	29,900
40		195	402	818	1,430	2,030	4,330	7,800	12,300	25,600
50		173	356	725	1,270	1,800	3,840	6,920	10,900	22,700
60		157	323	657	1,150	1,630	3,480	6,270	9,880	20,600
70		144	297	605	1,060	1,500	3,200	5,760	9,090	18,900
80		134	276	562	983	1,390	2,980	5,360	8,450	17,600
90		126	259	528	922	1,310	2,790	5,030	7,930	16,500
100		119	245	498	871	1,240	2,640	4,750	7,490	15,600
125		105	217	442	772	1,100	2,340	4,210	6,640	13,800
150		95	197	400	700	992	2,120	3,820	6,020	12,500
175		88	181	368	644	913	1,950	3,510	5,540	11,500
200		82	168	343	599	849	1,810	3,270	5,150	10,700
250		72	149	304	531	753	1,610	2,900	4,560	9,510
300		66	135	275	481	682	1,460	2,620	4,140	8,610
350		60	124	253	442	628	1,340	2,410	3,800	7,920
400		56	116	235	411	584	1,250	2,250	3,540	7,370
450		53	109	221	386	548	1,170	2,110	3,320	6,920
500		50	103	209	365	517	1,110	1,990	3,140	6,530
550		47	97	198	346	491	1,050	1,890	2,980	6,210
600 650		45	93	189	330	469	1,000	1,800	2,840	5,920
650 700		43	89 86	181	316	449	959 021	1,730	2,720	5,670
700		41	86 82	174	304	431	921	1,660	2,620	5,450
750		40	82	168	293	415	888	1,600	2,520	5,250
800 850		39 37	80 77	162 157	283 274	401 388	857 829	1,540	2,430	5,070 4,900
850 900		37 36	77 75	157	274	388	829 804	1,490 1,450	2,350 2,280	4,900

95	0	35	72	147	258	366	781	1,410	2,220	4,620
1,0	00	34	71	143	251	356	760	1,370	2,160	4,490
1,1	00	32	67	136	238	338	721	1,300	2,050	4,270
1,2	00	31	64	130	227	322	688	1,240	1,950	4,070
1,3	00	30	61	124	217	309	659	1,190	1,870	3,900
1,4	00	28	59	120	209	296	633	1,140	1,800	3,740
1,5	00	27	57	115	201	286	610	1,100	1,730	3,610
1,6	00	26	55	111	194	276	589	1,060	1,670	3,480
1,7	00	26	53	108	188	267	570	1,030	1,620	3,370
1,8	00	25	51	104	182	259	553	1,000	1,570	3,270
1,9	00	24	50	101	177	251	537	966	1,520	3,170
2,0	00	23	48	99	172	244	522	940	1,480	3,090

Note: All table entries are rounded to 3 significant digits.

*Table capacities are based on Type K copper tubing inside diameter (shown), which has the smallest inside diameter of the copper tubing products.

Table 6.3.1(h) Corrugated Stainless Steel Tubing (CSST)

_	_	_	_	_	_	_	_	_	_	_		<u>Gas:</u>	<u>Undilu</u> Propa	
-	_	_	_	_	_	_	_	_	_	_	Pre	<u>Inlet</u> ssure:	<u>11.0 in</u>	. W.C.
-	_	_	_	_	_	_	_	_	_	_	Pre	essure Drop:	<u>0.5 in.</u>	<u>W.C.</u>
-	_	_	_	_	_	_	_	_	_	_		<u>pecific</u> ravity:	<u>1.50</u>	
INTENDED	USE	E: C										<u>e (Low-</u>	Pressu	<u>re)</u>
			<u>Re</u>	<u>gula</u>	tor a	nd A	<u>Appli</u>	ance	e Shut	off Val	ve.			
-								Tube	<u>Size</u>	(<u>EHD</u>)				
<u>Flow</u> <u>Designation:</u>	<u>13</u>	<u>15</u>	<u>18</u>	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	<u>46</u>	<u>48</u>	<u>60</u>	<u>62</u>
Length (ft)					<u>Cap</u>	bacit	<u>y in</u>	Tho	usand	s of Bt	u per l	<u>lour</u>		
5	72	99	181	211	355	426	744	863	1,420	1,638	2,830	3,270	5,780	6,550
10	50	69	129	150	254	303	521	605	971	1,179	1,990	2,320	4,110	4,640
15	39	55	104	121	208	248	422	490	775	972	1,620	1,900	3,370	3,790
20	34	49	91	106	183	216	365	425	661	847	1,400	1,650	2,930	3,290
25	30	42	82	94	164	192	325	379	583	762	1,250	1,480	2,630	2,940
30	28	39	74	87	151	177	297	344	528	698	1,140	1,350	2,400	2,680
40	23	33	64	74	131	153	256	297	449	610	988	1,170	2,090	2,330
50	20	30	58	66	118	137	227	265	397	548	884	1,050	1,870	2,080
60	19	26	53	60	107	126	207	241	359	502	805	961	1,710	1,900
70	17	25	49	57	99	117	191	222	330	466	745	890	1,590	1,760
80	15	23	45	52	94	109	178	208	307	438	696	833	1,490	1,650
90	15	22	44	50	90	102	169	197	286	414	656	787	1,400	1,550
100	14	20	41	47	85	98	159	186	270	393	621	746	1,330	1,480
150	11	15	31	36	66	75	123	143	217	324	506	611	1,090	1,210

200	9	14	4 28	3 33	60 6	59 112	2 129	183	283	438	531	948	1,050	
250	8	12	2 25	5 30	53 6	61 99	117	163	254	390	476	850	934	
300	8	11	1 23	3 26	50 5	57 90	107	147	234	357	434	777	854	
EHD: Equivale different tubing Notes: (1) Table includ numbers of be following equa additional fittin (2) All table en	des lo nds a tion: gs ar	es. T osse and/o L = nd/o	he g es for or fitt 1.3 <i>n</i> , r ber	four stings s , wher nds.	90 deg hall be	lue of ree be incre additio	EHD, ends ar ased b nal ler	the gro nd two by an e ngth (fl	eater t end fi equival	he gas ttings. lent ler	capaci Tubing ngth of t	ty of the runs wi ubing to	tubing th large the	
					-		-							
Table 6.3.1(i)	Com	Jgale	ea S	lainies	ss Stee		ng (Ce	51)						
-	-	-	_	-	-	-	-	-	-	-		<u>Gas:</u>	<u>Undilu</u> Propa	
-	-	-	-	-	-	-	-	-	-	-		Inlet ssure: essure	<u>2.0 ps</u> i	<u>i</u>
-	-	-	-	-	-	-	-	-	-	-		Drop: pecific	<u>1.0 ps</u>	<u>i</u>
-	-	-	-	-	-	-	-	-	-	-	<u>G</u>	<u>ravity:</u>	<u>1.50</u>	
INTEND	ED L	JSE:	CSS	ST Siz	zing B	etwee	<u>n 2 ps</u>	<u>ig Ser</u>	vice a	nd Lin	e Pres	sure Re	<u>egulato</u>	r.
-							<u>Tul</u>	oe Siz	<u>e (EHI</u>	<u>)</u>				
Flow			40	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	46	<u>48</u>	<u>60</u>	<u>6</u>
	<u>13</u>	<u>15</u>	<u>18</u>						1					
	<u>13</u>	<u>15</u>	18		<u>Ca</u>	pacity	in Th		nds of	Btu po	er Hou	 :		
Designation:								ousar			er Hou	16,800		34,
<u>Designation:</u> <u>Length (ft)</u>	426	558		1,110	1,740	2,170	4,100	ousar 4,720	7,130	7,958	er Houi 15,200	-	29,400	
Designation: Length (ft) 10	426 262	558 347	927	1,110 701	1,740 1,120	2,170 1,380	4,100 2,560	ousar 4,720 2,950	7,130 4,560	7,958 5,147	er Houi 15,200	16,800 10,700	29,400	21,
Designation: Length (ft) 10 25	426 262 238	558 347 316	927 591	1,110 701 640	1,740 1,120 1,030	2,170 1,380 1,270	4,100 2,560 2,330	ousar 4,720 2,950 2,690	7,130 4,560 4,180	7,958 5,147	er Hou 15,200 9,550 8,710	16,800 10,700 9,790	 29,400 18,800	21, 19,
Designation: Length (ft) 10 25 30	426 262 238 203	558 347 316 271	927 591 540	1,110 701 640 554	1,740 1,120 1,030	2,170 1,380 1,270 1,100	4,100 2,560 2,330 2,010	ousar 4,720 2,950 2,690 2,320	7,130 4,560 4,180 3,630	7,958 5,147 4,719 4,116	er Hou 15,200 9,550 8,710	16,800 10,700 9,790 8,500	29,400 18,800 17,200	21, 19, 17,
Designation: Length (ft) 10 25 30 40	426 262 238 203 181	558 347 316 271 243	927 591 540 469	1,110 701 640 554 496	1,740 1,120 1,030 896	2,170 1,380 1,270 1,100	4,100 2,560 2,330 2,010 1,790	ousar 4,720 2,950 2,690 2,320 2,070	7,130 4,560 4,180 3,630 3,260	7,958 5,147 4,719 4,116 3,702	er Hour 15,200 9,550 8,710 7,530	16,800 10,700 9,790 8,500 7,610	29,400 18,800 17,200 14,900	21, 19, 17, 15,
Designation: Length (ft) 10 25 30 40 50	426 262 238 203 181 147	558 347 316 271 243 196	927 591 540 469 420	1,110 701 640 554 496 406	1,740 1,120 1,030 896 806	2,170 1,380 1,270 1,100 986	4,100 2,560 2,330 2,010 1,790 1,460	ousar 4,720 2,950 2,690 2,320 2,070 1,690	7,130 4,560 4,180 3,630 3,260 2,680	7,958 5,147 4,719 4,116 3,702 3,053	er Houi 15,200 9,550 8,710 7,530 6,730	16,800 10,700 9,790 8,500 7,610 6,230	29,400 18,800 17,200 14,900 13,400	21, 19, 17, 15, 12,
Designation: Length (ft) 10 25 30 40 50 75	426 262 238 203 181 147 140	558 347 316 271 243 196 189	927 591 540 469 420 344	1,110 701 640 554 496 406 393	1,740 1,120 1,030 896 806 663	2,170 1,380 1,270 1,100 986 809	4,100 2,560 2,330 2,010 1,790 1,460 1,410	ousar 4,720 2,950 2,690 2,320 2,070 1,690 1,630	7,130 4,560 4,180 3,630 3,260 2,680 2,590	7,958 5,147 4,719 4,116 3,702 3,053	er Hour 15,200 9,550 8,710 7,530 6,730 5,480 5,300	16,800 10,700 9,790 8,500 7,610 6,230	29,400 18,800 17,200 14,900 13,400 11,000 10,600	21, 19, 17, 15, 12, 12,
Designation: Length (ft) 10 25 30 40 50 75 80	426 262 238 203 181 147 140 124	558 347 316 271 243 196 189 169	927 591 540 469 420 344 333	1,110 701 640 554 496 406 393 350	1,740 1,120 1,030 896 806 663 643	2,170 1,380 1,270 1,100 986 809 768	4,100 2,560 2,330 2,010 1,790 1,460 1,410 1,260	ousar 4,720 2,950 2,690 2,320 2,070 1,690 1,630 1,450	7,130 4,560 4,180 3,630 3,260 2,680 2,590 2,330	7,958 5,147 4,719 4,116 3,702 3,053 2,961 2,662	er Hour 15,200 9,550 8,710 7,530 6,730 5,480 5,300	16,800 10,700 9,790 8,500 7,610 6,230 6,040	29,400 18,800 17,200 14,900 13,400 11,000 10,600	21, 19, 17, 15, 12, 12,
Designation: Length (ft) 10 25 30 40 50 75 80 100	426 262 238 203 181 147 140 124 101	558 347 316 271 243 196 189 169 137	927 591 540 469 420 344 333 298	1,110 701 640 554 496 406 393 350 287	1,740 1,120 1,030 896 806 663 643 578	2,170 1,380 1,270 1,100 986 809 768 703	4,100 2,560 2,330 2,010 1,790 1,460 1,410 1,260 1,020	ousar 4,720 2,950 2,690 2,320 2,070 1,690 1,630 1,450 1,180	7,130 4,560 4,180 3,630 3,260 2,680 2,590 2,330 1,910	7,958 5,147 4,719 4,116 3,702 3,053 2,961 2,662 2,195	Pr Hour 15,200 9,550 8,710 7,530 6,730 6,730 5,480 5,300 4,740	16,800 10,700 9,790 8,500 7,610 6,230 6,040 5,410	29,400 18,800 17,200 14,900 13,400 11,000 10,600 9,530	21, [*] 19, [*] 17, [*] 15, [*] 12,
Designation: Length (ft) 10 25 30 40 50 75 80 100 150	426 262 238 203 181 147 140 124 101 86	558 347 316 271 243 196 189 169 137 118	927 591 540 469 420 344 333 298 245	1,110 701 640 554 496 393 350 287 248	1,740 1,120 1,030 896 806 663 643 578 477	2,170 1,380 1,270 1,100 986 809 768 703 575	4,100 2,560 2,330 2,010 1,790 1,460 1,410 1,260 1,020	ousar 4,720 2,950 2,690 2,320 2,070 1,690 1,630 1,450 1,450 1,180 1,020	7,130 4,560 4,180 3,630 3,260 2,680 2,590 2,330 1,910 1,660	7,958 5,147 4,719 4,116 3,702 3,053 2,961 2,662 2,195 1,915	er Hour 15,200 9,550 8,710 7,530 6,730 5,480 5,300 4,740 3,860	16,800 10,700 9,790 8,500 7,610 6,230 6,040 5,410 4,430 3,840	29,400 18,800 17,200 14,900 13,400 11,000 10,600 9,530 7,810 6,780	21, 19, 17, 15, 12, 12, 10, 8,8 7,7
Designation: Length (ft) 10 25 30 40 50 75 80 100 150 200 250	426 262 238 203 181 147 140 124 101 86	558 347 316 271 243 196 189 169 137 118 105	927 591 540 469 420 344 333 298 245 213 191	1,110 701 640 554 496 406 393 350 287 248 222	1,740 1,120 1,030 896 806 663 643 578 477 415 373	2,170 1,380 1,270 1,100 986 809 768 703 575 501 448	4,100 2,560 2,330 2,010 1,790 1,460 1,410 1,260 1,020 880 785	ousar 4,720 2,950 2,690 2,320 2,070 1,690 1,630 1,450 1,180 1,180 1,020 910	7,130 4,560 4,180 3,630 3,260 2,680 2,590 2,330 1,910 1,660 1,490	7,958 5,147 4,719 4,116 3,702 3,053 2,961 2,662 2,195 1,915 1,722	er Hour 15,200 9,550 8,710 7,530 6,730 5,480 5,300 4,740 3,860 3,340 2,980	16,800 10,700 9,790 8,500 7,610 6,230 6,040 5,410 4,430 3,840 3,440	29,400 18,800 17,200 14,900 13,400 11,000 10,600 9,530 7,810 6,780 6,080	21, ⁷ 19, ¹ 17, ² 15, ¹ 12, ¹ 12, ² 10, ⁹ 8, ⁸ 7, ⁷ 6, ⁹
Designation: Length (ft) 10 25 30 40 50 75 80 100 150 200	426 262 238 203 181 147 140 124 101 86 77	558 347 316 271 243 196 189 169 137 118 105 96	927 591 540 469 420 344 333 298 245 213	1,110 701 640 554 496 406 393 350 287 248 222 203	1,740 1,120 1,030 896 806 663 643 578 477 415	2,170 1,380 1,270 1,100 986 809 768 703 575 501	4,100 2,560 2,330 2,010 1,790 1,460 1,410 1,260 1,020 880	ousar 4,720 2,950 2,690 2,320 2,070 1,690 1,630 1,450 1,450 1,180 1,020 910 829	7,130 4,560 4,180 3,630 3,260 2,680 2,590 2,330 1,910 1,660 1,490 1,360	7,958 5,147 4,719 4,116 3,702 3,053 2,961 2,662 2,195 1,915 1,915 1,722 1,578	Er Hour 15,200 9,550 8,710 7,530 6,730 5,480 5,300 4,740 3,860 3,340	16,800 10,700 9,790 8,500 7,610 6,230 6,040 5,410 4,430 3,840	29,400 18,800 17,200 14,900 13,400 11,000 10,600 9,530 7,810 6,780	21, ⁷ 19, ¹ 17, ² 15, ¹ 12, ¹ 12, ² 10, ¹ 8, 8

EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency between different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing.

Notes:

(1) Table does not include effect of pressure drop across the line regulator. Where regulator loss exceeds $\frac{1}{2}$ psi (based on 13 in. w.c. outlet pressure), do not use this table. Consult with regulator manufacturer for pressure drops and capacity factors. Pressure drops across a

regulator may vary with flow rate.

(2) CAUTION: Capacities shown in table may exceed maximum capacity for a selected regulator. Consult with regulator or tubing manufacturer for guidance.

(3) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger number of bends and/or fittings shall be increased by an equivalent length of tubing according to the following equation: L = 1.3n, where L is additional length (ft) of tubing and n is the number of additional fittings and/or bends.

(4) All table entries are rounded to 3 significant digits.

Table 6.3.1(j) Corrugated Stainless Steel Tubing (CSST)

_	_	_	_	_	_	_	_	_	_	-		<u>Gas:</u>	Undil Propa
-	_	_	_	_	_	_	_	-	_	-	Pre	Inlet ssure:	<u>5.0 p</u> s
_	_	_	_	_	_	_	_	_	_	_	Pro	essure Drop:	<u>3.5 p</u> s
-	_	_	_	_	_	_	_	-	_	-		pecific ravity:	<u>1.50</u>
_							Tub	e Size	<u>e (EHD)</u>				
Flow Designation:	<u>13</u>	<u>15</u>	<u>18</u>	<u>19</u>	<u>23</u>	<u>25</u>	<u>30</u>	<u>31</u>	<u>37</u>	<u>39</u>	<u>46</u>	<u>48</u>	<u>60</u>
<u>Length (ft)</u>					<u>Cap</u>	<u>acity</u>	in The	ousan	ds of B	<u>tu per l</u>	Hour		
10	826	1,070	1,710	2,060	3,150	4,000	7,830	8,950	13,100	14,441	28,600	31,200	54,400
25	509	664	1,090	1,310	2,040	2,550	4,860	5,600	8,400	9,339	18,000	19,900	34,700
30	461	603	999	1,190	1,870	2,340	4,430	5,100	7,680	8,564	16,400	18,200	31,700
40	396	520	867	1,030	1,630	2,030	3,820	4,400	6,680	7,469	14,200	15,800	27,600
50	352	463	777	926	1,460	1,820	3,410	3,930	5,990	6,717	12,700	14,100	24,700
75	284	376	637	757	1,210	1,490	2,770	3,190	4,920	5,539	10,300	11,600	20,300
80	275	363	618	731	1,170	1,450	2,680	3,090	4,770	5,372	9,990	11,200	19,600
100	243	324	553	656	1,050	1,300	2,390	2,760	4,280	4,830	8,930	10,000	17,600
150	196	262	453	535	866	1,060	1,940	2,240	3,510	3,983	7,270	8,210	14,400
200	169	226	393	464	755	923	1,680	1,930	3,050	3,474	6,290	7,130	12,500
250	150	202	352	415	679	828	1,490	1,730	2,740	3,124	5,620	6,390	11,200
300	136	183	322	379	622	757	1,360	1,570	2,510	2,865	5,120	5,840	10,300
400	117	158	279	328	542	657	1,170	1,360	2,180	2,498	4,430	5,070	8,920
500	104	140	251	294	488	589	1,050	1,210	1,950	2,247	3,960	4,540	8,000

EHD: Equivalent hydraulic diameter. A measure of the relative hydraulic efficiency between different tubing sizes. The greater the value of EHD, the greater the gas capacity of the tubing.

Notes:

(1) Table does not include effect of pressure drop across the line regulator. Where regulator loss exceeds ¹/₂ psi (based on 13 in. w.c. outlet pressure), do not use this table. Consult with regulator manufacturer for pressure drops and capacity factors. Pressure drops across a regulator may vary with flow rate.

(2) CAUTION: Capacities shown in table may exceed maximum capacity for a selected regulator. Consult with regulator or tubing manufacturer for guidance.

(3) Table includes losses for four 90 degree bends and two end fittings. Tubing runs with larger number of bends and/or fittings shall be increased by an equivalent length of tubing according

	lvethvlen	e Plastic F	Pipe					
						Gas:	Undilute Propane	<u>d</u>
-	-	-	-	-	Inlet P	ressure:	11.0 in. w	/.C.
-	-	-	-	-		re Drop:	0.5 in. w.	
-	-	-	-	-	<u></u>		<u>0.5 m. w.</u>	<u>c.</u>
						Specific Gravity:	1.50	
- NTENDED USI	- F· PF Pir	- e Sizina	- Between	- Integral	Second-9			Tank or
		Stage (Lo						
				Pipe S	Size (in.)			
- Nominal OD:	1/2	3/4	1	<u>11/4</u>	1 ¹ / ₂	2	3	<u>4</u>
	SDR							
Designation:	9.3	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 10</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>
Actual ID:	<u>0.660</u>	<u>0.860</u>	<u>1.077</u>	<u>1.328</u>	<u>1.554</u>	<u>1.943</u>	<u>2.864</u>	<u>3.682</u>
Length (ft)		<u>C</u>	apacity i	n Thousa	ands of B	<u>stu per Ho</u>	<u>our</u>	
10	340	680	1,230	2,130	3,210	5,770	16,000	30,900
20	233	468	844	1,460	2,210	3,970	11,000	21,200
30	187	375	677	1,170	1,770	3,180	8,810	17,000
40	160	321	580	1,000	1,520	2,730	7,540	14,600
50	142	285	514	890	1,340	2,420	6,680	12,900
60	129	258	466	807	1,220	2,190	6,050	11,700
70	119	237	428	742	1,120	2,010	5,570	10,800
80	110	221	398	690	1,040	1,870	5,180	10,000
90	103	207	374	648	978	1,760	4,860	9,400
100	98	196	353	612	924	1,660	4,590	8,900
125	87	173	313	542	819	1,470	4,070	7,900
150	78	157	284	491	742	1,330	3,690	7,130
175	72	145	261	452	683	1,230	3,390	6,560
200	67	135	243	420	635	1,140	3,160	6,100
250	60	119	215	373	563	1,010	2,800	5,410
300	54	108	195	338	510	916	2,530	4,900
350	50	99	179	311	469	843	2,330	4,510
400	46	92	167	289	436	784	2,170	4,190
450	43	87	157	271	409	736	2,040	3,930
500	41	82	148	256	387	695	1,920	3,720

Table 6.3.1(I) Polyethylene Plastic Pipe

-	-	_	-	<u>Gas:</u>	Undiluted Propane
-	-	_	-	Inlet Pressure:	<u>2.0 psi</u>
-	-	_	-	Pressure Drop:	<u>1.0 psi</u>

-	_	_		_	<u>Specific</u>	Gravity:	<u>1.50</u>	
INTENDED U	SE: PE P	<u>Pipe Sizin</u>		en 2 psi S gulator.	ervice R	egulator a	and Line P	ressure
_				Pipe	<u>Size (in.)</u>			
Nominal OD:	1 <u>/</u> 2	3/4	1	<u>1¼</u>	<u>11/2</u>	<u>2</u>	<u>3</u>	<u>4</u>
Designation:	<u>SDR</u> <u>9.3</u>	<u>SDR</u> <u>11</u>	<u>SDR 11</u>	<u>SDR 10</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>	<u>SDR 11</u>
Actual ID:	<u>0.660</u>	<u>0.860</u>	<u>1.077</u>	<u>1.328</u>	<u>1.554</u>	<u>1.943</u>	<u>2.864</u>	<u>3.682</u>
Length (ft)			Capacity	in Thous	ands of E	<u>Stu per H</u>	our	
10	3,130	6,260	11,300	19,600	29,500	53,100	147,000	284,000
20	2,150	4,300	7,760	13,400	20,300	36,500	101,000	195,000
30	1,730	3,450	6,230	10,800	16,300	29,300	81,100	157,000
40	1,480	2,960	5,330	9,240	14,000	25,100	69,400	134,100
50	1,310	2,620	4,730	8,190	12,400	22,200	61,500	119,000
60	1,190	2,370	4,280	7,420	11,200	20,100	55,700	108,000
70	1,090	2,180	3,940	6,830	10,300	18,500	51,300	99,100
80	1,010	2,030	3,670	6,350	9,590	17,200	47,700	92,200
90	952	1,910	3,440	5,960	9,000	16,200	44,700	86,500
100	899	1,800	3,250	5,630	8,500	15,300	42,300	81,700
125	797	1,600	2,880	4,990	7,530	13,500	37,500	72,400
150	722	1,450	2,610	4,520	6,830	12,300	33,900	65,600
175	664	1,330	2,400	4,160	6,280	11,300	31,200	60,300
200	618	1,240	2,230	3,870	5,840	10,500	29,000	56,100
250	548	1,100	1,980	3,430	5,180	9,300	25,700	49,800
300	496	994	1,790	3,110	4,690	8,430	23,300	45,100
350	457	914	1,650	2,860	4,320	7,760	21,500	41,500
400	425	851	1,530	2,660	4,020	7,220	12,000	38,600
450	399	798	1,440	2,500	3,770	6,770	18,700	36,200
500	377	754	1,360	2,360	3,560	6,390	17,700	34,200
550	358	716	1,290	2,240	3,380	6,070	16,800	32,500
600	341	683	1,230	2,140	3,220	5,790	16,000	31,000
650	327	654	1,180	2,040	3,090	5,550	15,400	29,700
700	314	628	1,130	1,960	2,970	5,330	14,700	28,500
750	302	605	1,090	1,890	2,860	5,140	14,200	27,500
800	292	585	1,050	1,830	2,760	4,960	13,700	26,500
850	283	566	1,020	1,770	2,670	4,800	13,300	25,700
900	274	549	990	1,710	2,590	4,650	12,900	24,900
950	266	533	961	1,670	2,520	4,520	12,500	24,200
1,000	259	518	935	1,620	2,450	4,400	12,200	23,500
1,100	246	492	888	1,540	2,320	4,170	11,500	22,300
1,200	234	470	847	1,470	2,220	3,980	11,000	21,300
1,300	225	450	811	1,410	2,120	3,810	10,600	20,400
1,400	216	432	779	1,350	2,040	3,660	10,100	19,600
1,500	208	416	751	1,300	1,960	3,530	9,760	18,900

1,600	201	402	725	1,260	1,90		3,410	9,430	18,200
1,700	194	389	702	1,220	1,84	40	3,300	9,130	17,600
1,800	188	377	680	1,180	1,78	30	3,200	8,850	17,100
1,900	183	366	661	1,140	1,73	30	3,110	8,590	16,600
2,000	178	356	643	1,110	1,68	30	3,020	8,360	16,200
ote: All table e	ntries are	rounded	to 3 signi	ficant digi	ts.				
able 6.3.1(m) I	Polyethyle	ne Plasti	c Tubing						
_					Gas:	Und	diluted P	ropane	
-			lr	nlet Press	sure:	<u>11.(</u>) in. w.c.		
-			P	ressure C	rop:	0.5	in. w.c.		
_			Spe	ecific Gra	<u>vity:</u>	1.5	<u>0</u>		
	SE: Sizin	g Betwee	en Integra	al 2-Stage	Reg	ulat	or at Tan	k or Secol	nd-Stage
				<u>gulator) a</u>					
		<u>Pla</u>	stic Tubi	<u>ng Size (</u>	<u>CTS)</u>	(<u>in.</u>)			
Nor	ninal OD:		¹ /2					<u>1</u>	
Des	ignation:		<u>SDR</u>	2 7				<u>SDR 11</u>	
4	Actual ID:		<u>0.44</u>	<u>15</u>				<u>0.927</u>	
Length	(<u>ft</u>)		<u>Cap</u>	<u>acity in T</u>	hous	and	<u>s of Btu p</u>	<u>per Hour</u>	
10			121					828	
20			83					569	
30			67					457	
40			57					391	
50			51					347	
60			46					314	
70			42					289	
80			39					269	
90			37					252	
100			35					238	
125			31					211	
150			28					191	
175			26					176	
200			24					164	
225			22					154	
250			21					145	
275			20					138	
300			19					132	
350			18					121	
400			16					113	
450			15					106	
500			15					100	

CTS: Copper tube size.

Note: All table entries are rounded to 3 significant digits.

6.3.2

Section 6.4 shall be used in conjunction with one of the methods described in 6.1.2 through 6.1.4 for non-corrugated stainless steel tubing.

6.4 Sizing Equations.

The inside diameter of smooth wall pipe or tubing shall be determined by the sizing equations in 6.4.1 and 6.4.2 using the equivalent pipe length determined by the methods in 6.1.2 through 6.1.4.

6.4.1* Low-Pressure Gas Formula.

Less than 1.5 psi (10.3 kPa):

$$D = \frac{Q^{0.381}}{19.17 \left(\frac{\Delta H}{Cr \times L}\right)^{0.206}}$$
[6.4.1]

where:

D = inside diameter of pipe (in.)

Q = input rate appliance(s) (cubic feet per hour at 60°F and 30 in. mercury column)

 ΔH = pressure drop [in. w.c. (27.7 in. H₂O = 1 psi)]

L = equivalent length of pipe (ft) See Table 6.4.2 for values of Cr.

6.4.2* High-Pressure Gas Formula.

1.5 psi (10.3 kPa) and above:

$$D = \frac{Q^{0.381}}{18.93 \left[\frac{\left(P_1^2 - P_2^2\right) \cdot Y}{Cr \times L} \right]^{0.206}}$$
[6.4.2]

where:

D = inside diameter of pipe (in.)

Q = input rate appliance(s) (cubic feet per hour at 60°F and 30 in. mercury column)

 P_1 = upstream pressure [psia (P_1 + 14.7)]

 P_2 = downstream pressure [psia (P_2 + 14.7)]

L = equivalent length of pipe (ft)

See Table 6.4.2 for values of Cr and Y.

Table 6.4.2 Cr and Y for Natural Gas and Undiluted Propane at Standard Conditions

-	<u>Formula</u>	a Factors
Gas	<u>Cr</u>	<u>Y</u>
Natural gas	0.6094	0.9992
Undiluted propane	1.2462	0.9910

Additional Proposed Changes

File Name	Description
Public_Comment_No43-NFPA_54-2022.docx	PC 43 in WORD Format

82 of 127

Approved

Statement of Problem and Substantiation for Public Comment

Sizing tables for PEX-AL-PEX piping have traditionally been found in the manufacturer's instructions. This PC adds the sizing tables to the standard.

Related Item

• Public Input No. 91-NFPA 54-2021

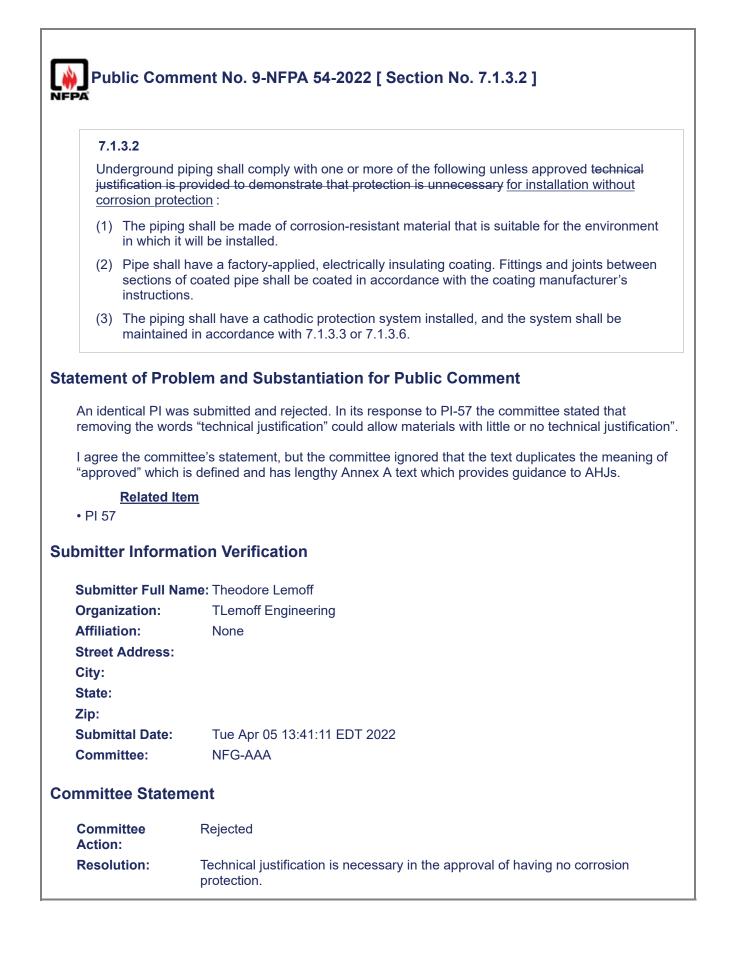
Submitter Information Verification

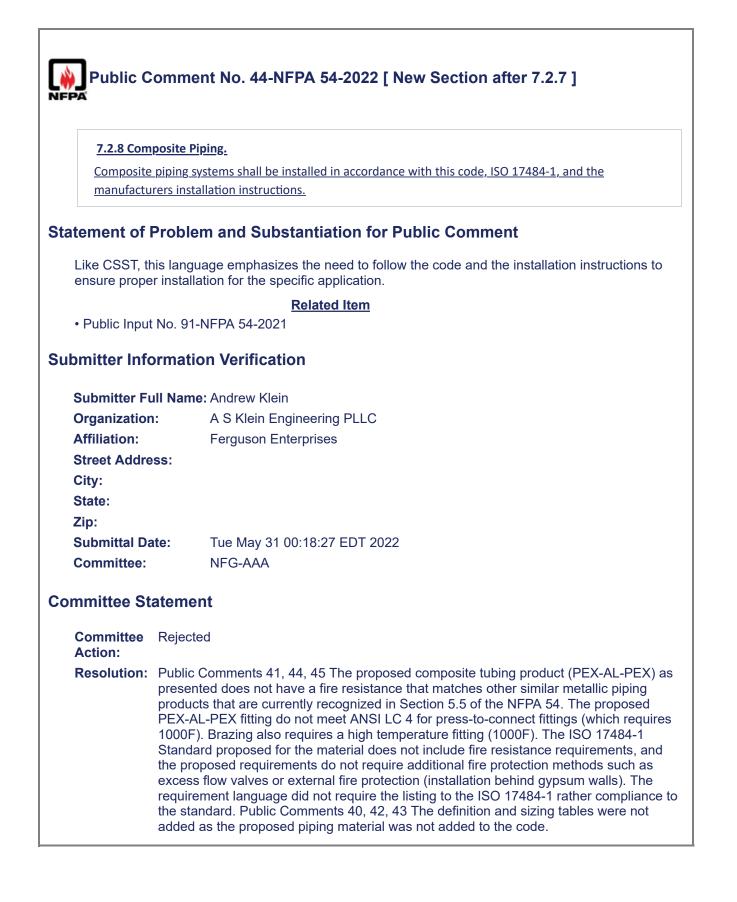
Submitter Full Name	e: Andrew Klein
Organization:	A S Klein Engineering PLLC
Affiliation:	Ferguson Enterprises
Street Address:	
City:	
State:	
Zip:	
Submittal Date:	Mon May 30 23:47:10 EDT 2022
Committee:	NFG-AAA

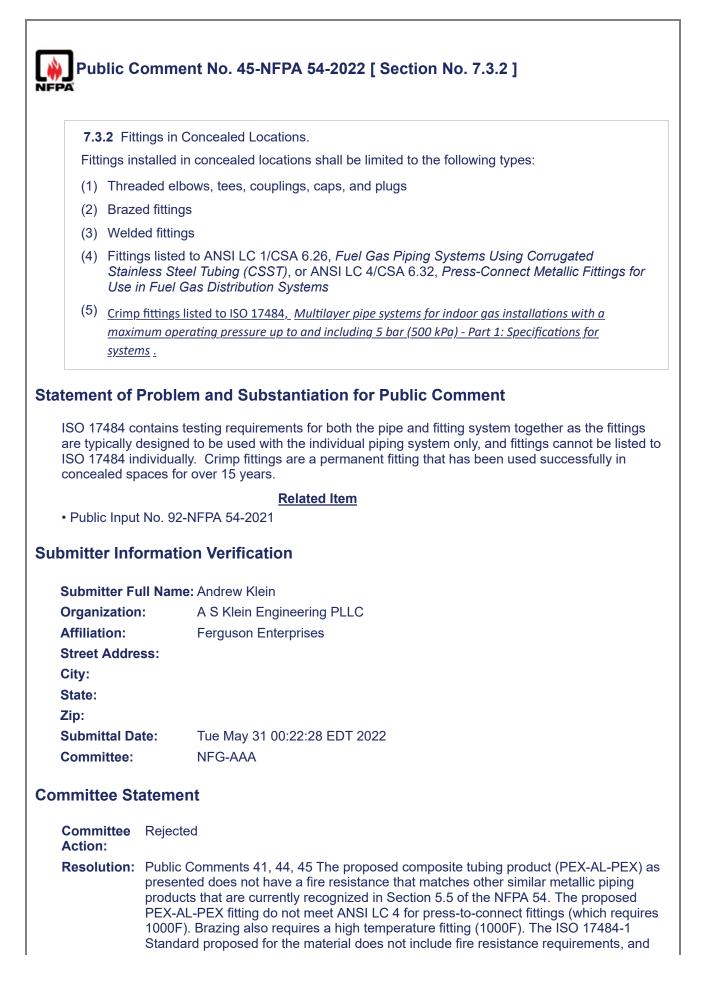
Committee Statement

Committee
Action:RejectedResolution:Public Comments 41, 44, 45 The proposed composite tubing product (PEX-AL-PEX) as
presented does not have a fire resistance that matches other similar metallic piping
products that are currently recognized in Section 5.5 of the NFPA 54. The proposed
PEX-AL-PEX fitting do not meet ANSI LC 4 for press-to-connect fittings (which requires
1000F). Brazing also requires a high temperature fitting (1000F). The ISO 17484-1
Standard proposed for the material does not include fire resistance requirements, and
the proposed requirements do not require additional fire protection methods such as
excess flow valves or external fire protection (installation behind gypsum walls). The
requirement language did not require the listing to the ISO 17484-1 rather compliance to
the standard. Public Comments 40, 42, 43 The definition and sizing tables were not
added as the proposed piping material was not added to the code.

FA	
6.1.4 Hybrid	Pressure.
	o for each section of higher pressure gas piping shall be determined Pressure. Sizing of high and low pressure portions of a hybrid pressure system rmined:
<u>a. For the hig</u> branch length regulator.	<u>h pressure portion</u> <u>using the longest length of piping</u> <u>method in 6.1.1 or the</u> <u>n method in 6.1.2</u> from the point of delivery to the most remote line pressure e from the line pressure regulator to each outlet shall be determined using the
length of pipil	ng from the regulator to the most remote outlet served by the regulator
or the branch	ection of lower pressure piping using the longest length of piping method in 6.1.1 length method in 6.1.2 from the line pressure regulator to the outlets consistent g method used .
	nize that the longest length and branch length sizing methods should be used to siz pressure portions of a hybrid system, and make the requirement easier to
the high and low	pressure portions of a hybrid system, and make the requirement easier to
the high and low understand. <u>Related It</u> • PI-5	pressure portions of a hybrid system, and make the requirement easier to
the high and low understand. • PI-5 bmitter Inform	pressure portions of a hybrid system, and make the requirement easier to <u>em</u>
the high and low understand. • PI-5 bmitter Inform	pressure portions of a hybrid system, and make the requirement easier to <u>em</u> nation Verification
the high and low understand. • PI-5 bmitter Inform Submitter Full N Organization: Affiliation:	pressure portions of a hybrid system, and make the requirement easier to em nation Verification Name: Theodore Lemoff TLemoff Engineering Omega Flex
the high and low understand. • PI-5 bmitter Inform Submitter Full N Organization: Affiliation: Street Address:	pressure portions of a hybrid system, and make the requirement easier to em nation Verification Name: Theodore Lemoff TLemoff Engineering Omega Flex
the high and low understand. • PI-5 bmitter Inform Submitter Full N Organization: Affiliation: Street Address: City:	pressure portions of a hybrid system, and make the requirement easier to em nation Verification Name: Theodore Lemoff TLemoff Engineering Omega Flex
the high and low understand. • PI-5 bmitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State:	pressure portions of a hybrid system, and make the requirement easier to em nation Verification Name: Theodore Lemoff TLemoff Engineering Omega Flex
the high and low understand. • PI-5 bmitter Inform Submitter Full N Organization: Affiliation: Street Address: City:	pressure portions of a hybrid system, and make the requirement easier to em nation Verification Name: Theodore Lemoff TLemoff Engineering Omega Flex
the high and low understand. <u>Related It</u> • PI-5 bmitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State: Zip:	pressure portions of a hybrid system, and make the requirement easier to em nation Verification Name: Theodore Lemoff TLemoff Engineering Omega Flex
the high and low understand. • PI-5 bmitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State: Zip: Submittal Date:	pressure portions of a hybrid system, and make the requirement easier to em hation Verification Name: Theodore Lemoff TLemoff Engineering Omega Flex Tue Apr 05 13:26:33 EDT 2022 NFG-AAA
the high and low understand. Related It • PI-5 bmitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State: Zip: Submittal Date: Committee:	pressure portions of a hybrid system, and make the requirement easier to em hation Verification Name: Theodore Lemoff TLemoff Engineering Omega Flex Tue Apr 05 13:26:33 EDT 2022 NFG-AAA

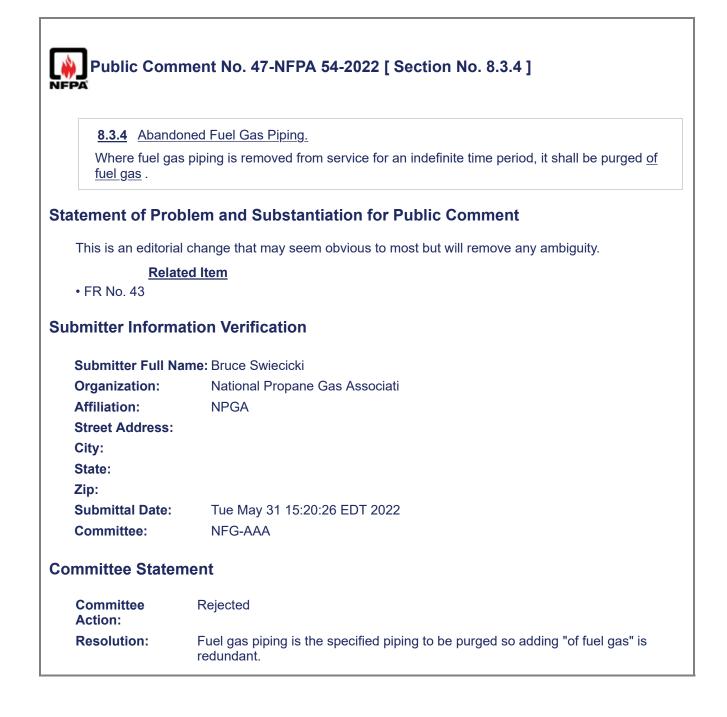




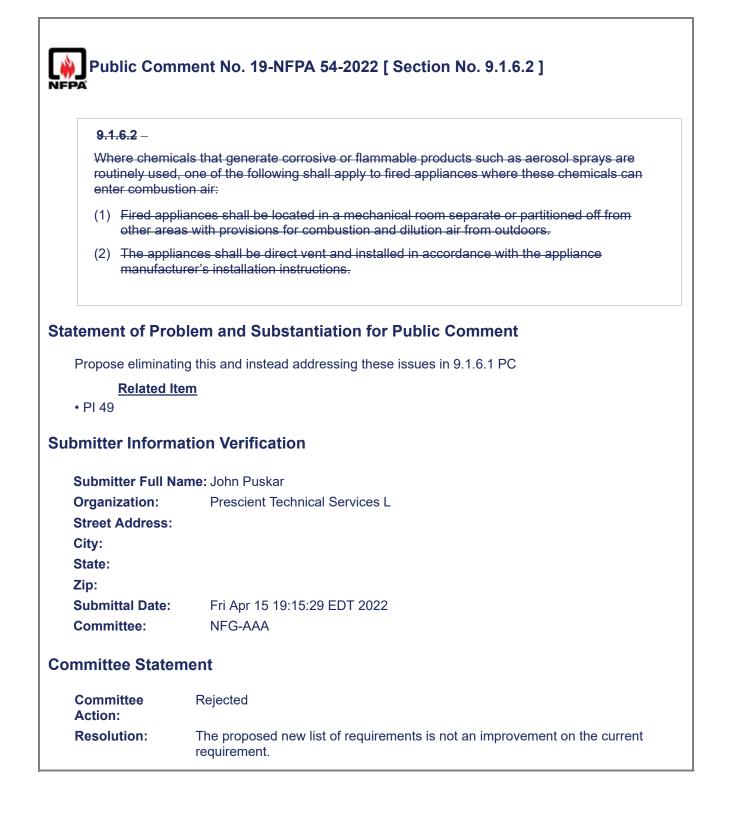


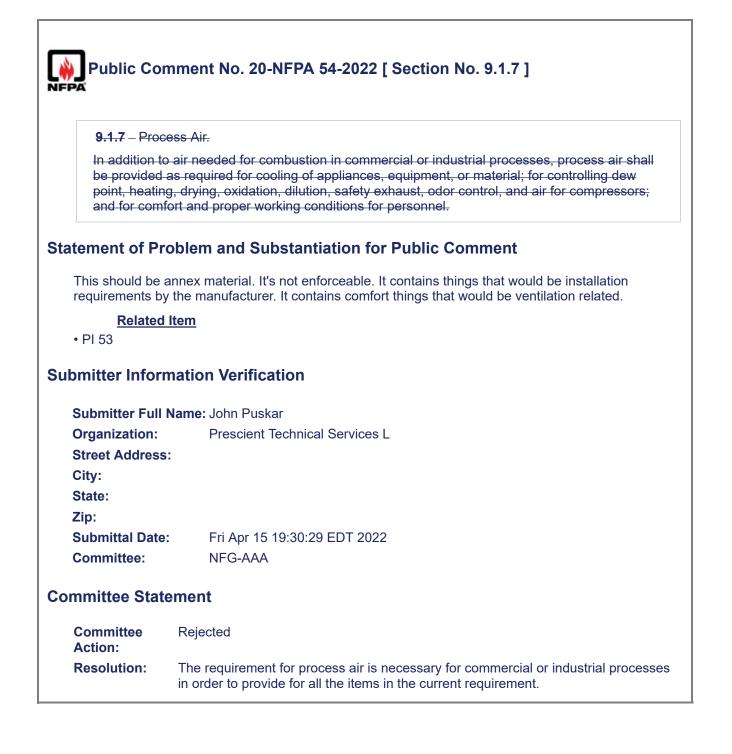
the proposed requirements do not require additional fire protection methods such as excess flow valves or external fire protection (installation behind gypsum walls). The requirement language did not require the listing to the ISO 17484-1 rather compliance to the standard. Public Comments 40, 42, 43 The definition and sizing tables were not added as the proposed piping material was not added to the code.

	ment No. 10-NFPA 54-2022 [Section No. 8.2.3]
8.2.3* Leak (Check.
	diately after the gas is turned on into a new system or into a system that has been ad after an interruption of service, the piping system shall be checked for leakage.
8.2.3.2 Where have been ma	e leakage is indicated, the gas supply shall be shut off until the necessary repairs ide.
8.2.3.3 Where checks shall b	e minor repairs have been made in accordance with 8.1.1.3, no additional leak e required.
tatement of Pro	blem and Substantiation for Public Comment
to placing the sys for leak testing pr	jected this recommendation in PI-64 stating: "Any repairs require a leak check prior tem back into use." The proposed reference to 8.1.1.3, which includes requirements ovides this check. The committee's technical substantiation did not support the and this comment should be accepted.
Related It	
• PI 64	
ubmitter Inform	ation Verification
Submitter Full N	ame: Theodore Lemoff
Organization:	TLemoff Engineering
Affiliation:	None
Street Address:	
City:	
State:	
State: Zip:	
	Tue Apr 05 13:46:24 EDT 2022
Zip:	Tue Apr 05 13:46:24 EDT 2022 NFG-AAA
Zip: Submittal Date:	NFG-AAA
Zip: Submittal Date: Committee:	NFG-AAA



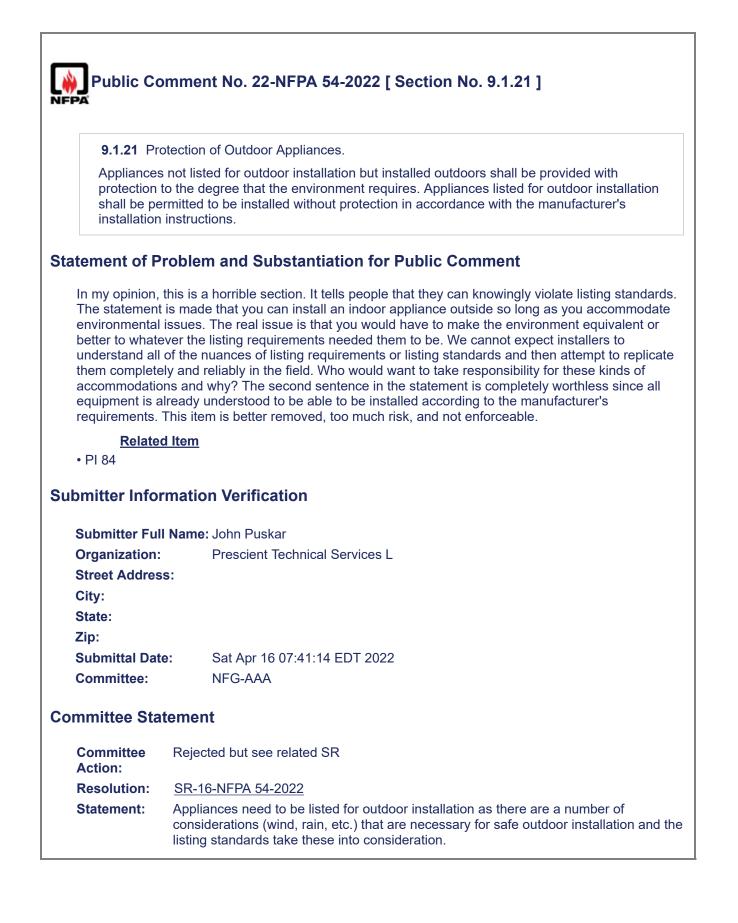
Public Com	ment No. 18-NFPA 54-2022 [Section No. 9.1.6.1]
9.1.6.1	
monoxide, hyd present, means	ve- <u>corrosive fumes</u> or flammable process fumes or gases , such as carbon rogen sulfide, ammonia, chlorine, and halogenated hydrocarbons, as are s for their safe disposal shall be provided. <u>are present in the appliance operating concentrations that can compromise the appliances safe operations the be provided:</u>
<u>a) A means for</u>	safe disposal or dilution of the corrosive fumes shall be provided.
<u>b) The applian</u>	ce shall be listed and labeled for the environmental conditions.
	nces shall be located in a mechanical room separate or partitioned off from other visions for combustion and dilution air from outdoors.
	ce shall be direct vent and installed in accordance with the appliance installation instructions.
Statement of Prob	plem and Substantiation for Public Comment
nothing is listed to	nazardous condition and also not compliant with a listing requirement. Likely that be operated in a flammable environment. This revision has been reduced in ade more focused on what I believe the original intent of this item was, (corrosive)
Submitter Informa	ation Verification
Submitter Full Na	me. John Puskar
Organization: Street Address: City: State: Zip:	
Submittal Date:	Fri Apr 15 18:55:55 EDT 2022
Committee:	NFG-AAA
Committee Staten	nent
Committee Action:	Rejected





PA	
9.1.8.2	
	cations selected for installation of appliances and equipment , the <u>are other than at</u> slab or within a basement the following shall be provided:
must be val	amic and static load <u>-</u> carrying capacities of the building structure shall be checked <u>idated by a licensed engineer</u> to determine whether they are <u>that they are</u> o carry the additional loads.
	liances and equipment shall be supported and shall be connected to the piping so tert undue stress on the connections.
atement of P	roblem and Substantiation for Public Comment
	The is installed of a slab in a basement of at grade since the load is not then supported
by the building Related • PI 83	
• PI 83	structure.
Related • PI 83 Ibmitter Infor	structure. <u>d Item</u>
Related • PI 83 Ibmitter Infor Submitter Full Organization: Street Address City:	structure. <u>d Item</u> mation Verification Name: John Puskar Prescient Technical Services L
Related • PI 83 ubmitter Infor Submitter Full Organization: Street Address City: State:	structure. <u>d Item</u> mation Verification Name: John Puskar Prescient Technical Services L
Related • PI 83 Ibmitter Infor Submitter Full Organization: Street Address City:	structure. <u>d Item</u> <u>rmation Verification</u> I Name: John Puskar Prescient Technical Services L s:
Related • PI 83 Ibmitter Infor Submitter Full Organization: Street Address City: State: Zip:	structure. <u>d Item</u> <u>rmation Verification</u> I Name: John Puskar Prescient Technical Services L s:
Related • PI 83 Ibmitter Infor Submitter Full Organization: Street Address City: State: Zip: Submittal Date	structure. d Item mation Verification Name: John Puskar Prescient Technical Services L s: e: Sat Apr 16 07:28:30 EDT 2022 NFG-AAA
Related • PI 83 ubmitter Infor Submitter Full Organization: Street Address City: State: Zip: Submittal Data Committee:	structure. d Item mation Verification Name: John Puskar Prescient Technical Services L s: e: Sat Apr 16 07:28:30 EDT 2022 NFG-AAA

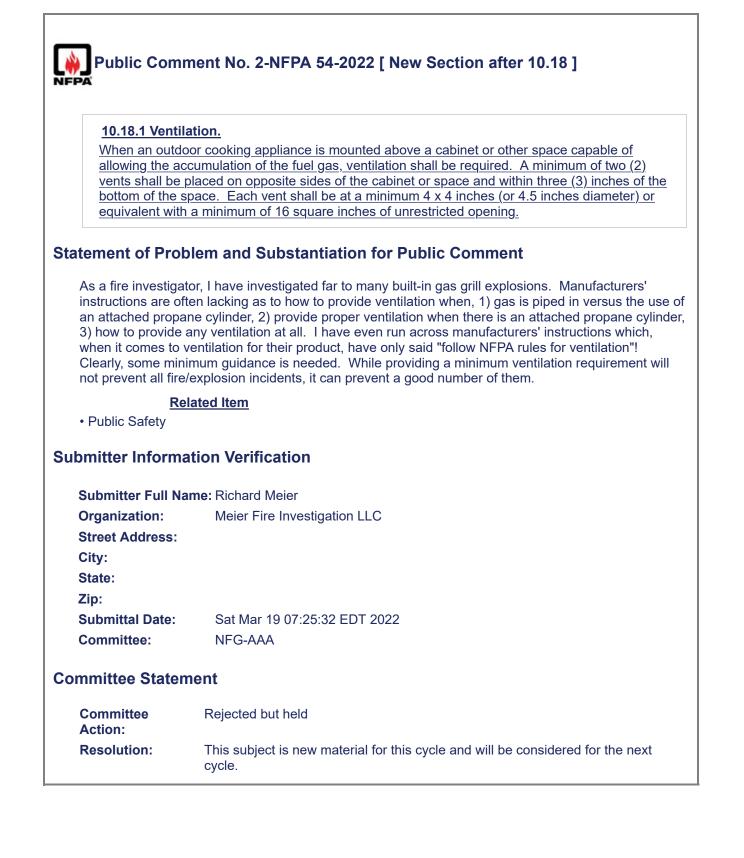
Resolution:	Gas appliance regulators are under the scope of the code and requirements are needed for them.
Committee Action:	Rejected
nmittee Staten	nent
Committee:	NFG-AAA
Submittal Date:	Fri May 20 13:52:17 EDT 2022
Zip:	
State:	
City:	
Street Address:	
Affiliation:	None
Organization:	TLemoff Engineering
Submitter Full Na	me: Theodore Lemoff
mitter Informa	tion Verification
• FR-12	
Related It	<u>em</u>
	e regulators are part of appliances, and are not covered by this Code, therefore uch regulators are deleted. Alternately, the requirement could be revised to requir lators.
tement of Prob	elem and Substantiation for Public Comment
operate or varie regulator listed	supply pressure is higher than that at which the appliance is designed to as beyond the design pressure limits of the appliance, a gas appliance pressure in accordance with ANSI Z21.18/CSA 6.3, <i>Gas Appliance Pressure</i> all be installed.
	ppliance Pressure Regulators.

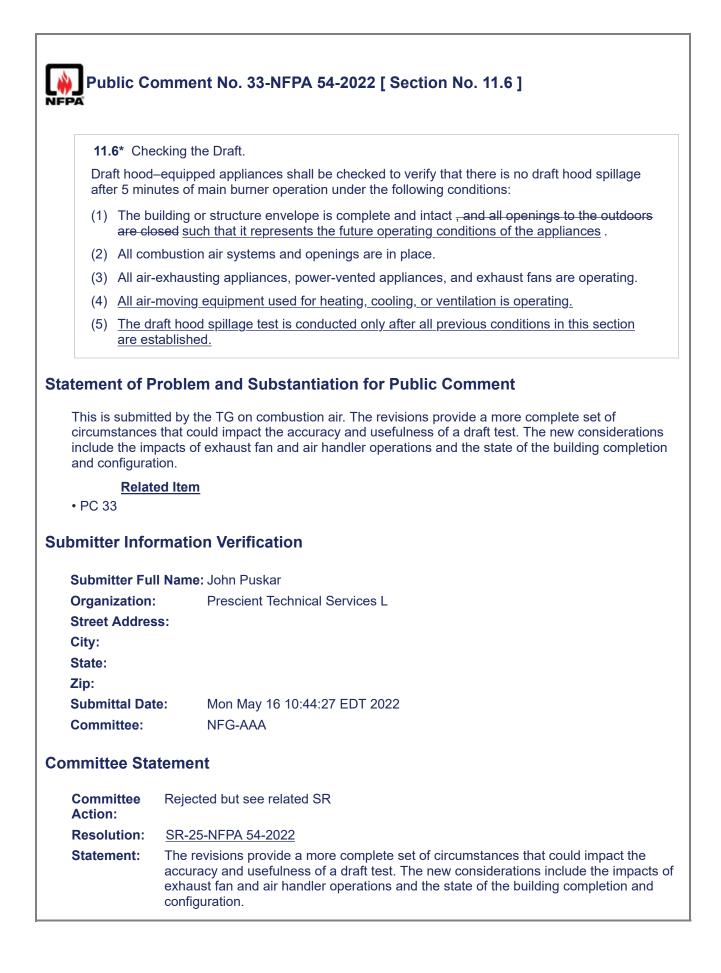


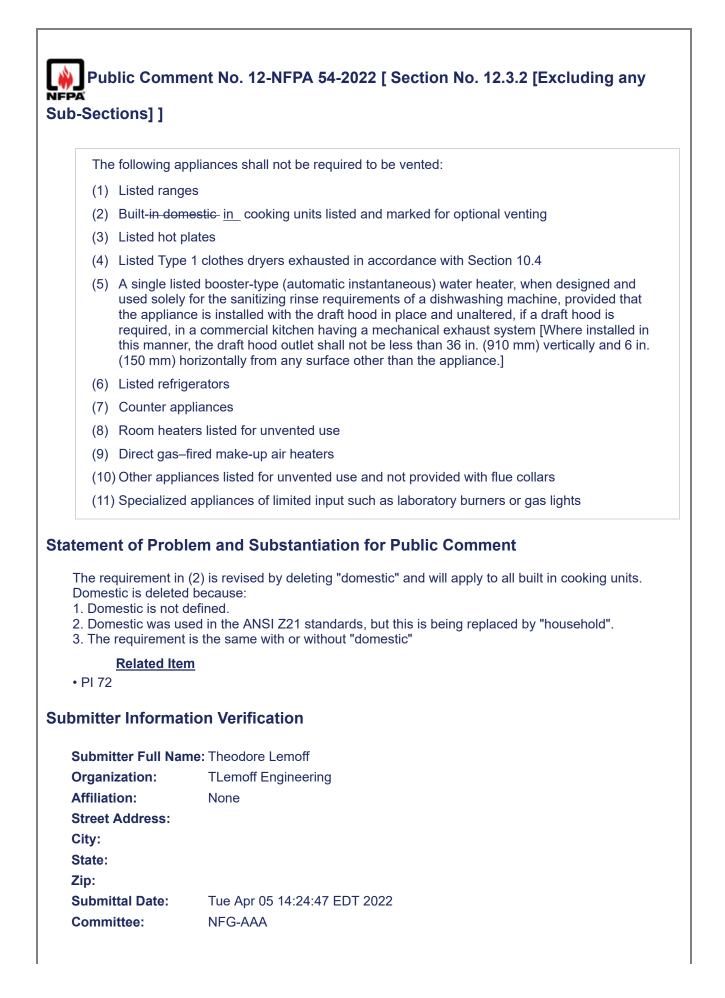
10.11.2 Clea	rance for Listed Appliances.
deep fat fryers ovens, shall b	or-mounted food service appliances, such as ranges for hotels and restaurants, s, unit broilers, kettles, steam cookers, steam generators, and baking and roasting be installed at least 6 in. (150 mm) from combustible material except that at least a clearance shall be maintained . <u>be provided</u> between a draft hood and naterial.
	or-mounted food service appliances listed for installation at lesser clearances shall accordance with the manufacturer's installation instructions.
<u>10.11.2.3</u> App be installed el	pliances designed and marked "For use only in noncombustible locations" shall not sewhere.
	mples of floor-mounted food service appliances are ranges for hotels and eep fat fryers, unit broilers, kettles, steam cookers, steam generators, and baking ovens.
2. The list of floor	ents is separated into 3 paragraphs, as they are separate requirements r-mounted food service appliances is relocated to Annex A as lists are never
3. The requireme	elong in Annex A. Int for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation.
3. The requireme clearance be prov this distance into <u>Related In</u>	ent for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation.
3. The requireme clearance be pro this distance into <u>Related In</u> • PI 70	ent for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation.
3. The requireme clearance be pro- this distance into <u>Related In</u> • PI 70 • mitter Inform	ent for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation.
3. The requireme clearance be pro- this distance into <u>Related In</u> • PI 70 • mitter Inform	ent for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation.
 3. The requireme clearance be protected and the protected	ent for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation. tem hation Verification hame: Theodore Lemoff
3. The requireme clearance be pro- this distance into <u>Related It</u> • PI 70 • mitter Inform Submitter Full N Organization: Affiliation:	ent for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation. tem tation Verification lame: Theodore Lemoff TLemoff Engineering
3. The requireme clearance be pro- this distance into <u>Related It</u> • PI 70 omitter Inform Submitter Full N Organization: Affiliation: Street Address: City:	ent for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation. tem tation Verification lame: Theodore Lemoff TLemoff Engineering
3. The requireme clearance be pro- this distance into <u>Related In</u> • PI 70 • Omitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State:	ent for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation. tem tation Verification lame: Theodore Lemoff TLemoff Engineering
3. The requireme clearance be pro- this distance into <u>Related It</u> • PI 70 • mitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State: Zip:	ent for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation. tem hation Verification Hame: Theodore Lemoff TLemoff Engineering None
3. The requireme clearance be pro- this distance into <u>Related In</u> • PI 70 • Omitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State: Zip: Submittal Date:	<pre>white for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation. tem hation Verification lame: Theodore Lemoff TLemoff Engineering None Wed Apr 06 14:42:30 EDT 2022</pre>
3. The requireme clearance be pro- this distance into <u>Related In</u> PI 70 mitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State: Zip: Submittal Date: Committee:	It for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation. tem hation Verification hame: Theodore Lemoff TLemoff Engineering None Wed Apr 06 14:42:30 EDT 2022 NFG-AAA
3. The requireme clearance be pro- this distance into <u>Related In</u> PI 70 mitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State: Zip: Submittal Date:	It for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation. tem hation Verification hame: Theodore Lemoff TLemoff Engineering None Wed Apr 06 14:42:30 EDT 2022 NFG-AAA
3. The requireme clearance be pro- chis distance into <u>Related In</u> PI 70 mitter Inform Submitter Full N Organization: Affiliation: Street Address: City: State: Zip: Submittal Date: Committee State	It for clearance between a draft hood and combustible material is revised that the vided, rather than maintained. It is not the responsibility of the installer to maintain the future, rather to ensure that is exists at the time of installation. tem hation Verification hame: Theodore Lemoff TLemoff Engineering None Wed Apr 06 14:42:30 EDT 2022 NFG-AAA

Statement: 1. The requirements is separated into 3 paragraphs, as they are separate requirements
2. The list of floor-mounted food service appliances is relocated to Annex A as lists are never complete, and belong in Annex A.
3. The requirement for clearance between a draft hood and combustible material is revised that the clearance be provided, rather than maintained. It is not the responsibility of the installer to maintain this distance into the future, rather to ensure that is exists at the time of installation.

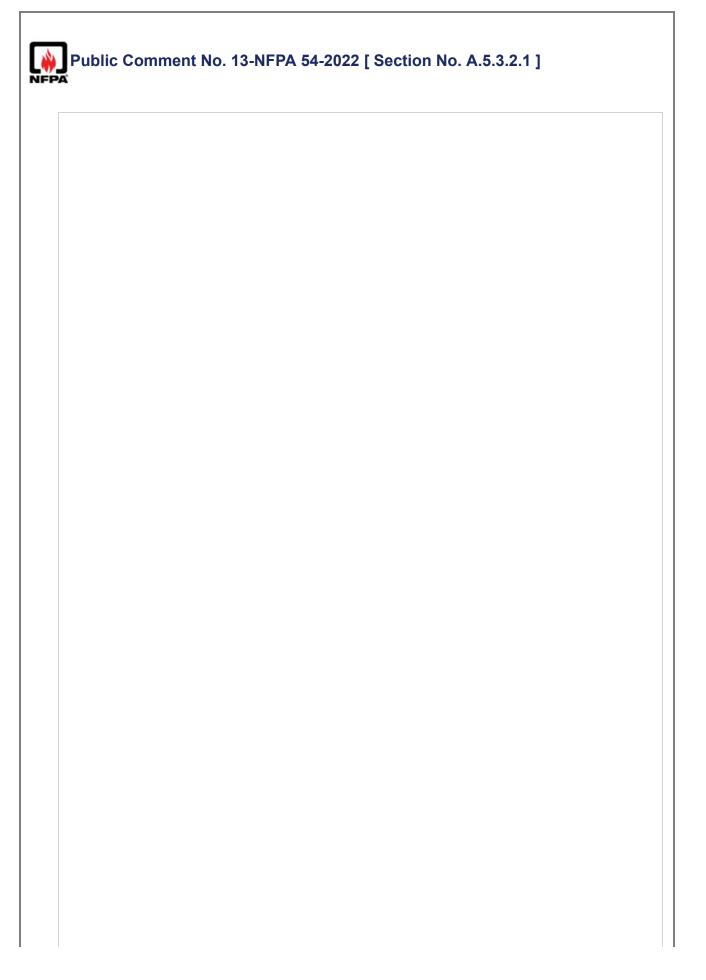
-	
	ction Above Domestic Units.
Domestic	
Above Open	Top Broilers.
than 0.0122 in and the unders	n-top broiler <u>units</u> _ <u>units</u> _shall be provided with a metal ventilating hood not less . (0.3 mm) thick with a clearance of not less than ¼ in. (6 mm) between the hood side of combustible material or metal cabinets A clearance of at least 24 in. I be maintained between the
cabinet, and th	<u>clearance between the</u> cooking top and the combustible material or metal e hood shall be at - <u>a minimum of 24 in. (610 mm) at</u> least as wide as the open- and centered over the unit Domestic
exhaust system	n-top broiler units <u>installed in residential occupancies</u> incorporating an integral n and listed for use without a ventilating hood shall not be required to be provided ng hood if installed in accordance with 10.13.3.1(1).
the requirement is <u>Related It</u> • PI 68	
the requirement is <u>Related It</u> • PI 68 bmitter Informa	a revised to be applicable to all open top broiler units.
the requirement is <u>Related It</u> • PI 68 bmitter Informa Submitter Full Na	arevised to be applicable to all open top broiler units.
the requirement is <u>Related It</u> • PI 68 omitter Informa Submitter Full Na Organization:	ation Verification ame: Theodore Lemoff TLemoff Engineering
the requirement is <u>Related It</u> • PI 68 bmitter Informa Submitter Full Na Organization: Affiliation:	arevised to be applicable to all open top broiler units.
the requirement is <u>Related It</u> • PI 68 Domitter Informa Submitter Full Na Organization: Affiliation: Street Address:	ation Verification ame: Theodore Lemoff TLemoff Engineering
the requirement is <u>Related Ita</u> • PI 68 Domitter Informa Submitter Full Na Organization: Affiliation: Street Address: City:	ation Verification ame: Theodore Lemoff TLemoff Engineering
the requirement is <u>Related It</u> • PI 68 Domitter Informa Submitter Full Na Organization: Affiliation: Street Address: City: State:	ation Verification ame: Theodore Lemoff TLemoff Engineering
the requirement is <u>Related Ita</u> • PI 68 Domitter Informa Submitter Full Na Organization: Affiliation: Street Address: City: State: Zip:	arevised to be applicable to all open top broiler units.
the requirement is <u>Related It</u> • PI 68 Domitter Informa Submitter Full Na Organization: Affiliation: Street Address: City: State:	ation Verification ame: Theodore Lemoff TLemoff Engineering
the requirement is <u>Related It</u> • PI 68 Domitter Informa Submitter Full Na Organization: Affiliation: Street Address: City: State: Zip: Submittal Date:	arevised to be applicable to all open top broiler units. am ation Verification ame: Theodore Lemoff TLemoff Engineering None Tue Apr 05 14:08:28 EDT 2022 NFG-AAA
the requirement is <u>Related Ita</u> • PI 68 bmitter Informa Submitter Full Na Organization: Affiliation: Street Address: City: State: Zip: Submittal Date: Committee:	arevised to be applicable to all open top broiler units. am ation Verification ame: Theodore Lemoff TLemoff Engineering None Tue Apr 05 14:08:28 EDT 2022 NFG-AAA
the requirement is <u>Related Ita</u> • PI 68 Domitter Informa Submitter Full Na Organization: Affiliation: Street Address: City: State: Zip: Submittal Date: Committee Stater Committee	erevised to be applicable to all open top broiler units. em ation Verification ame: Theodore Lemoff TLemoff Engineering None Tue Apr 05 14:08:28 EDT 2022 NFG-AAA nent







Committee Statement: Rejected but see related SR Action: SR-27-NFPA 54-2022 Tomestic is deleted because: Domestic is deleted because: 1. Domestic is not defined. 2. Domestic was used in the ANSI Z21 standards, but this is being replaced by "household". 3. The requirement is the same with or without "domestic" See Global SR32 for related multi-requirement changes.



A.5.3.2.1

Some older appliances do not have a nameplate. In this case Table A.5.3.2.1 or an estimate of the appliance input should be used. The input can be based on the following:

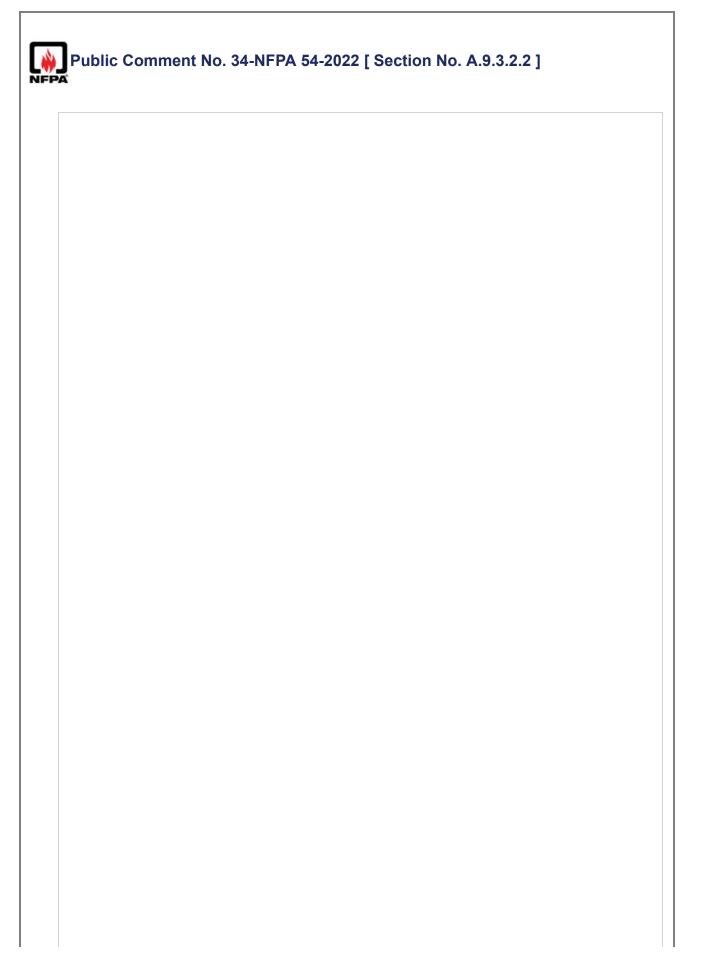
- (1) A rating provided by the manufacturer
- (2) The rating of similar appliances
- (3) Recommendations of the gas supplier
- (4) Recommendations of a qualified agency
- (5) A gas flow test
- (6) Measurement of the orifice size of the appliance

The requirement of 5.3.1 that the piping system provide sufficient gas to each appliance inlet must be complied with.

 Table A.5.3.2.1 Approximate Gas Input for Typical Selected Appliances used in residential occupancies

Appliance	Input Btu/hr (Approx.)
Space Heating Units	· · ·
Warm air furnace	_
Single family	100,000
Multifamily, per unit	60,000
Hydronic boiler	_
Single family	100,000
Multifamily, per unit	60,000
Space and Water Heating Units	
Hydronic boiler	-
Single family	120,000
Multifamily, per unit	75,000
Water Heating Appliances	-
Water heater, automatic storage 30 gal to 40 gal tank	35,000
Water heater, automatic storage 50 gal tank	50,000
Water heater, automatic instantaneous	-
Capacity at 2 gal/min	142,800
Capacity at 4 gal/min	285,000
Capacity at 6 gal/min	428,400
Water heater, domestic, circulating or side-arm	35,000
Cooking Appliances	_
Range, freestanding , domestic	65,000
Built-in oven or broiler unit , domestic	25,000
Built-in top unit , domestic	40,000
Other Appliances	_
Refrigerator	3,000
Clothes dryer, Type 1 (domestic)	35,000
Gas fireplace direct vent	40,000
Gas log	80,000
Barbecue	40,000
Gas light	2,500

Statement of Pr	oblem and Substantiation for Public Comment				
	The title of the Table A.5.3.2.1 is revised to reflect the contents of the Table. In addition, "domestic" is deleted in 4 table entries.				
The term "dome	estic" is not needed in the table.				
<mark>Related</mark> ∙ PI 73	ltem				
Submitter Inform	nation Verification				
Submitter Full	Name: Theodore Lemoff				
Organization:	TLemoff Engineering				
Affiliation:	None				
Street Address	:				
City:					
State:					
Zip:					
Submittal Date	: Tue Apr 05 14:36:44 EDT 2022				
Committee:	NFG-AAA				
Committee State	ement				
Committee Action:	Rejected but see related SR				
Resolution:	<u>SR-19-NFPA 54-2022</u>				
Statement:	The title of the Table A.5.3.2.1 is revised to reflect the contents of the Table. The term "domestic" is not needed in the table as it provides no further information.				



A.9.3.2.2

See Table A.9.3.2.2(a) and Table A.9.3.2.2(b).

Table A.9.3.2.2(a) Known Air Infiltration Rate Method: Minimum Space Volume for Appliances Other than Fan-Assisted for Specified Infiltration Rates *(ACH)*

Appliance		<u>Space Volume (ft³)</u>	
<u>Input</u> (<u>Btu/hr</u>)	<u>0.25 ACH</u>	<u>0.30 ACH</u>	<u>0.35 ACH</u>
5,000	420	350	300
10,000	840	700	600
15,000	1,260	1,050	900
20,000	1,680	1,400	1,200
25,000	2,100	1,750	1,500
30,000	2,520	2,100	1,800
35,000	2,940	2,450	2,100
40,000	3,360	2,800	2,400
45,000	3,780	3,150	2,700
50,000	4,200	3,500	3,000
55,000	4,620	3,850	3,300
60,000	5,040	4,200	3,600
65,000	5,460	4,550	3,900
70,000	5,880	4,900	4,200
75,000	6,300	5,250	4,500
80,000	6,720	5,600	4,800
85,000	7,140	5,950	5,100
90,000	7,560	6,300	5,400
95,000	7,980	6,650	5,700
100,000	8,400	7,000	6,000
105,000	8,820	7,350	6,300
110,000	9,240	7,700	6,600
115,000	9,660	8,050	6,900
120,000	10,080	8,400	7,200
125,000	10,500	8,750	7,500
130,000	10,920	9,100	7,800
135,000	11,340	9,450	8,100
140,000	11,760	9,800	8,400
145,000	12,180	10,150	8,700
150,000	12,600	10,500	9,000
160,000	13,440	11,200	9,600
170,000	14,280	11,900	10,200
180,000	15,120	12,600	10,800
190,000	15,960	13,300	11,400
200,000	16,800	14,000	12,000
210,000	17,640	14,700	12,600
220,000	18,480	15,400	13,200

Appliance	<u>Space Volume (ft³)</u>		
<u>Input</u> (<u>Btu/hr</u>)	<u>0.25 ACH</u>	<u>0.30 ACH</u>	<u>0.35 ACH</u>
230,000	19,320	16,100	13,800
240,000	20,160	16,800	14,400
250,000	21,000	17,500	15,000
260,000	21,840	18,200	15,600
270,000	22,680	18,900	16,200
280,000	23,520	19,600	16,800
290,000	24,360	20,300	17,400
300,000	25,200	21,000	18,000

For SI units, 1 ft³ = 0.028 m³, 1000 Btu/hr = 0.293 kW.

ACH: Air change per hour.

Table A.9.3.2.2(b) Known Air Infiltration Rate Method: Minimum Space Volume for Fan-Assisted Appliance, for Specified Infiltration Rates *(ACH)*

Appliance	<u>Required Volume (ft³)</u>		
<u>Input</u> (<u>Btu/hr</u>)	<u>0.25 ACH</u>	<u>0.30 ACH</u>	<u>0.35 ACH</u>
5,000	300	250	214
10,000	600	500	429
15,000	900	750	643
20,000	1,200	1,000	857
25,000	1,500	1,250	1,071
30,000	1,800	1,500	1,286
35,000	2,100	1,750	1,500
40,000	2,400	2,000	1,714
45,000	2,700	2,250	1,929
50,000	3,000	2,500	2,143
55,000	3,300	2,750	2,357
60,000	3,600	3,000	2,571
65,000	3,900	3,250	2,786
70,000	4,200	3,500	3,000
75,000	4,500	3,750	3,214
80,000	4,800	4,000	3,429
85,000	5,100	4,250	3,643
90,000	5,400	4,500	3,857
95,000	5,700	4,750	4,071
100,000	6,000	5,000	4,286
105,000	6,300	5,250	4,500
110,000	6,600	5,500	4,714
115,000	6,900	5,750	4,929
120,000	7,200	6,000	5,143
125,000	7,500	6,250	5,357
130,000	7,800	6,500	5,571

<u>Appliance</u> <u>Input</u> (<u>Btu/hr</u>)	<u>Required Volume (ft³)</u>		
	0.25 ACH	<u>0.30 ACH</u>	0.35 ACH
135,000	8,100	6,750	5,786
140,000	8,400	7,000	6,000
145,000	8,700	7,250	6,214
150,000	9,000	7,500	6,429
160,000	9,600	8,000	6,857
170,000	10,200	8,500	7,286
180,000	10,800	9,000	7,714
190,000	11,400	9,500	8,143
200,000	12,000	10,000	8,571
210,000	12,600	10,500	9,000
220,000	13,200	11,000	9,429
230,000	13,800	11,500	9,857
240,000	14,400	12,000	10,286
250,000	15,000	12,500	10,714
260,000	15,600	13,000	11,143
270,000	16,200	13,500	11,571
280,000	16,800	14,000	12,000
290,000	17,400	14,500	12,429
300,000	18,000	15,000	12,857
For SI units, 1 ft ³ = 0.02 A <i>CH</i> : Air change per ho	8 m ³ , 1000 Btu/hr = 0.2 ur.	93 kW.	
onal Proposed Cha	nges		
File Name	Descriptio	<u>n Approvec</u>	ł

Statement of Problem and Substantiation for Public Comment

The text added to this section is work of the TG on combustion air. The added text provides a method for converting ACH50, (which is commonly used in building tightness evaluations), to ACHNAT which is the parameter used in this code.

This additional text provides a better understanding of combustion air deficiencies and the determination of combustion air volume requirements based on the tightness of the building.

Related Item

• Pr 34

Submitter Information Verification

 Submitter Full Name: John Puskar

 Organization:
 Prescient Technical Services L

 Street Address:

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State: Zip: Submittal Date Committee:	e: Mon May 16 10:57:43 EDT 2022 NFG-AAA
Committee Stat	tement
Committee Action:	Rejected but see related SR
Resolution:	<u>SR-26-NFPA 54-2022</u>
Statement:	The added text provides a method for converting ACH50, (which is commonly used in building tightness evaluations), to ACHNAT which is the parameter used in this code. This additional text provides a better understanding of combustion air deficiencies and the determination of combustion air volume requirements based on the tightness of
	the building.

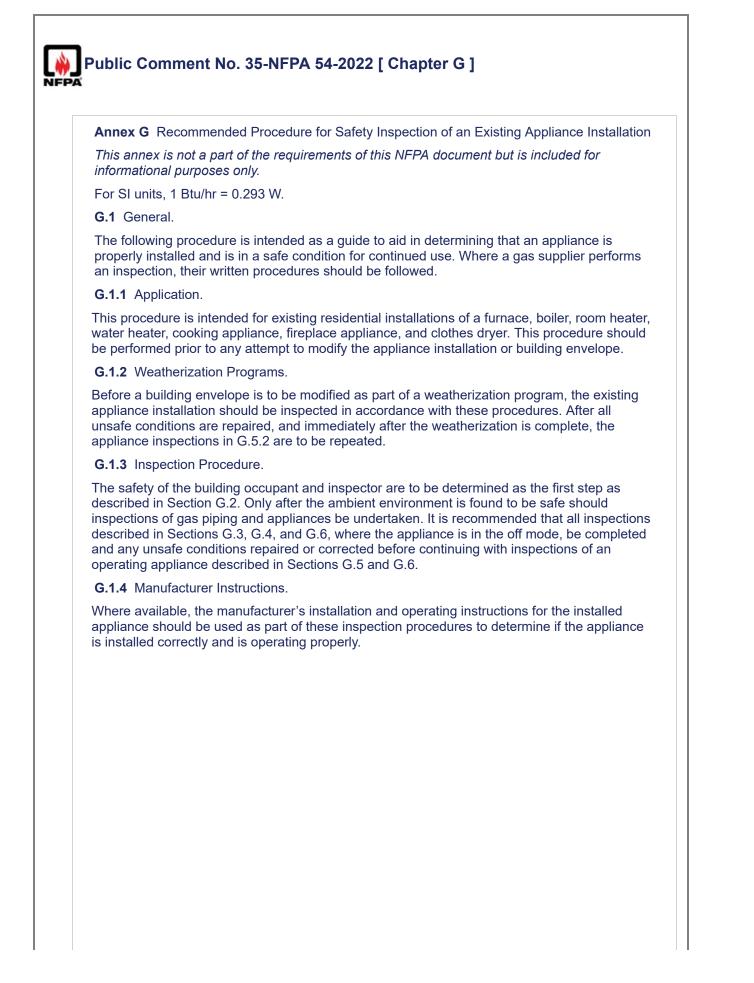
*9.3.2.2.

Meeting the requirements of the "Known Air Infiltration Rate Method" is not a guarantee that the equipment will pass the section 11.6 draft test with current tighter construction, and remodeling, and weatherization methods. There are also factors related to building airflows and combustion air that cannot be quantified or predicted including leakage of supply and return ducts in unconditioned spaces, multiple appliances operating at the same time, operation of exhaust fans, wind and weather conditions, and isolation of appliance areas from sources of combustion air by the closing of doors. This code is not a design manual and should not be considered as such. The formula used to determine the required indoor air volume is meant to provide you with the best guidance available at this time. Even tracer gas methods, for determining air infiltration rates, which require specialized equipment, can only determine rates of flow for the time and conditions when the test is conducted.

ACH (air changes per hour) in this formula is the number of air changes that occur within the building by natural means; (ACH_{NAT.}). Several methods to measure this although many factors affect this value including wind velocities, wind direction, barometric pressure, and the number and type of appliances installed and operated within the building.

Tracer gas methods have been developed to determine ACH. These produce the most reliable values for ACH. However, these methods can be expensive and cumbersome and out of reach of most contractors and or installers. Other published methods for estimating ACH's include ASHRAE estimating methods and those developed by the Air Conditioning Contractors of America Manual J, Residential Load Calculations, which includes tightness categories and estimated ACH for each category. The most prevalent technology in use today for evaluating air leakage characteristics associated with structures is through the use of blower door testing. This tool does provide a somewhat consistent and quantifiable means for arriving at the air leakage at a uniform depressurization of the building compared to the atmosphere, normally 50 pascals, and is called ACH ₅₀. This method has been successfully correlated to tracer gas measured natural air infiltration rates. ASHRAE 62.2 provides a method for converting ACH₅₀ to an ACH value that reflects the actual number of air changes under normal conditions, called ACH_{NAT}.

Many buildings constructed to current building and energy codes can achieve very low $ACH_{NAT.}$ values, which require a relatively large indoor volume for naturally drafted appliances. Designers, builders, installers, and inspectors should know that these kinds of values may require indoor air volumes that are greater than structures have available. In these cases, draft testing, identified in section 11.6 of this Code, may fail. This could require an alternate means of appliance venting, replacing the appliance, or other remedies for achieving the required combustion air other than using indoor air.



G.1.5 Instruments.

The inspection procedures include measuring for fuel gas and carbon monoxide (CO) and will require the use of a combustible gas detector (CGD) and a CO detector. It is recommended that both types of detectors be listed. Prior to any inspection, the detectors should be calibrated or tested in accordance with the manufacturer's instructions. In addition, it is recommended that the detectors have the following minimum specifications:

- (1) Gas Detector: The CGD should be capable of indicating the presence of the type of fuel gas for which it is to be used (e.g. natural gas or propane). The combustible gas detector should be capable of the following:
 - (a) *PPM:* Numeric display with a parts per million (ppm) scale from 1 ppm to 900 ppm in 1 ppm increments
 - (b) *LEL:* Numeric display with a percent lower explosive limit (% LEL) scale from 0 percent to 100 percent in 1 percent increments
 - (c) Audio: An audio sound feature to locate leaks
- (2) CO Detector: The CO detector should be capable of the following functions and have a numeric display scale as follows:
 - (a) *PPM:* For measuring ambient room and appliance emissions a display scale in parts per million (ppm) from 0 to 1,000 ppm in 1 ppm increments
 - (b) *Alarm:* A sound alarm function where hazardous levels of ambient CO is found (see Section G.2 for alarm levels)
 - (c) *Air Free:* Capable of converting CO measurements to an air-free level in ppm. Where a CO detector is used without an air-free conversion function, the CO air free can be calculated in accordance with Footnote 3 in Table G.6.

G.2 Occupant and Inspector Safety.

Prior to entering a building, the inspector should have both a combustible gas detector (CGD) and CO detector turned on, calibrated, and operating. Immediately upon entering the building, a sample of the ambient atmosphere should be taken. Based on CGD and CO detector readings, the inspector should take the following actions:

- (1) Where the CO detector indicates a carbon monoxide level of 70 ppm or greater, the inspector should immediately notify the occupant of the need for themselves and any building occupant to evacuate; the inspector should immediately evacuate and call 911.
- (2) Where the CO detector indicates a reading between 30 ppm and 70 ppm, the inspector should advise the occupant that high CO levels have been found and recommend that all possible sources of CO be turned off immediately and windows and doors be opened. Where it appears that the source of CO is a permanently installed appliance, advise the occupant to shut the appliance off and have the appliance serviced by a qualified servicing agent.
- (3) Where the CO detector indicates CO below 30 ppm, the inspection can continue. (See U.S. Consumer Product Safety Commission, *Responding to Residential Carbon Monoxide Incidents, Guidelines For Fire and Other Emergency Response Personnel*)
- (4) Where the CGD indicates a combustible gas level of 20 percent LEL or greater, the inspector should immediately notify the occupant of the need for themselves and any building occupant to evacuate; the inspector should immediately evacuate and call 911.
- (5) Where the CGD indicates a combustible gas level below 20 percent LEL, the inspection can continue.

If during the inspection process it is determined a condition exists that could result in unsafe appliance operation, shut off the appliance and advise the owner of the unsafe condition. Where a gas leak is found that may result in an unsafe condition, advise the owner of the unsafe condition and call the gas supplier to turn off the gas supply. The inspector should not continue a safety inspection on an operating appliance, venting system, and piping system until repairs have been made.

G.3 Gas Piping and Connection Inspections.

G.3.1 Leak Checks.

Conduct a test for gas leakage using either a noncorrosive leak detection solution or a CGD confirmed with a leak detection solution.

The preferred method for leak checking is by use of gas leak detection solution applied to all joints. This method provides a reliable visual indication of significant leaks.

The use of a CGD in its audio sensing mode can quickly locate suspect leaks but can be overly sensitive indicating insignificant and false leaks. All suspect leaks found through the use of a CGD should be confirmed using a leak detection solution.

Where gas leakage is confirmed, the owner should be notified that repairs must be made. The inspection should include the following components:

- (1) All gas piping fittings located within the appliance space
- (2) Appliance connector fittings
- (3) Appliance gas valve/regulator housing and connections

G.3.2 Appliance Connector.

Verify that the appliance connection type is compliant with Section 9.6. Inspect flexible appliance connections to determine if they are free of cracks, corrosion, and signs of damage. Verify that there are no uncoated copper alloy connectors. Where connectors are determined to be unsafe or where an uncoated copper alloy connector is found, the appliance shutoff valve should be placed in the off position and the owner notified that the connector must be replaced.

G.3.3 Piping Support.

Inspect piping to determine that it is adequately supported, that there is no undue stress on the piping, and if there are any improperly capped pipe openings.

G.3.4 Bonding.

Verify that the electrical bonding of gas piping is compliant with Section 7.12.

G.4 Inspections to Be Performed with the Appliance Not Operating.

The following safety inspection procedures are performed on appliances that are not operating. These inspections are applicable to all appliance installations.

G.4.1 Preparing for Inspection.

Shut off all gas and electrical power to the appliances located in the same room being inspected. For gas supply, use the shutoff valve in the supply line or at the manifold serving each appliance. For electrical power, place the circuit breaker in the off position or remove the fuse that serves each appliance. A lock type device or tag should be installed on each gas shutoff valve and at the electrical panel to indicate that the service has been shut off for inspection purposes.

G.4.2 Vent System Size and Installation.

Verify that the existing venting system size and installation are compliant with Chapters 12 and 13. The size and installation of venting systems for other than natural draft and Category I appliances should be in compliance with the manufacturer's installation instructions. Inspect the venting system to determine that it is free of blockage, restriction, leakage, corrosion, and other deficiencies that could cause an unsafe condition. Inspect masonry chimneys to determine if they are lined. Inspect plastic venting system to determine that it is free of sagging and it is sloped in an upward direction to the outdoor vent termination.

G.4.3 Combustion Air Supply.

Inspect provisions for combustion air as follows:

- (1) Non-Direct Vent Appliances. Determine that non-direct vent appliance installations are compliant with the combustion air requirements in Section 9.3. Inspect any interior and exterior combustion air openings and any connected combustion air ducts to determine that there is no blockage, restriction, corrosion, or damage. Inspect to determine if horizontal combustion air ducts are sloped upward toward the air supply source.
- (2) *Direct Vent Appliances.* Verify that the combustion air supply ducts and pipes are securely fastened to direct vent appliance and determine that there are no separations, blockage, restriction, corrosion, or other damage. Determine that the combustion air source is located in the outdoors or to areas that freely communicate to the outdoors.
- (3) Unvented Appliances. Verify that the total input of all unvented room heaters and gas-fired refrigerators installed in the same room or rooms that freely communicate with each other does not exceed 20 Btu/hr/ft³.

G.4.4 Flooded Appliances.

Inspect the appliance for signs that the appliance has been damaged by flooding. Signs of flooding include a visible water submerge line on the appliance housing, excessive surface or component rust, deposited debris on internal components, and mildew-like odor. Inform the owner that flood-damaged appliances should be replaced.

G.4.5 Flammable Vapors.

Inspect the room/space where the appliance is installed to determine if the area is free of the storage of gasoline or any flammable products such as oil-based solvents, varnishes or adhesives. Where the appliance is installed where flammable products will be stored or used, such as a garage, verify that the appliances burner is a minimum of 18 in. above the floor unless the appliance is listed as flammable vapor ignition–resistant.

G.4.6 Clearances to Combustibles.

Inspect the immediate location where the appliance is installed to determine if the area is free of rags, paper, or other combustibles. Verify that the appliance and venting system is compliant with clearances to combustible building components in 9.2.2.

G.4.7 Appliance Components.

Inspect internal components by removing access panels or other components for the following:

- Inspect burners and crossovers for blockage and corrosion. The presence of soot, debris, and signs of excessive heating could indicate incomplete combustion due to blockage or improper burner adjustments.
- (2) Metallic and non-metallic hoses for signs of cracks, splitting, corrosion, and loose connections
- (3) Signs of improper or incomplete repairs
- (4) Modifications that override controls and safety systems
- (5) Electrical wiring for loose connections; cracked, missing, or worn electrical insulation; and indications of excessive heat or electrical shorting. Appliances requiring an external electrical supply should be inspected for proper electrical connection in accordance with *NFPA 70*.
- G.4.8 Placing Appliances Back in Operation.

Return all inspected appliances and systems to their pre-existing state by reinstalling any removed access panels and components. Turn on the gas supply and electricity to each appliance found in safe condition. Proceed to the operating inspections in Section G.5 through Section G.6.

G.5 Inspections to Be Performed with the Appliance Operating.

The following safety inspection procedures are to be performed on appliances that are operating where there are no unsafe conditions or where corrective repairs have been completed.

- **G.5.1** General Appliance Operation.
- (1) *Initial Startup.* Adjust the thermostat or other control device to start the appliance. Verify that the appliance starts up normally and is operating properly.

Determine that the pilot(s), where provided, is burning properly and that the main burner ignition is satisfactory by interrupting and re-establishing the electrical supply to the appliance in any convenient manner. If the appliance is equipped with a continuous pilot(s), test all pilot safety devices to determine whether they are operating properly by extinguishing the pilot(s) when the main burner(s) is off and determining, after 3 minutes, that the main burner gas does not flow upon a call for heat. If the appliance is not provided with a pilot(s), test for proper operation of the ignition system in accordance with the appliance manufacturer's lighting and operating instructions.

- (2) Flame Appearance. Visually inspect the flame appearance for proper color and appearance. Visually determine that the main burner gas is burning properly (i.e., no floating, lifting, or flashback). Adjust the primary air shutter as required. If the appliance is equipped with high and low flame controlling or flame modulation, check for proper main burner operation at low flame.
- (3) *Appliance Shutdown*. Adjust the thermostat or other control device to shut down the appliance. Verify that the appliance shuts off properly.

G.5.2 Test for Combustion Air and Vent Drafting for Natural Draft and Category I Appliances.

Combustion air and vent draft procedures are for natural draft and category I appliances equipped with a draft hood and connected to a natural draft venting system.

- (1) *Preparing for Inspection.* Close all exterior building doors and windows and all interior doors between the space in which the appliance is located and other spaces of the building that can be closed. Turn on any clothes dryer. Turn on any exhaust fans, such as range hoods and bathroom exhausts, so they will operate at maximum speed. Do not operate a summer exhaust fan. Close fireplace dampers and any fireplace doors.
- (2) *Placing the Appliance in Operation.* Place the appliance being inspected in operation. Adjust the thermostat or control so the appliance will operate continuously.
- (3) *Spillage Test.* Verify that all appliances located within the same room are in their standby mode and ready for operation. Follow lighting instructions for each appliance as necessary. Test for spillage at the draft hood relief opening as follows:
 - (a) After 5 minutes of main burner operation, check for spillage using smoke.
 - (b) Immediately after the first check, turn on all other fuel gas burning appliances within the same room so they will operate at their full inputs and repeat the spillage test.
 - (c) Shut down all appliances to their standby mode and wait for 15 minutes.
 - (d) Repeat the spillage test steps (a) through (c) on each appliance being inspected.
- (4) Additional Spillage Tests: Determine if the appliance venting is impacted by other door and air handler settings by performing the following tests:
 - (a) Set initial test condition in accordance with G.5.2(1).
 - (b) Place the appliance(s) being inspected in operation. Adjust the thermostat or control so the appliance(s) will operate continuously.
 - (c) Open the door between the space in which the appliance(s) is located and the rest of the building. After 5 minutes of main burner operation, check for spillage at each appliance using smoke.
 - (d) Turn on any other central heating or cooling air handler fan that is located outside of the area where the appliances are being inspected. After 5 minutes of main burner operation, check for spillage at each appliance using smoke. The test should be conducted with the door between the space in which the appliance(s) is located and the rest of the building in the open and in the closed position.
- (5) Return doors, windows, exhaust fans, fireplace dampers, and any other fuel gas burning appliance to their previous conditions of use.
- (6) If spillage occurs during testing, the owner should be notified, be instructed as to which configuration of the home would lessen its impact, and arrange for corrective action by an HVAC or venting professional. Where it is believed that the venting system performance is inadequate, the owner should be notified that alternative vent sizing, design, or configuration is needed in accordance with Chapters 12 and 13. Where it is believed that sufficient combustion air is not available, the owner should be notified that additional combustion air is needed in accordance with Section 9.3.
- G.6 Appliance-Specific Inspections.

The following appliance-specific inspections are to be performed as part of a complete inspection. These inspections are performed either with the appliance in the off or standby mode (indicated by "*OFF*") or on an appliance that is operating (indicated by "*ON*"). The CO measurements are to be taken only after the appliance is determined to be venting properly. The CO detector should be capable of calculating CO emissions in ppm air free. Table G.6 contains CO thresholds for specific appliances.

Table G.6 CO Thresholds

Appliance	Threshold Limit
Central furnace	
(all categories)	400 ppm ^a air free ^{b,c}
Floor furnace	400 ppm air free
Gravity furnace	400 ppm air free
Wall furnace	200 ppm air free
Wall furnace (direct vent)	400 ppm air free
Vented room heater	200 ppm air free
Vent-free room heater	200 ppm air free
Boilers (all categories)	400 ppm air free
Water heater	200 ppm air free
Oven/Broiler	225 ppm as measured
Top burner	25 ppm as measured (per burner)
Clothes dryer	400 ppm air free
Refrigerator	25 ppm as measured
Gas log (gas fireplace)	25 ppm as measured in vent
Gas log (installed in wood-burning fireplace)	400 ppm air free in firebox

Notes:

^aParts per million

^bAir-free emission levels are based on a mathematical equation (involving carbon monoxide and oxygen or carbon dioxide readings) to convert an actual diluted flue gas carbon monoxide testing sample to an undiluted air-free flue gas carbon monoxide level utilized in the appliance certification standards. For natural gas or propane, using as-measured CO ppm and O₂ percentage:

$$CO_{AFppm} = \left(\frac{20.9}{20.9 - O_2}\right) \times CO_{ppm}$$
 [G.6a]

where:

COAFppm = Carbon monoxide, air-free ppm

CO_{ppm} = As-measured combustion gas carbon monoxide

 O_2 = Percentage of oxygen in combustion gas, as a percentage

^CAn alternate method of calculating the CO air-free when access to an oxygen meter is not available:

$$CO_{(air-free)} = \frac{UCO_2}{CO_2}(CO)$$
 [G.6b]

where:

- UCO₂ = Ultimate concentration of carbon dioxide for the fuel being burned in percent for natural gas (12.2 percent) and propane (14.0 percent)
 - CO_2 = Measured concentration of carbon dioxide in combustion products in percent
 - CO = Measured concentration of carbon monoxide in combustion products in percent
- G.6.1 Forced Air Furnaces.
- (1) OFF. Verify that an air filter is installed and that it is not excessively blocked with dust.
- (2) *OFF*. Inspect visible portions of the furnace combustion chamber for cracks, ruptures, holes, and corrosion. A heat exchanger leakage test should be conducted.
- (3) *ON.* Verify that both the limit and fan controls are operating properly. Limit control operation can be checked by blocking the circulating air inlet or temporarily disconnecting the electrical supply to the blower motor and determining that the limit control acts to shut off the main burner gas.
- (4) *ON.* Verify that the blower compartment door is installed properly and can be resecured properly if opened. Verify that the blower compartment door safety switch operates properly.
- (5) ON. Check for flame disturbance before and after blower comes on, which can indicate heat exchanger leaks.
- (6) *ON.* Measure the CO in the vent after 5 minutes of main burner operation. The CO should not exceed threshold in Table G.6.

G.6.2 Boilers.

- (1) OFF and ON. Inspect for evidence of water leaks around boiler and connected piping.
- (2) ON. Verify that the water pumps are in operating condition. Test low water cutoffs, automatic feed controls, pressure and temperature limit controls, and relief valves in accordance with the manufacturer's recommendations to determine that they are in operating condition.
- (3) *ON*. Measure the CO in the vent after 5 minutes of main burner operation. The CO should not exceed threshold in Table G.6.

G.6.3 Water Heaters.

- (1) *OFF*. Verify that the pressure-temperature relief valve is in operating condition. Water in the heater should be at operating temperature.
- (2) *OFF.* Verify that inspection covers, glass, and gaskets are intact and in place on a flammable vapor ignition resistant (FVIR)–type water heater.
- (3) *ON.* Verify that the thermostat is set in accordance with the manufacturer's operating instructions and measure the water temperature at the closest tub or sink to verify that it is no greater than 120°F.
- (4) *OFF.* Where required by the local building code in earthquake-prone locations, inspect that the water heater is secured to the wall studs in two locations (high and low) using appropriate metal strapping and bolts.
- (5) *ON.* Measure the CO in the vent after 5 minutes of main burner operation. The CO should not exceed threshold in Table G.6.

G.6.4 Cooking Appliances.

- (1) *OFF.* Inspect oven cavity and range-top exhaust vent for blockage with aluminum foil or other materials.
- (2) OFF. Inspect cook top to verify that it is free from a build-up of grease.
- (3) ON. Measure the CO above each burner and at the oven exhaust vents after 5 minutes of burner operation. The CO should not exceed threshold in Table G.6.

G.e	5.5 Vented Room Heaters.
(1)	<i>OFF</i> . For built-in room heaters and wall furnaces, inspect that the burner compartment is free of lint and debris.
(2)	<i>OFF</i> . Inspect that furnishings and combustible building components are not blocking the heater.
(3)	<i>ON.</i> Measure the CO in the vent after 5 minutes of main burner operation. The CO should not exceed threshold in Table G.6.
G.e	6.6 Vent-Free Heaters.
(1)	<i>OFF</i> . Verify that the heater input is a maximum of 40,000 Btu/hr input, but not more than 10,000 Btu/hr where installed in a bedroom, and 6,000 Btu/hr where installed in a bathroom.
(2)	<i>OFF</i> . Inspect the ceramic logs provided with gas log–type vent-free heaters to verify that they are located and aligned properly.
(3)	OFF. Inspect the heater to verify that it is free of excess lint build-up and debris.
(4)	<i>OFF</i> . Verify that the oxygen depletion safety shutoff system has not been altered or bypassed.
(5)	<i>ON.</i> Verify that the main burner shuts down within 3 minutes by extinguishing the pilot light. The test is meant to simulate the operation of the oxygen depletion system (ODS).
(6)	<i>ON.</i> Measure the CO after 5 minutes of main burner operation. The CO should not exceed threshold in Table G.6.
G.e	6.7 Gas Log Sets and Gas Fireplaces.
(1)	<i>OFF</i> . For gas logs installed in wood-burning fireplaces equipped with a damper, verify that the fireplace damper is in a fixed open position.
(2)	<i>ON.</i> Measure the CO in the firebox (log sets installed in wood burning fireplaces or in the vent [gas fireplace]) after 5 minutes of main burner operation. The CO should not exceed threshold in Table G.6.
G.e	5.8 Gas Clothes Dryer.
(1)	<i>OFF</i> . Where installed in a closet, verify that a source of make-up air is provided and inspect that any make-up air openings, louvers, and ducts are free of blockage.
(2)	<i>OFF.</i> Inspect for excess amounts of lint around the dryer and on dryer components. Verify that the lint trap is installed properly and that it does not have holes or tears. Verify that it is in a clean condition.
(3)	<i>OFF.</i> Inspect visible portions of the exhaust duct and connections for loose fittings and connections, blockage, and signs of corrosion. Verify that the duct termination is not blocked and that it terminates in an outdoor location. Verify that only approved metal vent ducting material is installed (plastic and vinyl materials are not approved for gas dryers).
(4)	ON. Verify mechanical components, including drum and blower, are operating properly.
(5)	<i>ON.</i> Operate the clothes dryer and verify that exhaust system is intact and exhaust is exiting the termination.
(6)	<i>ON.</i> Measure the CO at the exhaust duct or termination after 5 minutes of main burner operation. The CO should not exceed threshold in Table G.6.
iona	al Proposed Changes
	File Name Description Approved nal_2-22_NFPA_54_Annex_G_1docx Annex G. Rewrite

Statement of P	Statement of Problem and Substantiation for Public Comment			
A complete rewrite of Annex G.5.2 is recommended by the task group on combustion air. The rewrite provides more accurate and comprehensive method for draft testing. The proposed method provides a means to consider more variables such as the impact of door closure, duct leakage, and testing sequence.				
• fr 36	l Item			
Submitter Infor	rmation Verification			
Submitter Ful	I Name: John Puskar			
Organization:	Prescient Technical Services L			
Street Addres	s:			
City:				
State:				
Zip:				
Submittal Dat	e: Mon May 16 11:05:33 EDT 2022			
Committee:	NFG-AAA			
Committee Sta	tement			
Committee Action:				
Resolution:	n: <u>SR-28-NFPA 54-2022</u>			
Statement:	The rewrite provides more accurate and comprehensive method for draft testing. The proposed method provides a means to consider more variables such as the impact of door closure, duct leakage, and testing sequence.			

NFPA 54 Annex G. Redraft

G.5.2 Test for Combustion Air and Vent Drafting for Natural Draft and Category I Appliances for single-zone constant volume systems.

Combustion air and vent draft procedures are for natural draft and category I appliances equipped with a draft hood and connected to a natural draft venting system.

(1) Preparation For Testing.

a. Close all exterior building doors and windows and other openings to the outdoors.

b. Close solid-fuel burning appliances and fireplace dampers and combustion air controls.

c. Remove or replace the forced air heating/cooling system air filter.

d. Open heating/cooling supply air registers outside of the combustion appliance zone and close supply air registers within the combustion appliance. The combustion appliance zone in the room or space in which the appliance(s) to be tested Is located.

e. Close all interior doors except those to rooms that contain an exhaust fan or air exhausting appliance.

f. Operate all exhaust fans, air exhausting appliances and appliance mechanical draft exhausters at maximum capacity.

g. Clean filters and exhaust terminals of air exhausting appliances.

h. Do not operate summer exhaust fans.

(2) Measuring Combustion Appliance Zone Pressure.

a. Set up a manometer to measure the combustion appliance zone pressure with reference to the outdoors.

b. Obtain two combustion appliance zone pressure measurements (a total of two data points) with the heating/cooling system air handler(s) not operating.

i. One with the entrance/exit doors to the combustion appliance zone room open

ii. One with the entrance/exit doors to the combustion appliance zone room closed

c. Operate any heating/cooling system air handler at the maximum speed at which it Is expected to operate.

d. Obtain two combustion appliance zone pressure measurements (a total of 2 data points).

i. One with the entrance/exit doors to the combustion appliance zone room open

ii. One with the entrance/exit doors to the combustion appliance zone room closed

e. The most negative pressure in the combustion appliance zone, referenced to the outdoors, shall be considered to be the most negative depressurization case.

(3) Placing the Appliance in Operation.

a. Configure the building in the identified most negative pressure referenced to the outdoors of the 4 data points recorded in steps 2 (b) and (d).

b. Verify that all appliances located within the same room are in their standby mode

and ready for operation.

c. Start with the lowest Btuh input appliance in the space.

d. Place the appliance being tested in operation. Adjust the thermostat or control so that the appliance will operate continuously

e. Spillage Test. Test for spillage at the draft hood relief opening according to the appliance manufacturers' instructions. It is recommended, for personnel safety, to monitor ambient carbon monoxide (CO) levels in the space in which the testing is being conducted. Do not continue testing in an environment with more than 50 ppm (OSHA 8 hour time-weighted average limit) for Carbon monoxide exposure. Carbon Monoxide has cumulative effects, and multiple exposures can be dangerous. CO can cause headaches, dizziness, mental dullness, weakness, sleepiness, nausea, vomiting, unconsciousness, and death [Fire Protection Guide to Hazardous Materials, 14th edition, NFPA]. Persons who exhibit these signs after exposure should seek medical attention immediately.

(4) Draft Testing

If the manufacturer's instructions for draft spillage testing are not available, test as follows: a. After 5 minutes of main burner operation, check for spillage using smoke or a mirror for fogging.

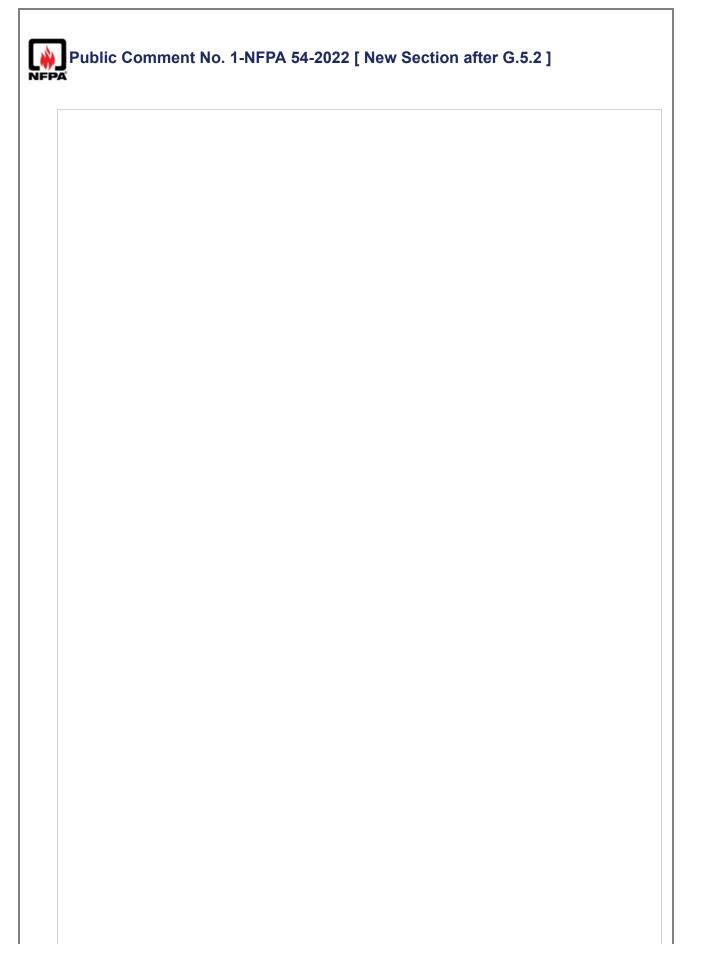
c. Immediately after the first check, turn on all other fuel gas burning appliances that obtain combustion air from indoors so that they will operate at their full inputs and repeat the spillage test for each appliance to make sure that there is no spillage as all appliances operate together.

(5) After Appliance Testing is Complete:

a. Return doors, windows, exhaust fans, heating/cooling system air handlers, fireplace dampers, and other fuel gas burning appliances to their previous conditions prior to preparation for testing.

(6) Owner Warning, Draft Testing Failures

If spillage occurs during draft testing, the owner must be notified in writing, and the owner must be instructed to arrange for corrective action by an HVAC or venting professional before the systems are again operated.



G.5.2 Test for Combustion Air and Vent Drafting for Natural Draft and Category I

Appliances for single-zone constant volume systems.

<u>Combustion air and vent draft procedures are for natural draft and category I appliances</u> <u>equipped with a draft hood and connected to a natural draft venting system.</u>

(1) Preparation For Testing.

a. Close all exterior building doors and windows and other openings to the outdoors.

b. Close solid-fuel burning appliance and fireplace dampers and combustion air

controls.

c. Remove or replace the forced air heating/cooling system air filter.

d. Open heating/cooling supply air registers outside of the combustion appliance

zone and close supply air registers within the combustion appliance zone. The combustion

appliance zone is the room or space in which the appliance(s) to be tested

Is located.

e. Close all interior doors except those to rooms that contain an exhaust fan or air

exhausting appliance.

f. Clean filters and exhaust terminals of air-exhausting appliances.

g. Operate all exhaust fans, air exhausting appliances, and appliance mechanical draft

exhausters at maximum capacity.

h. Do not operate summer exhaust fans.

(2) Measuring Combustion Appliance Zone Pressure.

a. Set up a manometer to measure the combustion appliance zone pressure with reference to the outdoors.

<u>b. Obtain two combustion appliance zone pressure measurements (a total of two data points) with the heating/cooling system air</u> <u>handler(s) not operating.</u>

i. One with the entrance/exit doors to the combustion appliance zone room open

ii. One with the entrance/exit doors to the combustion appliance zone room

<u>closed</u>

c. Operate any heating/cooling system air handler at the maximum speed at which it

is expected to operate.

<u>d.</u> <u>Obtain two combustion appliance zone pressure measurements (a total of 2 data points).</u>

i. One with the entrance/exit doors to the combustion appliance zone room open

ii. One with the entrance/exit doors to the combustion appliance zone room closed

e. The most negative pressure in the combustion appliance zone, referenced to the outdoors, shall be considered to be the most negative depressurization case.

(3) Placing the Appliance in Operation.

a. Configure the building in the identified most negative pressure referenced to the outdoors of the 4 data points recorded in steps 2 (b) and (d).

b. Verify that all appliances located within the same room are in their standby mode

and ready for operation.

c. Start with the lowest Btuh input appliance in the space.

d. Place the appliance being tested in operation. Adjust the thermostat or control so

that the appliance will operate continuously

e. Spillage Test. Test for spillage at the draft hood relief opening according to the

appliance manufacturers' instructions. It is recommended, for personnel safety, to

monitor ambient carbon monoxide (CO) levels in the space in which the testing is being conducted. Do not continue testing in an environment with more than 50 ppm (OSHA 8 hour time-weighted average limit) for carbon monoxide exposure. Carbon monoxide has cumulative effects, and multiple exposures can be dangerous. Carbon monoxide can cause headaches, dizziness, mental dullness, weakness, sleepiness, nausea, vomiting, unconsciousness, and death [Fire Protection Guide to Hazardous Materials, 14 th edition, NFPA]. Persons who exhibit these signs after exposure should seek medical attention immediately.

(4) Draft Testing

If the manufacturer's instructions for draft spillage testing are not available, test as follows:

a. After 5 minutes of main burner operation, check for spillage using smoke or a

mirror for fogging.

b. Immediately after the first check, turn on all other fuel gas burning appliances that

obtain combustion air from indoors so that they will operate at their maximum inputs

and repeat the spillage test for each appliance to make sure that there is no spillage

as all appliances operate together.

(5) After Appliance Testing is Complete:

a. Return doors, windows, exhaust fans, heating/cooling system air handlers,

fireplace dampers, and other fuel gas burning appliances to their previous

conditions prior to preparation for testing.

(6) Owner Warning, Draft Testing Failures

If spillage occurs during draft testing, the owner must be notified in writing, and the owner must be instructed to arrange for corrective action by an HVAC or venting professional before the systems are again operated.

Statement of Problem and Substantiation for Public Comment

Work product of combustion air task group.

Related Item

• 54 TG combustion air

Submitter Information Verification

Submitter Full Name: John PuskarOrganization:Prescient Technical Services LStreet Address:City:City:State:State:Fi Feb 25 09:36:20 EST 2022Committee:NFG-AAA

Committee Statement

Committee Rejected but see related SR **Action:**

Resolution: SR-28-NFPA 54-2022

Statement: The rewrite provides more accurate and comprehensive method for draft testing. The proposed method provides a means to consider more variables such as the impact of door closure, duct leakage, and testing sequence.